

Ball-milled magnetite for efficient arsenic decontamination: Insights into oxidation–adsorption mechanism

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1 **Ball-milled magnetite for efficient arsenic decontamination: Insights**
2 **into oxidation–adsorption mechanism**

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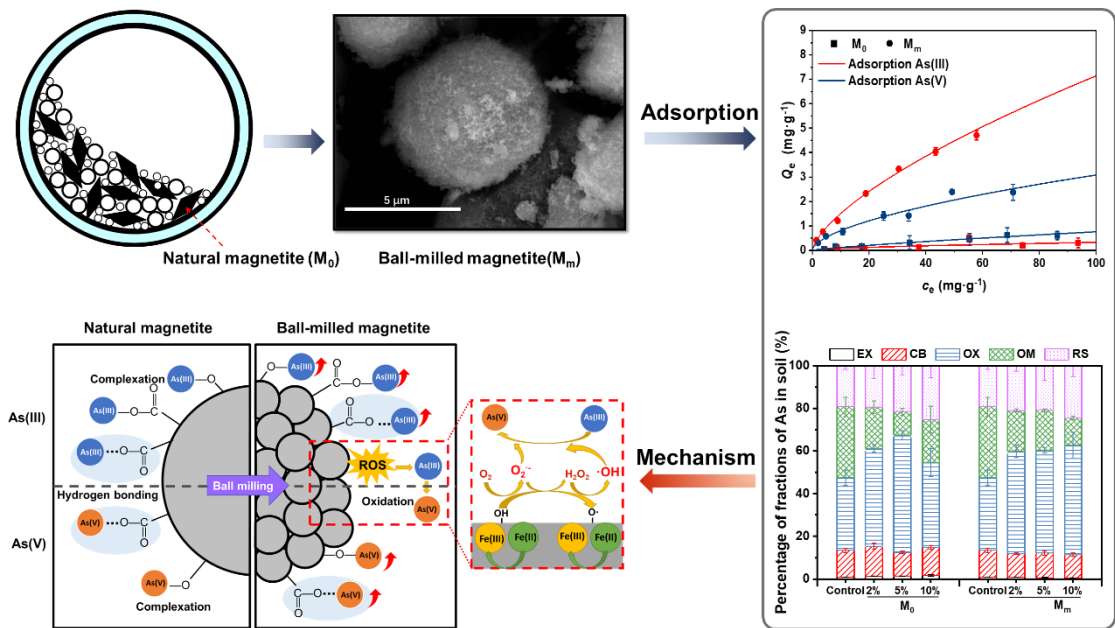
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22 **Highlights:**

- 23 ● Ball-milled modified magnetite exhibited high stability and As-adsorption capacity.
- 24 ● Dry ball milling facilitated the formation of hydroxyl and carboxyl groups upon the
- 25 magnetite.
- 26 ● Roles of surface functional groups and reactive oxygen species during the As adsorption
- 27 were discussed.
- 28 ● Enhanced As(III) removal was achieved via oxidation-adsorption mechanism.

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30

31 **Graphical Abstract:**



32
33

34 **Abstract**

35 Conventional adsorbents for decontaminating arsenic exhibit low efficacy for the removal
36 of arsenite (As(III)). This study aims to develop a robust As adsorbent from natural magnetite
37 (M_0) via a facile ball milling process, and evaluate their performance for decontaminating As(III)
38 and As(V) in water and soil systems. The ball milling process decreased the particle size and
39 crystallinity of M_0 , resulting in pronounced As removal by the ball-milled magnetite (M_m). Ball
40 milling under air facilitated the formation of Fe-OH and Fe-COOH functional groups on M_m
41 interface, contributing to effective elimination of As(III) and As(V) via hydrogen bonding and
42 complexation mechanisms. Synergistic oxidation effects of hydroxyl and carboxyl groups, and
43 reactive oxygen species (O_2^- , and $\cdot OH$) on the transformation of As(III) to As(V) during the
44 adsorption were proposed to explain the enhanced As(III) removal by M_m . A short-term soil
45 incubation experiment indicated that the addition of M_m (10 wt%) induced a decrease in the
46 concentration of exchangeable As by 30.25%, and facilitated the transformation of water-
47 soluble As into residual fraction. Ball milling thus is considered as an eco-friendly (chemical-
48 free) and inexpensive (scalable, one-stage process) method for upgrading the performance of
49 natural magnetite towards remediating As, particularly for tackling the highly mobile As(III).

50

51 **Keywords:** Arsenic, Magnetite, Ball milling, Synergistic oxidation, Sustainable environmental
52 engineering.

53 **1. Introduction**

54 Arsenic (As) is an omnipresent contaminant in soil, water, and atmosphere. The
55 undesirable emission of As-bearing substances results in extensive ecological problems owing
56 to the high migration ability and ecotoxicity of these substances (Turunen et al., 2016). These
57 toxins can enter the food chain primarily via crops cultivated on contaminated soil and/or
58 irrigation water, and intake of polluted drinking water (Chen et al., 2020), thereby posing
59 significant health risk to plants, animals, and humans (Zhang et al., 2017). Approximately 140
60 million people across 50 countries are exposed to water with As contents significantly higher
61 than the provisional guideline of $10 \mu\text{g}\cdot\text{L}^{-1}$ established by the World Health Organization (WHO,
62 1993). The predominant As species in groundwater and soil are comprised of As(III) and As(V).
63 The apparent toxicity and mobility of As(III) are higher than those of As(V). The coexistence
64 and transformation of As(III) and As(V) should also be considered within the pH range of 6-9
65 in natural aquifers (Shankar et al., 2014). Therefore, development of efficient As(III)/As(V)
66 decontamination protocols for both water and soil is a global research need.

67 Several methods have been intensively implemented for the removal of As from soil and
68 water. Primary efforts for reducing human exposure to As involve the development of
69 affordable and sustainable techniques for the simultaneous removal of As(III) and As(V), while
70 avoiding any secondary adverse effects on the local environments (Khalid et al., 2017).
71 Chemical precipitation/flocculation, ion exchange, reverse osmosis, nanofiltration, and
72 adsorption are the commonly used methods to remove As from drinking water (Bhardwaj et al.,
73 2019). Meanwhile, adsorption is considered feasible approach for eliminating As(III) from
74 water due to high efficiency, cost-effectiveness, and ease of operation. To mitigate soil arsenic

75 pollution, solidification/stabilization, backfilling, phytoremediation, and electric remediation
76 are applied (Miretzky and Cirelli, 2010). Potent adsorbents can also be used to mitigate soil As
77 contamination via stabilization, thereby lowering the bioavailability and migration of As
78 species in the soil (Yang et al., 2021). However, it is challenging to design and synthesize
79 adsorbent/stabilizer materials with a high affinity for both As(III) and As(V).

80 Recently, applying Fe-containing minerals, such as magnetite (Fe_3O_4), maghemite (γ -
81 Fe_2O_3), hematite (α - Fe_2O_3), goethite (α - FeOOH), ferrihydrite ($\text{Fe}_{10}\text{O}_{14}(\text{OH})_2$), lepidocrocite
82 ($\text{FeO}(\text{OH})$), and siderite (FeCO_3), has received a momentum for As removal from water (Liu et
83 al., 2014). Among them, the synthesized magnetite nanoparticles (MNPs) have high As affinity
84 and are magnetically separable. Wojciechowska and Lenzion-Bieluń (2020) confirmed that
85 MNPs prepared by co-precipitation method has a small size and a large specific surface area,
86 and the dose of $2.5 \text{ g}\cdot\text{L}^{-1}$ achieved the adsorption degree of 97-99% (initial concentration of
87 As(V): $10 \text{ mg}\cdot\text{L}^{-1}$ at $\text{pH}=7$). Partial substitution of MNPs with natural magnetite can avoid the
88 indispensable harmful chemicals used in the synthesis, create mutual benefit in green-adsorbent
89 development and market requirement. Nonetheless, natural magnetite shows a heterogeneity in
90 its properties and low adsorption efficiency for As, thereby limiting its engineering applications
91 (Su, 2017). Therefore, modifying the natural magnetite into powerful As(III)/As(V) adsorbent
92 has become an urgent need.

93 Common modification methods of magnetite include: 1) incorporation with other
94 components to form a composite material with high specific surface area and adsorption
95 capacity for As(III)/As(V); 2) functionalization with surfactants comprising hydroxyl, amino,
96 or carboxylic acid groups and polymer chitosan to form coatings on magnetite, thereby

97 increasing the presence of surface functional groups; and 3) use of oxidants to oxidize As(III)
98 to As(V) and then remove As(V) (Medina et al., 2019; Zhong et al., 2021). Compared with
99 chemical modification methods, ball milling is a solid-to-solid means with no need of harmful
100 chemicals (Wang et al., 2021b). It not only can rapidly reduce the particle size (Nandiyanto et
101 al., 2018), but introduce structure changes that generate defects and fresh fracture surfaces
102 (Petrovský et al., 2000), as well as alter surface chemistry of materials that increase the oxygen-
103 containing functional groups into a mineral interface. For example, Matović et al. (2019)
104 compared the variation in the number of oxygen-containing functional groups introduced in
105 activated carbon cloth via ball milling under air and argon atmospheres. Both conditions
106 increased the total number of functional groups; the concentration of functional groups on the
107 surface was higher under air ($4.0907 \text{ mmol}\cdot\text{g}^{-1}$) than under argon ($3.8346 \text{ mmol}\cdot\text{g}^{-1}$). Such
108 changes allow for an active adsorption surface, and attain the goal of efficient As removal.

109 The results obtained in previous studies validated the potential of oxidation–adsorption
110 mechanisms for effective As(III) decontamination (Ma et al., 2020). We hypothesized that
111 magnetite may exhibit excellent oxidizing ability via manipulating the Fe-related functional
112 groups on the surface matrix to promote As(III) oxidation. This will result in pronounced As
113 decontamination. The synergistic role of oxygen-containing functional groups and reactive
114 oxygen species (ROS), with the use of ball-milled magnetite, during the treatment of As-
115 contaminated water was comprehensively discussed. We characterized the physical and
116 chemical properties of natural and ball-milled magnetite, and evaluated the adsorption
117 capacities of these adsorbents for As(III) and As(V). Furthermore, the governing mechanisms
118 of As adsorption by magnetite before and after ball milling were elucidated. Finally, the use of

119 magnetite to stabilize As-polluted soil was investigated with respect to the application rate.

120

121 **2. Materials and methods**

122 **2.1 Chemicals and reagents**

123 Natural magnetite (M_0) was collected from an iron ore mine in Hebei Province, China,
124 located at 40°00'39"N, 118°51'22"E. M_0 was washed with deionized water, pulverized by the
125 coarse jaw crusher (LHMY-60, Shuangjin Machinery Company, China) and passed through a
126 200-mesh mm sieve. The chemical compositions of M_0 are shown in Table S1. All the chemicals
127 used were of guaranteed reagent (GR) grade, and they were purchased from Sinopharm
128 Chemical Reagent Co. Ltd., Shanghai, China. Deionized (DI) water (Direct-Q3,
129 MilliporeSigma, Massachusetts, USA) was used in all the experiments.

130 **2.2 Preparation of magnetite via ball milling**

131 Planetary ball milling (MITR-YXQM-2L, Miqi Instrument Equipment Co. Ltd., Changsha,
132 China) was performed under ambient conditions. The samples were ball-milled using an agate
133 tank in association with agate balls under solvent-free conditions. The ball-to-magnetite mass
134 ratio was 10:1. The rotation frequency was maintained at 640 rpm for 12 h. The as-modified
135 product was denoted as M_m , and stored in a desiccator before use.

136 **2.3 Characterization of magnetite**

137 Characterizations of chemical composition (elemental analyzer), morphology (scanning
138 electron microscopy combined with energy-dispersive X-ray spectroscopy (SEM-EDS)),
139 structural properties (X-ray diffraction (XRD) and Raman spectroscopy), crystallinity and
140 porosity (N_2 adsorption-desorption isotherm analysis), surface chemistry (X-ray photoelectron

141 spectroscopy (XPS) and Fourier-transform infrared (FTIR)), Zeta potentials, magnetism
142 (vibrating sample magnetometry (VSM)), ROS species (electron paramagnetic resonance
143 (EPR)), and electrochemical properties (electrochemical impedance spectra (EIS)) are
144 presented in detail in Text S1 of the Supplementary Material.

145 **2.4 Adsorption experiments**

146 Batch experiments were performed to evaluate the As-adsorption capacities of M_0 and M_m ,
147 and the specific experimental procedure was described in Text S2. The meanings and equations
148 of different kinetic (pseudo-first-order, pseudo-second-order, Elovich, and Weber–Morris
149 models) and isotherm (Langmuir, Freundlich, Temkin, and Dubinin–Radushkevich) models
150 were summarized in Table S2, Table S3.

151 To elucidate the variations in As(III)- and As(V)-adsorption capacities of M_0 and M_m , the
152 site energy distribution of the adsorbents was deduced from the isotherm parameters and
153 expressed as follows:

$$Q_e(C_e) = \int_0^{+\infty} Q_h(E, C_e) F(E) dE \quad (1)$$

154 where $Q_e(C_e)$ is the total adsorption of solute on the adsorbent, $Q_h(E, C_e)$ represents the
155 isotherm over local adsorption sites with an adsorption energy of E ($\text{kJ}\cdot\text{mol}^{-1}$), and $F(E)$ is the
156 site energy frequency distribution over a range of sites with homogeneous energies. The
157 adsorption energy, E , indicates the difference between the adsorption energies of the solute and
158 solvent at a specific adsorption site. The range is usually considered as $(0, +\infty)$ owing to the
159 unknown adsorption site energies.

160 The relation between C_e of the adsorbent and E , based on the condensation approximation,

161 is expressed as follows:

$$C_e = C_s \exp\left(-\frac{E - E_s}{RT}\right) = C_s \exp\left(-\frac{E^*}{RT}\right) \quad (2)$$

162 where C_s is the solute solubility in the solvent ($\text{mg}\cdot\text{L}^{-1}$), E_s is the lowest physically
163 realizable sorption energy ($\text{kJ}\cdot\text{mol}^{-1}$), and E^* is the lowest bond energy for adsorption at the
164 equilibrium concentration of C_e ($\text{kJ}\cdot\text{mol}^{-1}$).

165 The adsorption isotherm model can be described as a function of $Q_e(E^*)$ related to E^* ,
166 based on the relationship between C_e and E^* . The site energy distribution function, $F(E^*)$,
167 ($\text{mg}\cdot\text{mol}$) ($\text{kg}\cdot\text{J}$) $^{-1}$ can be obtained by deriving $Q_e(E^*)$:

$$F(E^*) = -\frac{dQ_e(E^*)}{dE^*} \quad (3)$$

168 The mathematical expectation (μ) and standard deviation (σ) of E^* , based on the site
169 energy distribution, were calculated to determine the average site energy (E_m , $\text{kJ}\cdot\text{mol}^{-1}$) and the
170 heterogeneous adsorption sites of the two magnetite materials for As(III) and As(V) (Zhang et
171 al., 2021).

$$E_m = \mu(E^*) \quad (4)$$

$$\sigma = \sqrt{\mu(E^{*2}) - \mu(E^*)^2} = \sqrt{\mu(E^{*2}) - E_m^2} \quad (5)$$

172 2.4 Soil chemical analysis and stabilization

173 Surface soil samples (0–20 cm) were collected from a contaminated agricultural soil in
174 Qinglong County, Hebei Province, China (40°22'36"N, 118°43'14"E). The soil samples were
175 air-dried, mildly crushed, and sieved through a 10-mesh sieve (<2 mm). The main
176 physicochemical properties of the soil samples are listed in Table 1.

177 **Table 1**

178 A series of short duration batch experiments was performed to quickly examine the effects
179 of magnetite addition on As stabilization in soil. A varied dosage of M_0 and M_m , with a
180 magnetite-to-soil mass ratio of 2, 5, and 10%, was added to 100 g of the soil. The liquid-solid
181 ratio was adjusted to 1:4 using DI water, and the samples without adding magnetite were
182 considered as the control group. The mixed samples were incubated at 25 °C using an artificial
183 climate box for 7 days. The five-step sequential extraction procedure was conducted followed
184 by Wenzel et al. (2001): (1) exchangeable (EX); (2) bound to carbonates (CB); (3) bound to Fe-
185 Mn oxides (OX); (4) bound to organic matter (OM); and (5) residual (RS), for the incubated
186 soils. The concentrations of total As and five fractions of As were analyzed using AFS coupled
187 with liquid chromatography (LC-AFS; AFS 9130, Titan Instruments Co. Ltd., Beijing, China).
188 The soil pH was determined using the 2.5:1 soil/H₂O method (Yan et al., 2020b). Each treatment
189 was repeated thrice.

190 **2.5 Statistical analysis**

191 Statistical analysis was performed via one-way analysis of variance, and the least
192 significant difference (LSD) test was used to compare the mean values using IBM SPSS
193 Statistics 19.0 for Windows. The data were presented as the mean \pm standard error.

194

195 **3. Results and discussion**

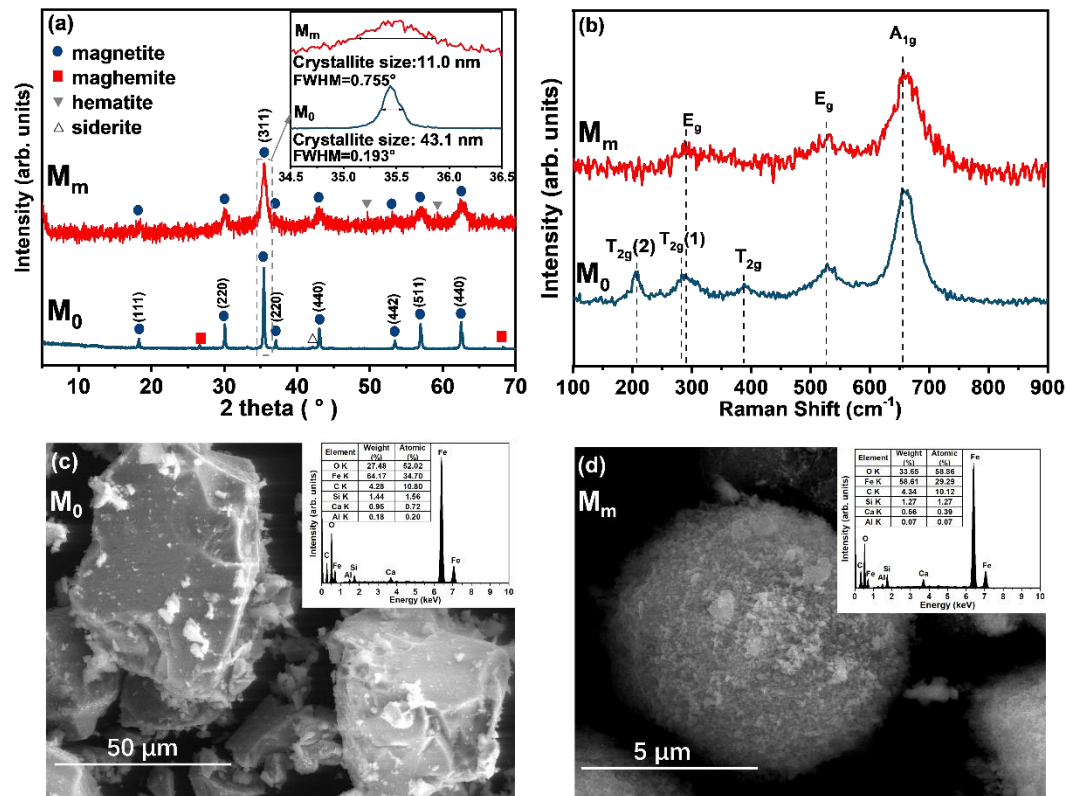
196 **3.1 Characterization of natural and ball-milled magnetite**

197 **3.1.1 Structural information and surface morphology**

198 The XRD results confirmed the presence of magnetite (Fe_3O_4), maghemite ($\gamma-Fe_2O_3$),
199 hematite ($\alpha-Fe_2O_3$) and siderite ($FeCO_3$) phases in M_0 and M_m (ICSD card number: 01-076-

200 1849, 01-039-1346, 01-085-0599 and 01-083-1764). Ball milling changed the full width half
201 maximum of the high-intensity reflection at $2\theta = 35.441^\circ$ of M_0 and M_m from 0.193° to 0.755° .
202 The crystallite sizes for M_0 (43.1 nm) sharply decreased compared to that of M_m (11.0 nm). The
203 decrease in crystalline size might induce an increase in stacking faults and structural disordering.
204 This resulted in substantial peak broadening, indicating periodic damage to the crystal lattice
205 occurred (Tung et al., 2009). Natural magnetite was crystalline; however, the height and width
206 of the diffraction peaks decreased and increased, respectively, after ball milling, hinting partial
207 decay of the crystallinity. M_m exhibited more amorphous, higher disorder and number of surface
208 defects than M_0 , allowing for M_m may have more active sites for adsorbing As (Yuan et al.,
209 2019). Furthermore, the characteristic peak of siderite disappeared after ball milling because
210 siderite might be decomposed with the participation of oxygen ($\text{FeCO}_3 + 1/2 \text{O}_2 \rightarrow \text{Fe}_3\text{O}_4 +$
211 CO_2) (Mora-Mendoza et al., 2019).

212 Raman spectroscopy was performed to analyze the chemical bonding and intramolecular
213 bonds (Fig. 1b). Five Raman-active bands was identified via factor group analysis of M_0 and
214 M_m : A_{1g} , E_g , and three T_{2g} (Moon et al., 2010). Both M_0 and M_m presented a magnetite A_{1g} mode
215 at 655 cm^{-1} that was assigned to a symmetric stretch of oxygen atoms in conjunction with Fe–
216 O bonds (Wang et al., 2009). For M_m , the T_{2g} mode band at 283 cm^{-1} broadened and redshifted
217 to the hematite E_g mode (290 cm^{-1}). This behavior is likely due to stress effects on the surface
218 of the nanocrystals (Mendili et al., 2016). The weak peak around 205 cm^{-1} as the T_{2g} model
219 originated from vibrations of Fe^{3+} and O^{2-} (Shebanova et al., 2003), which disappeared after
220 the ball milling. M_0 presented characteristic absorption peaks at 388 cm^{-1} corresponding to
221 maghemite T_{2g} , which was consistent with the observations in XRD patterns (Peng et al., 2015).



222 **Fig. 1** Structural characterization and morphological features of the magnetite sample before
 223 and after ball milling. (a) XRD patterns; (b) Raman spectra; (c, d) SEM images (inset: EDS
 224 mapping). M_0 and M_m denote natural magnetite and ball-milled magnetite, respectively.

225

226 The SEM images of M_0 illustrated the presence of irregular, micron-scale, nonporous, and
 227 loosely packed particles that were transformed into submicron spherical particles after ball
 228 milling. Initially, the particles were broken into polygonal particles primarily during the milling
 229 and then the particle shapes became blunt and smooth with the action of friction and shear (Lai
 230 and Chen, 2017). The free surface energy increased owing to fracture of the powder, thereby
 231 increasing the presence of atomic dislocations (Byrne et al., 2016). Ball milling dramatically
 232 increased the specific surface area, by 34.48-fold, and total pore volume, by 33.00-fold, than
 233 those of the natural magnetite; however, the average pore diameter remained approximately

234 unchanged (Table 2). The EDS mapping and elemental analyzer indicated that both surface and
235 bulk O and H contents were multiplied after ball milling, and approximately 1.4 wt% of C was
236 detected in two samples that could come from the siderite or the organic impurities (Mora-
237 Mendoza et al., 2019; Wang et al., 2020). These observations agree well with the previous
238 literatures, which probably due to the oxygen and moisture inside the reactor was introduced
239 onto the newly generated interface of magnetite during ball milling, forming a highly reactive
240 surface (Table 2) (Kumar et al., 2020; Xu et al., 2021).

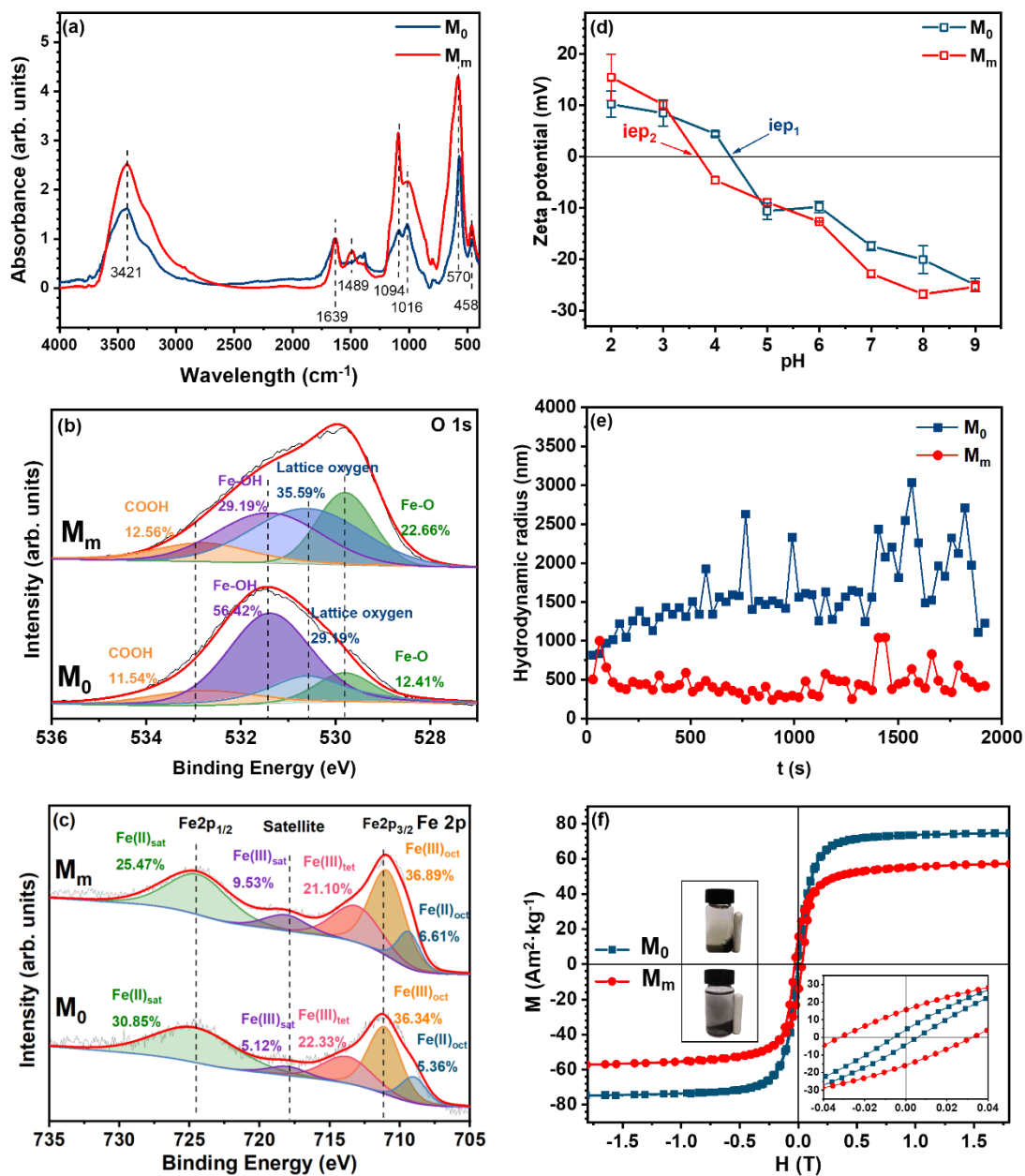
241 **Table 2**

242 **3.1.2 Analysis of surface chemistry and magnetic properties**

243 Fig. 2a shows the FTIR spectra of various functional groups in M_0 and M_m . The peaks at
244 3421 and 1094 cm^{-1} can be ascribed to O–H stretching vibration and the absorption band of
245 hydroxyl group, and the O–Si–O combination bands (1639 cm^{-1}) and the Fe–OH stretching
246 groups (1016 cm^{-1}) are also presented. The Fe–O stretching groups, where bands at 570 and
247 458 cm^{-1} represent the positions of the octahedron and tetrahedron, respectively (Salem et al.,
248 2013). The Fe–O bond provided an extended lattice framework, which would potentially
249 increase the number of octahedral holes to capture more As cations (Ellis et al., 1993).
250 Specifically, M_m has a new COO– stretching vibration group (1489 cm^{-1}) compared to M_0 ,
251 which may due to the siderite decomposition or the cracking of organic impurities in
252 mechanochemical processes (Liu et al., 2015a).

253 Fig. 2b–c and Fig. S1a–b present the high-resolution deconvoluted XPS spectra for M_0 and
254 M_m . The binding energy peaks at ~ 709 and 711 eV correspond to Fe(II) and Fe(III) in octahedral
255 coordination, and at 714 eV is attributed to Fe(III) in tetrahedral coordination of Fe_3O_4

256 (Srivastava et al., 2018). The peak at ~ 724 and 719 eV are associated with Fe (II)_{sat} and Fe
257 (III)_{sat}. Results indicated that charge transfer between Fe(II) and Fe(III) was followed by the
258 existence of a mixed oxide in magnetite. The atomic ratios of Fe(III) to Fe(II) ions shifted from
259 1.76 for M₀ to 2.11 for M_m, respectively, suggesting that the surface of M₀ was oxidized during
260 ball milling in the atmosphere of air. The peak of O 1s at ~ 529.8 eV (Fig. 2b) revealed that the
261 introduced O atoms reacted with surface Fe to form Fe-bound oxygen species (FeO_x, Fe₃O₄,
262 and FeOOH) (Zhang et al., 2019). The peak at 530.6 eV resulted from the lattice oxygen in
263 Fe₃O₄ (Han et al., 2017) and the content of lattice oxygen increased from 29.19% to 35.59%
264 due to ball milling. The increase of lattice oxygen may aid to form an environment with high O
265 activity and accelerate the oxidation reaction. This because the improved electron transfer of
266 oxygen-containing functional groups (Zheng et al., 2019).



267

268 **Fig. 2** Analytical measurements of the magnetite sample before and after ball milling. (a) FTIR
 269 spectra; (b, c) O 1s, Fe 2p signals recorded via XPS; (d) zeta potential changes as function of
 270 pH; (e) hydrodynamic radius; and (f) magnetic properties recorded via VSM (inset: the
 271 photographs of magnetite particles were placed in a magnetic field). M₀ and M_m denote natural
 272 magnetite and ball-milled magnetite, respectively.

273

274 The overall trends of the zeta potentials of M_0 and M_m varied consistently with an
275 increase in pH (Fig. 2d). High zeta potentials (either negative or positive) indicate the presence
276 of electrically stable particles (Samimi et al., 2019), revealing that the magnetite is more stable
277 at neutral pH after ball milling. The sign of the zeta potential for M_0 was reversed at pH 4.3.
278 This was recognized as the isoelectric point (*iep*), and the *iep* of M_m decreased to pH 3.6. The
279 M_m had a smaller hydrodynamic radius than the natural at 298 K (Fig. 2e). Ball milling can
280 improve the stability and aggregation of particles in the aqueous solution. Nevertheless, the
281 rising in hydroxyl and carboxyl groups made the magnetite's surface characteristics more
282 hydrophilic, which is propitious to the arsenic removal (Veloso et al., 2020).

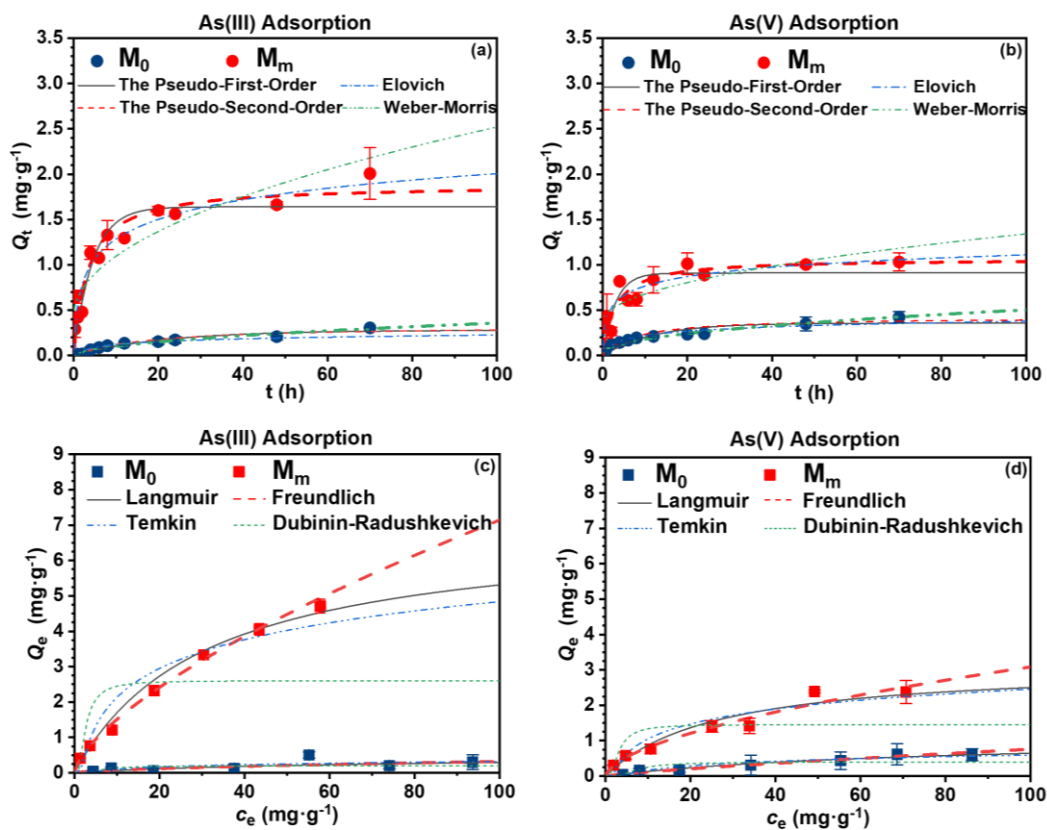
283 The magnetic hysteresis curves of M_0 and M_m are presented in Fig. 2f. Both the adsorbents
284 were ferromagnetic in nature owing to the low coercivity (H_{ci}) and remanence (M_r) values
285 (Ahmadzadeh et al., 2017). Despite ball milling resulted in a slight decrease in the saturation
286 magnetization from $74.69 \text{ Am}^2\cdot\text{kg}^{-1}$ (M_0) to $57.44 \text{ Am}^2\cdot\text{kg}^{-1}$ (M_m). The insets in Fig. 2f
287 demonstrated the photographs of M_0 and M_m particles placed in a magnetic field for 30 s,
288 representing that magnetic separation of the particles from water was still valid for M_m .

289 **3.2 Adsorptive performance of ball-milled magnetite for As removal from water**

290 **3.2.1 Adsorption kinetics**

291 Fig. 3a–b presented the variation in the As(III) and As(V) adsorption capacities with time,
292 and equilibrium was attained after 20 h. The fitting results in Table S4 revealed that the
293 adsorption of As(III) and As(V) by M_0 was consistent with the Weber–Morris model ($R^2 =$
294 0.9699 and 0.9562 , respectively). The multilinearity of intraparticle diffusion plot of M_0 for

295 As(III) and As(V) adsorption is shown in Fig. S2, corresponding to two slopes of two primary
296 mechanisms: (I) external mass transfer, and (II) intraparticle diffusion (Largitte et al., 2016). It
297 was inferred that As adsorption on M_0 was a two-step process involving initial mass transfer of
298 the adsorbate molecule to the magnetite boundary layer and subsequent adsorbate diffusion into
299 magnetite. Internal diffusion depends on the extent of surface reaction and pore structure of the
300 adsorbent, resulting in a slow reaction rate (Pholosi et al., 2020). Differently, the kinetic data of
301 M_m exhibited an optimal fit, under neutral conditions, to the pseudo-second-order model (R^2 for
302 As(III) and As(V) was 0.9728 and 0.9923, respectively). The theoretical $Q_{e,cal}$ (2.06 and 1.07
303 $\text{mg}\cdot\text{g}^{-1}$) was consistent with the experimental $Q_{e,exp}$ (2.11 and 1.03 $\text{mg}\cdot\text{g}^{-1}$). Ball milling
304 increased the specific surface area and number of adsorption sites of magnetite, forming a
305 heterogeneous surface; furthermore, the process followed the mechanism of binuclear surface
306 adsorption (Dutta et al., 2020), which explained the increased the adsorption capacity and
307 adsorption rate of As by M_m . The adsorption process for M_m was dominated by surface reactions;
308 therefore, it was subsequently controlled by further complexation interactions (Xie et al., 2014).



309 **Fig. 3** Adsorption kinetics (a, b) and isotherms (c, d) of the adsorbents. M_0 and M_m denote
 310 natural magnetite and ball-milled magnetite, respectively.

311

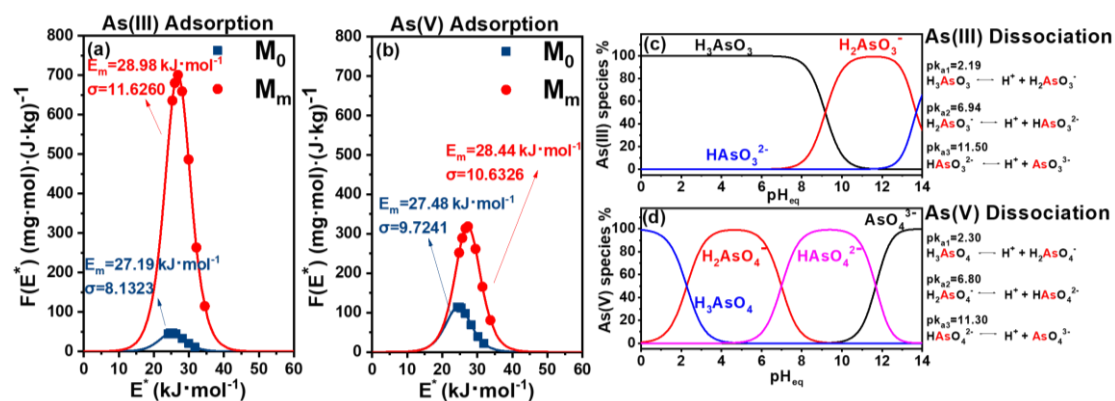
312 3.2.2 Adsorption isotherms

313 Fig. 3c–d displayed the curves describing the concentration, C_e ($\text{mg}\cdot\text{L}^{-1}$), vs. adsorption
 314 capacity, Q_e ($\text{mg}\cdot\text{g}^{-1}$), of As(III) and As(V). Multilayer adsorption occurred in both the materials
 315 because the correlation coefficient of the Freundlich model exhibited the optimal fit (Table S5)
 316 (Vikrant et al., 2018). The adsorption isotherms of both M_0 and M_m were nonuniform and
 317 involved different adsorption forces (Singh et al., 2012). K_F is the adsorption capacity per unit
 318 pressure, and a high K_F indicates a strong adsorption capacity. The K_F of M_m for both As(III)
 319 and As(V) clearly outweigh the values for M_0 . The $1/n$ value is generally less than 1, and its
 320 magnitude reflects the influence of adsorbate concentration on the adsorption capacity. The

321 values of n calculated from the Freundlich model fitting were all greater than 1, thereby
322 indicating their validity for the active adsorption sites (Vikrant et al., 2018). It was inferred that
323 adsorption was an endothermic process and induced disorder at the solid–liquid interface.
324 Moreover, adsorption and oxidation occurred simultaneously between the As species and the
325 adsorbents (Liu et al., 2011).

326 **3.2.3 Site energy distribution**

327 The relationship between the adsorption efficiency for As(III)/As(V) and the site energy
328 distribution on M_0 and M_m was derived using the Langmuir–Freundlich model (Fig. 4a–b). The
329 high-adsorption-energy sites were preferentially occupied because the concentration of
330 As(III)/As(V) was low. As(III) and As(V), with an increase in their concentration, gradually
331 occupied the low-energy sites owing to saturation of a substantial portion of the high-energy
332 sites. The energy of the sites were the dominant contributors to the adsorption of As(III) and
333 As(V) on magnetite shifted from the high- to low-energy side after ball milling. The area
334 occupied by M_m was greater than that occupied by M_0 , indicating the pronounced adsorption of
335 As(III)/As(V) on M_m . The high E_m after ball milling signified the strong adsorption affinities of
336 M_m for As(III) ($28.98 \text{ kJ}\cdot\text{mol}^{-1}$) and As(V) ($28.44 \text{ kJ}\cdot\text{mol}^{-1}$). The high σ value indicated the
337 presence of numerous heterogeneous sorption sites. The maximum increase in the number of
338 heterogeneous adsorption sites for As(III) was observed in M_m . The presence of heterogeneous
339 surfaces originated from the heterogeneity in the chemical composition (Shen et al., 2015).



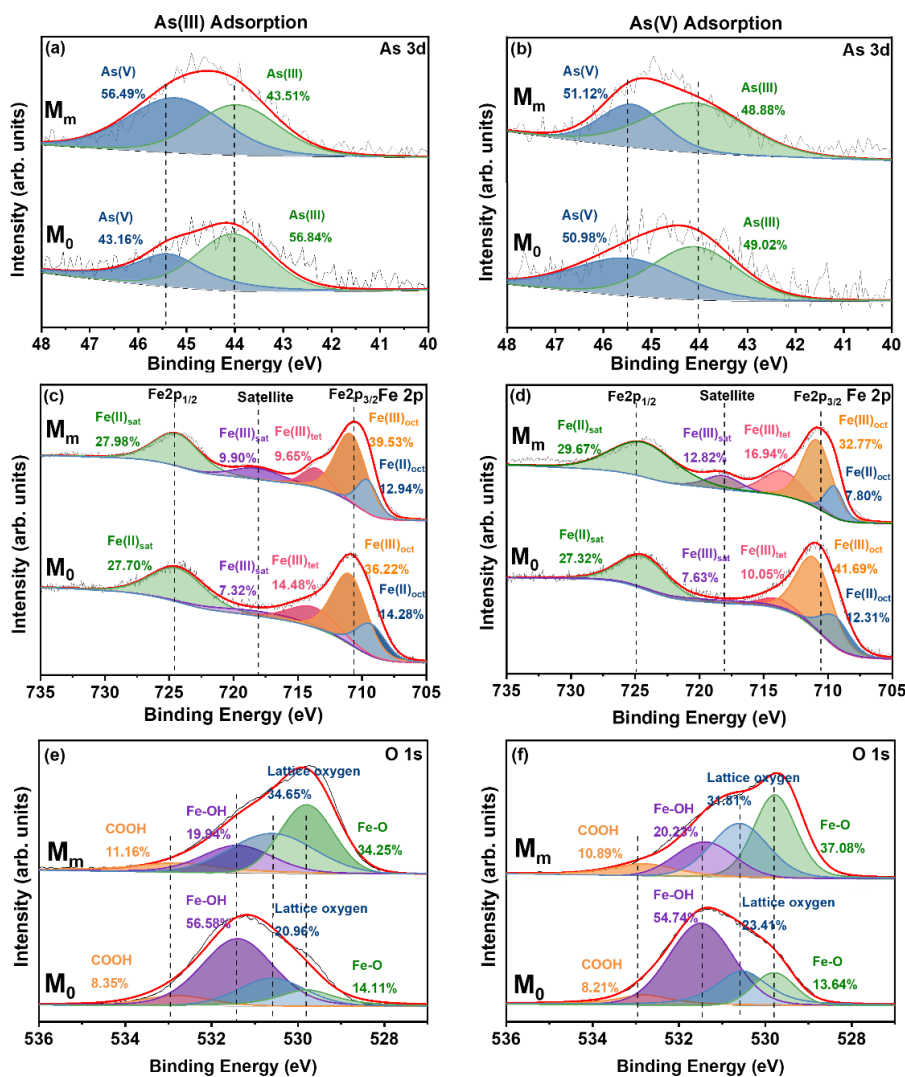
340 **Fig. 4** Site energy distributions for M_0 and M_m after As(III) and As(V) removal (a, b), and
 341 variation in As speciation at different pH (c, d). M_0 and M_m denote natural magnetite and ball-
 342 milled magnetite, respectively.

343

344 3.2.4 Roles of surface functional groups and ROS in As oxidation and adsorption

345 3.2.4.1 Role of surface functional groups

346 Fig. 5a–b showed the As 3d spectra obtained via XPS analysis. These results revealed the
 347 successful adsorption of As on M_0 and M_m . Arsenic exists in different forms under neutral pH
 348 conditions owing to the difference in dissociation constant (pK_a). As(III) and As(V) exist in the
 349 form of H_3AsO_3 , $H_2AsO_4^-$, and $HAsO_4^{2-}$ (Fig. 4c–d). These anions can interact with hydrogen
 350 bond acceptors. The oxygen in Fe-COOH groups functions as H-bond-accepting sites that
 351 contribute to capture As (Wu et al., 2020). The O 1s spectra illustrated an increase of carboxyl
 352 groups for M_m after the adsorption of As(III) and As(V), affirming that hydrogen bonding could
 353 be partly responsible for the As adsorption upon the magnetite adsorbents.

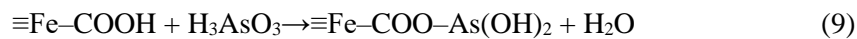
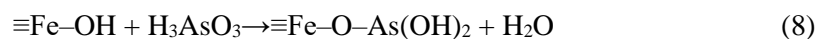
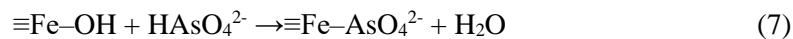


354 **Fig. 5** As 3d (a, b), Fe 2p (c, d), and O 1s (e, f) spectra, obtained via XPS, of adsorbents before
 355 and after adsorptive removal of As(III) and As(V). M₀ and M_m denote natural magnetite and
 356 ball-milled magnetite, respectively.

357

358 A new low-intensity band, designated as the characteristic peak of Fe–O–As, appeared in
 359 the FTIR spectrum at 870 cm⁻¹ (Fig. S3a–b). Replacement of Fe–OH on the mineral surface
 360 with As to form a surface complex should be one of the main mechanism for both As(V) and
 361 As(III) elimination (Perez et al., 2019). Silva et al. (2009) proposed that -COOH groups affected

362 the mobility of As(V) in an environment under Fe bridging. This would facilitate the hydrogen
 363 bonding formation and efficient As adsorption. Besides, the ionizable impurity carbon-based
 364 functional groups may acquire charge through protonation and deprotonation with solutes, and
 365 result in electrostatic attractions with negatively charged arsenate species (Vithanage et al.,
 366 2017). Nevertheless, surface ion-exchange reactions might also play a part during the
 367 adsorption process, which illustrated by the following equations (Hao et al., 2018; Peng et al.,
 368 2021).



369 3.2.4.2 Role of ROS

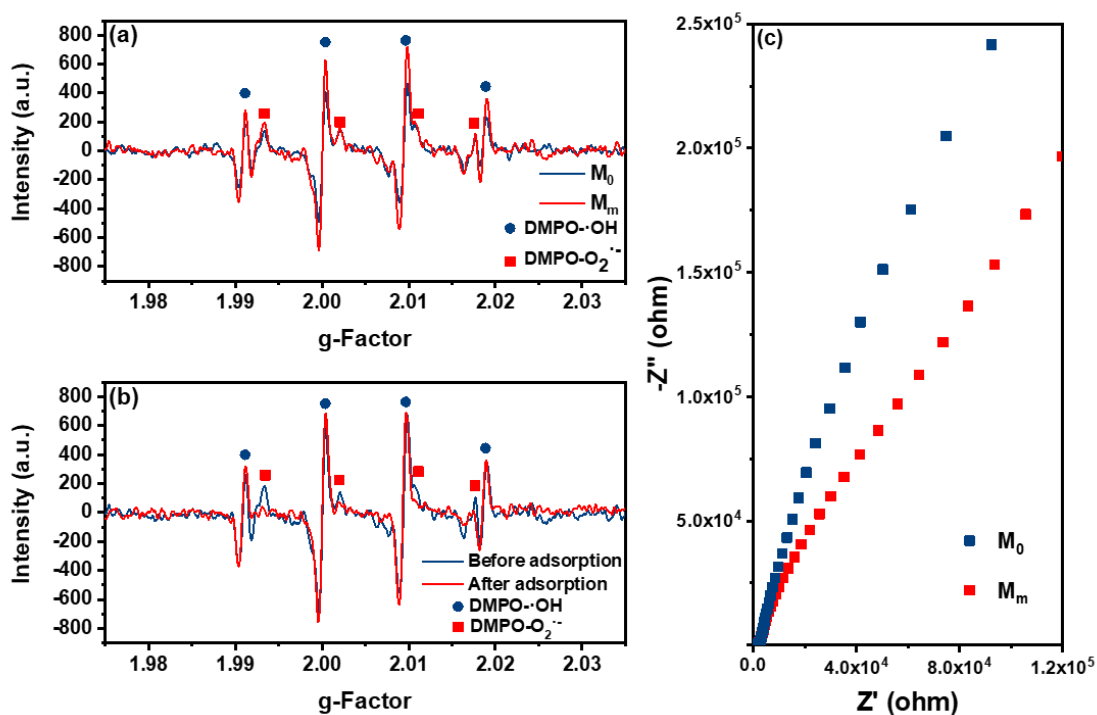
370 Comparing the As 3d spectra of As (III) adsorbed by magnetite, an increase in As(V)
 371 occurred from 43.16% to 56.49% was observed after ball milling; however, an opposite trend
 372 was observed for As(III). This suggested the occurrence of a redox reaction between As(V) and
 373 As(III) on the surface of the adsorbents. The intensity of the Fe(II)_{oct} peak decreased after As(III)
 374 adsorption. The relative contents of Fe(III)_{oct} in M₀ and M_m were 36.22% and 39.53%,
 375 respectively. These validated that the occurrence of parallel oxidation of As(III) and Fe(II). Fe
 376 atoms in magnetite existed as Fe(II) and Fe(III) mixed-valence states; therefore, cation
 377 vacancies were generated at the octahedral sites during the oxidation of Fe(II) octatoms to Fe(III)
 378 (Liu et al., 2015b). Either electron migration or Fe(II) diffusion from the internal to the oxidized
 379 surface of magnetite might happen, considering the balance of electroneutrality. Zheng et al.

380 (2021) also proposed that the release of Fe(II) from the mineral surface could take place during
381 adsorbing/oxidizing As(III). Hence, role of reactive Fe(II) is of significance during the redox
382 transformation of adsorbed As (Schaefer et al., 2011).

383 In addition to the oxidation of adsorbed As(III) via the direct reaction with surface Fe-OH
384 and Fe-COOH groups, some studies claimed that highly oxidizing substances could also impact
385 the oxidation of adsorbed As(III) (Zhong et al., 2018). We propose that the As(III) oxidation
386 capacities of magnetite might be related to the ROS; herein, EPR analysis for both M_0 and M_m
387 was performed in an air atmosphere with DMPO as the radical scavenger. M_0 and M_m presented
388 broad singlet EPR signals, thereby indicating the presence of ROS in both materials (Fig. 6a).
389 Oxygen was trapped by electrons on magnetite surface, producing superoxide radical $O_2^{\cdot-}$ (Eqs.
390 10–11) (Liu et al., 2015b), and DMPO- $O_2^{\cdot-}$ according to the splitting constant, $aN=14.3$ G, and
391 the peak signals of 1:1:1:1. In addition, a spectrum of 1:2:2:1 quartet and splitting at aN
392 $=aH=14.9$ G were observed, which were indicative of the presence of DMPO-OH adduct
393 (Wang et al., 2021a). The $O_2^{\cdot-}$ functioned as an effective oxidizing agent for H_2O and catalyzed
394 the formation of H_2O_2 that further reacted with free electrons to generate $\cdot OH$ (Eqs. 12–13)
395 (Vandjelovic et al., 2012). Significantly, the signal intensity of DMPO-OH was higher for M_m
396 than for M_0 . $\cdot OH$ and $O_2^{\cdot-}$ were likewise generated by the oxidation of Fe(II) on the magnetite
397 interface via a Fenton-type reaction (Eqs. 14–15) (Perez et al., 2019). After the adsorption of
398 As(III), DMPO- $O_2^{\cdot-}$ and DMPO-OH in M_m intensity decreased (Fig. 6b), hinting the ROS were
399 consumed and involved in As(III) oxidation process (Eq. 12) (Wu et al., 2021). Generally, $\cdot OH$
400 and $O_2^{\cdot-}$ might play a vital role in promoting the adsorption of As(III) via oxidation-adsorption
401 mechanism (Eqs. 16–17) (Perez et al., 2019).



402 EIS patterns were presented in Fig. 6c. In the low frequency region of the electrolyte, as
403 the impedance slope decreased, the rate of ion diffusion between the material and the electrolyte
404 increased. The slopes of M_0 and M_m were 2.92 and 1.71, respectively. The smaller value can be
405 ascribed to large specific surface area and fast electron transfer channels (Lyu et al., 2019). This
406 results validated that the ion storage layers of M_m had relatively higher ion diffusion rates than
407 M_0 , suggesting ball milling potentially could accelerate the transfer reactions, therefore
408 facilitating As(III) oxidizing (Zhong et al., 2018). The VSM measurements verified that the As-
409 adsorbed magnetite samples (Fig. S3c–d) exhibited high potential as a magnetically separable
410 adsorbent.

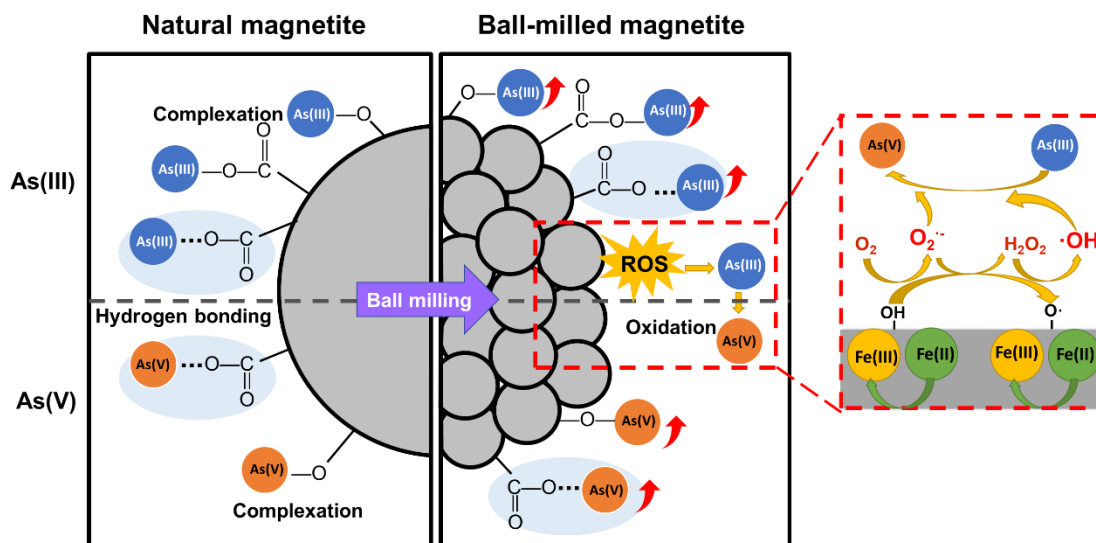


411

412 **Fig. 6** EPR spectra of (a) M_0 and M_m , (b) before and after As(III) adsorption of M_m , and (c) the
 413 electrochemical impedance spectra of adsorbents. M_0 and M_m denote natural magnetite and
 414 ball-milled magnetite, respectively.

415

416 Plausible mechanisms of As adsorption on M_m are summarized in Fig. 7. The adsorption
 417 mechanisms by magnetite adsorbents can be generally interpreted into three parts: 1) Hydrogen
 418 bonding. Protonated arsenic interacts with the hydrogen bond acceptor carboxyl group. 2)
 419 Surface complexation. The surface complexation between arsenic and surface hydroxyl and
 420 carboxyl groups may play a key role in the As(V) and As(III) elimination. 3) Oxidation-
 421 adsorption. The As(III) is firstly adsorbed by the mineral adsorptive sites, then oxidized to As(V)
 422 via the variation of valence of Fe species, and oxidation effects of ROS (O_2^- and $\cdot OH$), which
 423 contributes to the improved As(III) adsorption efficiency.



424

425 **Fig. 7** Mechanisms of As adsorption onto adsorbents. M_0 and M_m denote natural magnetite and
 426 ball-milled magnetite, respectively.

427

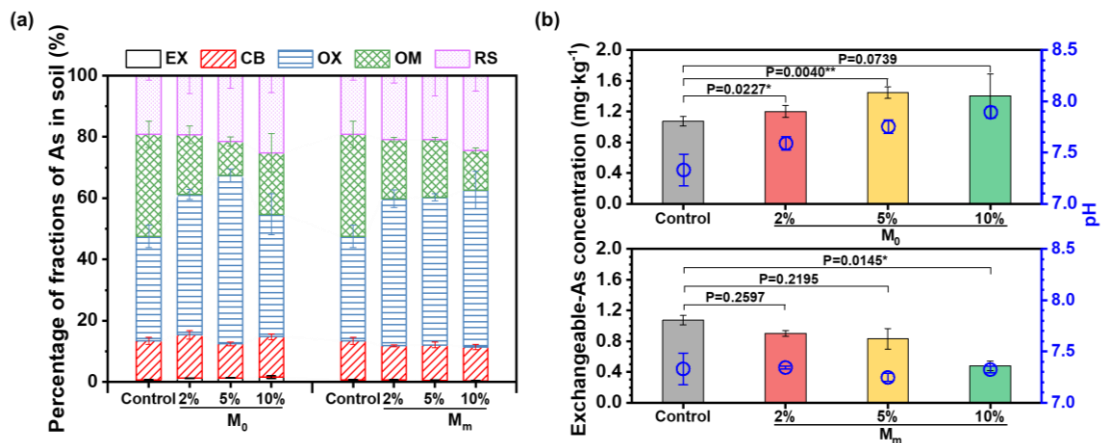
428 3.3 Arsenic stability in the natural and ball-milled magnetite-amended soils

429 The chemical forms of As in the soil for M_0 and M_m treatments were determined using a
 430 five-step sequential extraction method (Fig. 8a). Increasing the application rate of magnetite
 431 reduced the exchangeable As, but increased residual fraction of As in the soil. These results
 432 demonstrated low leachability/availability of As in amended soils. The 10 wt% dose of
 433 exchangeable-As for M_m decreased by 30.25% than the control value (Fig. 8b). Ball milling
 434 induced the transformation of magnetite into reactive amorphous Fe (hydr)oxides with high
 435 sorption capacities. Furthermore, As could either be adsorbed on the newly formed Fe
 436 (hydr)oxides or coprecipitated with the Fe (hydr)oxides. The sizes and specific surface areas of
 437 the Fe particles exerted a significant effect on the application of these particles in As
 438 stabilization (Komárek et al., 2013).

439 Arsenic removal depends considerably on the soil pH (Zhang et al., 2010). The soil pH

440 slightly increased with the presence of different amounts of M_0 . The pH ranged from 7.59 to
 441 7.89 that was slightly higher than the pH (7.33) of the control sample (Fig. 8b). Zhang et al.
 442 (2010) employed three Fe-containing materials, i.e., nanoscale zerovalent Fe, iron sulfide, and
 443 magnetite, for soil treatment, and found an increase in the soil pH by ~ 0.5 units. This was
 444 attributed to the hydrolysis reaction of magnetite in the environment that resulted in the release
 445 of OH^- (Wu et al., 2015; Yan et al., 2020a). Unexpectedly, the variation in the dosage of M_m
 446 exerted a negligible effect on the soil pH. It was speculated that ball milling induced an increase
 447 in the concentration of acidic groups on the material surface, thereby lowering the impact on
 448 the soil pH. Soil stabilizers that exert a minimal effect on the soil environment are highly
 449 significant in practical applications. The pH of M_m , unlike that of most soil stabilizers, exhibited
 450 negligible variation.

451



452 **Fig. 8** Concentration profiles of different fractions of As (a); exchangeable-As vs pH (b) in soils
 453 after addition of different dosages of natural magnetite (M_0) and ball-milled magnetite (M_m).
 454

455 **3.4 Environmental implications**

456 Extensive research has been conducted on As adsorption by modified Fe-containing
457 materials, and the adsorption capacities of various materials for As(III) and As(V) are
458 summarized in Table S6. The As-adsorption capacity for M_m is comparable to that of other
459 competitive materials. Additionally, ball-milled magnetite resulted in less environmental
460 impacts and stronger redox-suitability, and appeared to be more competitive in practical
461 applications. This cost-effective, easy-to-scale up technology for As removal is suitable for
462 utilization in the low- and low-medium-income countries; furthermore, it can also be extended
463 in many cases for future development of adsorbents.

464 Ball milling is an effective method for the synthesis of nano-scale magnetite. Ball-milled
465 magnetite facilitates the elimination of As in water and soil systems. This technique allows the
466 rapid and facile fabrication of powerful adsorbents, alleviates the environmental issues
467 originating from the storage of ore waste, and enables waste treatment for sustainable
468 engineering. However, ball milling involves a degree of randomness with the generation of
469 defects and introduction of surface hydroxyl and carboxyl groups and ROS, further efforts are
470 needed to regulate the surface functional groups via electrochemical oxidation, and oxygen
471 plasma treatment etc., to upgrade the natural mineral materials (Bai et al., 2016). Nevertheless,
472 additional investigation should also be conducted to explore the reduction of strong attractive
473 interactions between particles (e.g., coated with a polymer or an inorganic nanostructure) to
474 minimize or avoid particle agglomeration to further enhance its application potential (Favela-
475 Camacho et al., 2019).

476

477 **4. Conclusions**

478 The present study demonstrated the modification of magnetite via a sustainable, low-cost
479 ball milling process with a mechanistic insight of the absorption of As(III)/As(V) in both
480 aqueous media and soil. The oxidation activity and ability to remove As(III) from water were
481 superior for ball-milled magnetite than for natural magnetite. The coordination of hydroxyl and
482 carboxyl groups in magnetite resulted in the formation of active chemisorption sites for the
483 direct removal of As(III)/As(V). Besides, ball milling not only increased the positive effect of
484 the mineral structure on As(III)/As(V) adsorption but also stimulated Fe(II) oxidation, and
485 surface hydroxyl and carboxyl groups and ROS ($O_2^{\cdot-}$ and $\cdot OH$) production to promote As(III)
486 oxidation. Magnetite was easily separated and recovered from the solution after use. Ball-milled
487 magnetite is thus a promising eco-friendly material suitable for the decontamination of As in
488 water and soil via oxidation–adsorption mechanisms. Ball milling exhibits immense potential
489 for maneuvering adsorbents with improved adsorption capacities for various pollutants, thereby
490 facilitating extensive practical applications.

491

492 **CRedit authorship contribution statement**

493 Xiao Yang: Conceptualization, Writing – review & editing, Methodology. Siyan Liu: Writing –
494 original draft, Data curation, Investigation. Tao Liang: Supervision. Xiulan Yan:
495 Conceptualization, Funding acquisition, Writing – review & editing. Yunhui Zhang: Writing –
496 review & editing. Yaoyu Zhou: Supervision, Writing – review & editing. Binoy Sarkar:
497 Supervision, Writing - review & editing. Yong Sik Ok: Conceptualization, Supervision, Writing
498 – review & editing.

499

500 **Declaration of Competing Interest**

501 The authors declare that they have no known competing financial interests or personal
502 relationships that could have appeared to influence the work reported in this paper.

503

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509 Republic of Korea.

510 **Tables**511 **Table 1** Physical and chemical characteristics of the soils

As (mg·kg⁻¹)	pH	Organic matter (g·kg⁻¹)	Cation-exchange capacity (c mol⁽⁺⁾·kg⁻¹)	Sandy (%)	Silty (%)	Clay (%)
228.00	7.33	22.88	13.15	67.2	22.0	10.8

512

513

Table 2 The physico-chemical properties of natural and ball-milled magnetite

Material	C (%)^a	H (%)^a	O (%)^a	N (%)^a	S (%)^a	Particle size (nm)	BET surface area (m²·g⁻¹)	Total pore volume (cc·g⁻¹)	Average pore diameter (nm)
M ₀	1.42	0.40	3.85	0.09	0.49	41339	0.75	2.61×10 ⁻³	0.14
M _m	1.44	0.75	9.12	0.09	0.61	233	26.00	86.14×10 ⁻³	0.13

514 Note: M₀ and M_m denote natural magnetite and ball-milled magnetite, respectively. ^a represent that the element data collected form elemental analyzer (Elementar

515 Analysensysteme GmbH vario EL, Germany)

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Supplementary Information for:

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Ball-milled magnetite for efficient arsenic decontamination:

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Insights into oxidation–adsorption mechanism

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Supplementary material

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768

769 The SI includes 3 texts, 6 tables and 3 figures. Detailed explanations for materials
770 characterization, batch adsorption experiment, and kinetics and isotherm modelling as well as
771 corresponding calculations were also provided here.

772

773 Text S1

774 Magnetite was subjected to particle size analysis (Mastersizer 2000, Malvern Panalytical,
775 Worcestershire, UK) via analyzing a suspension 200 mg·L⁻¹ particles in water. The
776 morphological and compositional features of the samples were characterized via scanning
777 electron microscopy (SEM) combined with energy-dispersive X-ray spectroscopy (SEM-EDS,
778 MIRA 3LM, Tescan, Czechia). The specific surface area and pore size were measured via
779 Brunauer–Emmett–Teller (BET) method (BSD-PS1/2, Beishide Instrument, China). The
780 specific surface area, pore-volume, and pore size of the magnetite were assessed by N₂
781 adsorption-desorption isotherm analysis at 77 K using a volumetric adsorption analyzer (BSD-
782 PS1/2, Beishide Instrument, China). Prior to each measurement of textural properties, the
783 samples were degassed under vacuum (10 μmHg) at a temperature of 473 K for 2 h. Specific
784 surface areas were calculated using the Brunauer Emmett Teller (BET) method from adsorption
785 data obtained in the relative pressure (P/P₀) range of 0.01–0.1. The total pore volumes were
786 obtained using the amount of N₂ adsorbed at a relative pressure of 0.99. The C, H, N, S, O
787 elemental were analyzed via elemental analyzer (Elementar Analysensysteme GmbH vario EL,
788 Germany).

789 Raman spectroscopy (LabRAM HR Evolution, HORIBA Ltd., Jobin-Yvon, France) was
790 performed using the 514 nm line of an Ar⁺ laser. The surface functionalities of the samples were
791 characterized using X-ray photoelectron spectroscopy (XPS; Axis Ultra, Kratos Analytical Ltd.,
792 Manchester, England). Fourier-transform infrared (FTIR) spectroscopy (Hyperion Tensor 37,
793 Germany) was detected, and dewatered the samples at 105 °C for 8 hours before analysis. **The**
794 **collected spectra were baselined using OMNIC software 6.0 (Thermo-Nicolet). The O–Si–O**

795 combination bands at 1639 cm^{-1} was taken as the basis for normalization (Krivoshein
796 et al., 2020). For normalization, the absorbance value of this band was set to 1.0 and
797 the complete spectrum was multiplied by a ratio factor. The normalization is based on
798 the equation below:

$$a_{norm}(w) = a(w) \cdot \frac{1}{a(1639\text{ cm}^{-1})} \quad (1)$$

799 where $a_{norm}(w)$ is normalized absorbance spectrum as a function of wave number
800 w ; $a(w)$ is original absorbance spectrum; $a(1639\text{ cm}^{-1})$ is original absorbance value at
801 the reference band at wave number 1639 cm^{-1} .

802 The structural features and crystal forms of samples were investigated by using X-ray
803 diffraction (XRD, D/max-rA, Rigaku Corporation, Tokyo, Japan) patterns with monochromatic
804 Cu K α radiation ($k = 0.154\text{ nm}$). The XRD patterns were processed using MDI Jade 6.5 loaded
805 with the inorganic crystal structure database (ICSD; Materials Data Inc., California, America).
806 The crystallite size of natural magnetite was calculated based on the datasets using Scherrer's
807 formula expressed as follows (Rajendrachari et al., 2020):

$$D = \frac{K\lambda}{\beta \cos\theta} \quad (2)$$

808 where D is the average crystallite size (nm), K is a constant equal to 0.94, λ is the
809 wavelength of X-ray radiation (0.154 nm), β is the full-width half maximum (FWHM) of the
810 high-intensity peak (in radians), and 2θ is the Bragg's angle ($^{\circ}$).

811 The zeta potential (ζ) and the hydrodynamic radius of samples were analyzed using a zeta
812 potential measurement system (Zetasizer Nano ZSP, Malvern Panalytical, Worcestershire, UK).
813 The magnetic properties were evaluated using vibrating sample magnetometry (VSM,
814 PMC3900, Lakeshore Cryotronics, Westerville, USA) at around 298 K.

815 The generation of ROS in the materials was detected via electron paramagnetic resonance
816 (EPR, Bruker, Germany). Briefly, dimethyl pyridine N-oxide (DMPO) was used as a spin-
817 trapping agent because it could react with $\cdot\text{OH}$ or $\cdot\text{O}_2^-$ to produce the signals of the DMPO- $\cdot\text{OH}$
818 adducts and DMPO- O_2^- adducts, respectively. The conductivities of M_0 and M_m were evaluated
819 by measuring the electrochemical impedance spectra (EIS, CS310, CorrTest, China) according
820 to previous study (Zhong et al., 2018).

821

822 **Text S2**

823 Batch experiments were performed to evaluate the As-adsorption capacities of M_0 and M_m .
824 Disodium hydrogen arsenate ($\text{Na}_2\text{HAsO}_4 \cdot 7\text{H}_2\text{O}$) and sodium arsenite (NaAsO_2) were used for
825 preparation of the stock solution of As(III) and As(V). Sodium nitrate (NaNO_3 , 0.01 M) was
826 employed as a background electrolyte to regulate the ionic strength, and the pH of the mixture
827 was adjusted to 7.0 using HNO_3 (1 M, 0.1 M) and/or NaOH (1 M, 0.1 M).

828 Kinetic studies were conducted at a fixed As(III) or As(V) concentration ($10 \text{ mg}\cdot\text{L}^{-1}$) by
829 interacting 50 mL of solution with M_0 and M_m ($2 \text{ g}\cdot\text{L}^{-1}$). This was followed by 70 h of agitation
830 at $25 \text{ }^\circ\text{C}$ and samples withdrawn at specified time intervals. The adsorption isotherm
831 experiments were conducted via addition of $2 \text{ g}\cdot\text{L}^{-1}$ of the adsorbent to 25 mL of the As(III) or
832 As(V) solution with initial As concentrations of $5\text{--}100 \text{ mg}\cdot\text{L}^{-1}$. The mixture was filtered after
833 24 h of adsorption. The As concentration in the supernatant was determined using atomic
834 fluorescence spectrometry (AFS; AFS-9780, Haiguang Instrument Equipment Co. Ltd., Beijing,
835 China) with a detection limit of $0.01 \text{ }\mu\text{g}\cdot\text{L}^{-1}$. The adsorption capacities of As(III) and/or As(V)
836 on M_0 and M_m were calculated as follows:

$$Q_t(\text{or } Q_e) = \frac{V}{m} \times (C_0 - C_t(\text{or } C_e)), \quad (3)$$

837 where Q_t and Q_e are the adsorption capacity per gram dry weight of the adsorbents at a
838 specific time and at equilibrium ($\text{mg}\cdot\text{g}^{-1}$), respectively; C_0 denotes the initial concentration of
839 As(III) and As(V); C_t ($\text{mg}\cdot\text{L}^{-1}$) signifies the concentration of As(III) or As(V) at a certain
840 sampling time; and C_e ($\text{mg}\cdot\text{L}^{-1}$) represents the final concentration of As(III) or As(V).
841 Furthermore, V (L) is the volume of the As(III) and As(V) solutions, and m (g) is the mass of

842 the adsorbent.

843

844 **Text S3**

845 The adsorption kinetic data were fitted using the pseudo-first-order, pseudo-second-order,
846 Elovich, and Weber–Morris models (Table S2). This enables the elucidation of adsorption
847 mechanisms and determination of the rate processes and kinetic parameters. The pseudo-first-
848 and pseudo-second-order models are empirical kinetic models and used to describe the
849 adsorption process based on chemical reaction kinetics (Largitte et al., 2016). The Elovich
850 model has proven to be suitable for highly heterogeneous systems (Wu et al., 2009). The first
851 three models belong to the empirical formula for surface adsorption (Zhang et al., 2018). The
852 Weber–Morris model (intraparticle diffusion model) is of major interest because internal
853 diffusion determines the adsorption rate in most liquid systems (Zhang et al., 2018).

854 Adsorption isotherm models describe the mobility of the adsorbate from the aqueous phase
855 to the solid phase at a constant temperature (Largitte et al., 2016). The Langmuir, Freundlich,
856 Temkin, and Dubinin–Radushkevich models were used to obtain the adsorption isotherms, as
857 presented in Table S3. The Freundlich isotherm is suitable for nonideal adsorption on
858 heterogeneous surfaces. It is assumed that there are multiple types of available sites, each with
859 different free energy of adsorption, acting simultaneously (Singh et al., 2012). The Langmuir
860 model is adopted for ideal solutions and for homogeneous and independent monolayer
861 adsorption. The Temkin model assumes that adsorption is a multilayer process (Al-Ghouti and
862 Da'ana, 2020). The Dubinin–Radushkevich model aims to distinguish between the physical and
863 chemical adsorptions of ions (Al-Ghouti and Da'ana, 2020).

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893

Table S1 Chemical compositions of the natural magnetite (wt.%)

Components	TFe	SiO₂	CaO	MgO	MnO	TiO₂	Al₂O₃	SO₃	Cl	K₂O	Cr₂O₃	V₂O₃	BaO	NiO	ZnO	PbO
Content	64.93	1.25	1.04	0.56	0.37	0.36	0.36	0.18	0.13	0.11	0.09	0.06	0.04	0.01	0.01	0.01

894

Chemical compositions of the magnetite samples measured by XRF (Niton XL3t 950).

895

Table S2 Adsorption kinetic models

Model	Model equation	Model parameters
Pseudo-first-order	$\ln(Q_e - Q_t) = \ln Q_e - k_1 t$ (h ⁻¹)	k_1 - Pseudo-first-order rate constant
Pseudo-second-order	$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{t}{Q_e}$	k_2 - Pseudo-second-order rate constant (mg·g ⁻¹ ·h ⁻¹)
Elovich	$Q_t = \left(\frac{1}{b}\right) \ln(ab) + \left(\frac{1}{b}\right) \ln t$	a - Initial adsorption rate (mg·g ⁻¹ ·h ⁻²) b - Elovich constant (mg·g ⁻¹)
Weber–Morris	$Q_t = k_3 t^{\frac{1}{2}} + C$	k_3 - Weber–Morris rate constant (mg·g ⁻¹ ·h ^{-1/2})

Table S3 Adsorption isotherm models

Model	Model equation	Model parameters
		Q_m - Maximum adsorption capacity ($\text{mg}\cdot\text{g}^{-1}$)
Langmuir	$C_e/Q_e = \frac{C_e}{Q_m} + \frac{1}{K_L Q_m}$	K_L - Langmuir constant representing the energy of adsorption ($\text{L}\cdot\text{mg}^{-1}$)
		K_F - Freundlich constant indicating the adsorption capacity ($(\text{mg}\cdot\text{g}^{-1}) (\text{L}\cdot\text{mg}^{-1})^{1/n}$)
Freundlich	$\ln Q_e = \ln K_F + \frac{1}{n} \ln C_e$	n - Freundlich exponent related to the energy distribution of adsorption sites (dimensionless)
		A - Temkin constants ($\text{L}\cdot\text{g}^{-1}$)
		B - Temkin constants ($\text{J}\cdot\text{mol}^{-1}$)
Temkin	$Q_e = \frac{RT}{B} \ln A + \frac{RT}{B} \ln C_e$	R - Gas constant ($8.314 \text{ J}\cdot(\text{mol}\cdot\text{K})^{-1}$)
		T - Absolute temperature (K)
		β - Constant related to the energy of adsorption ($\text{mol}^2\cdot\text{kJ}^{-2}$)
	$\ln Q_e = -\beta \varepsilon^2 + \ln Q_s$	
Dubinin–Radushkevich	$\varepsilon = RT \ln(1 + \frac{1}{C_e})$	ε - Polanyi potential
	$E = \frac{1}{\sqrt{2\beta}}$	Q_s - Theoretical saturation capacity ($\text{mol}\cdot\text{g}^{-1}$)
		E - Activation energy ($\text{kJ}\cdot\text{mol}^{-1}$)

Table S4 Parameters of kinetic model fitting to the As(III) and As(V) adsorption results

Kinetics models		As(III)		As(V)		
		M ₀	M _m	M ₀	M _m	
Experimental results	$Q_{e,exp}$ (mg·g ⁻¹)	0.31	2.11	0.42	1.03	
Pseudo-first-order	$Q_{e,cal}$ (mg·g ⁻¹)	0.28	1.64	0.36	0.91	
	k_1 (h ⁻¹)	0.05	0.22	0.08	0.34	
	R^2	0.9259	0.8084	0.8313	0.6025	
Pseudo-second-order	$Q_{e,cal}$ (mg·g ⁻¹)	0.33	2.06	0.42	1.07	
	k_2 (g·mg ⁻¹ ·h ⁻¹)	0.17	0.10	0.30	0.32	
	R^2	0.7845	0.9728	0.9352	0.9923	
Elovich	a (mg·g ⁻¹ ·h ⁻¹)	0.07	1.89	0.18	2.58	
	b (g·mg ⁻¹)	22.08	3.19	14.73	6.72	
	R^2	0.9464	0.9222	0.9363	0.8237	
Weber–Morris	k_3 (mg·g ⁻¹ ·h ^{-1/2})	0.04	0.21	0.05	0.10	
	C (mg·g ⁻¹)	-0.02	0.44	0.03	0.37	
	R^2	0.9699	0.8649	0.9562	0.7435	
	I	$k_{3(I)}$ (mg·g ⁻¹ ·h ^{-1/2})	0.05	0.43	0.08	0.28
		$C_{(I)}$ (mg·g ⁻¹)	-0.04	0.09	-0.01	0.13
		R_I^2	0.9428	0.7729	0.9301	0.5291
II	$k_{3(II)}$ (mg·g ⁻¹ ·h ^{-1/2})	0.03	0.14	0.04	0.07	
	$C_{(II)}$ (mg·g ⁻¹)	0.01	0.80	0.06	0.53	

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R_2^2

0.9614

0.9160

0.9799

0.6936

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Table S5 Parameters of model fitting to the As(III) and As(V) adsorption isotherms

Isotherm models		As(III)		As(V)	
		M ₀	M _m	M ₀	M _m
Langmuir	Q_m (mg·g ⁻¹)	0.47	6.95	1.14	3.16
	K_L (L·mg ⁻¹)	0.02	0.03	0.01	0.04
	R^2	0.3548	0.9248	0.6872	0.8313
Freundlich	K_F ((mg·g ⁻¹) (L·mg ⁻¹) ^{1/n})	0.02	0.32	0.02	0.21
	n	1.63	1.48	1.23	1.72
	R^2	0.6490	0.9908	0.9196	0.9624
Temkin	A (L·g ⁻¹)	0.30	0.62	0.24	0.56
	B	2.64×10 ⁴	0.21×10 ⁴	1.34×10 ⁴	0.41×10 ⁴
	R^2	0.4440	0.9200	0.8942	0.8178
Dubinin– Radushkevich	Q_s (mol·g ⁻¹)	0.20	2.61	0.40	1.46
	β (mol ² ·kJ ²)	6.25×10 ⁻⁶	1.12×10 ⁻⁶	8.19×10 ⁻⁶	1.58×10 ⁻⁶
	E (kJ·mol ⁻¹)	282.80	669.35	247.03	561.83
	R^2	0.4780	0.6504	0.8356	0.6520

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904 **Table S6** Comparison of the As(III) and As(V) removal capacities for the previously reported ball-milled Fe-containing materials and the material
 905 investigated in the present study

Materials	Adsorbed pollutant	Initial concentration (mg·L ⁻¹)	Maximum capacity (mg·g ⁻¹)	Equilibrium time (h)	Preparation method	References
Hematite-coated Fe ₃ O ₄ particles	As(III)	0.01–0.1	1	9	Ball milling under Ar atmosphere and addition of heptane as a lubricant	Simeonidis et al. (2011)
Fe ₂ O ₃ -MnO ₂		0.2–2	2.52	10	Mechanical–chemical treatment	Andjelkovic et al. (2014)
Fe ₂ O ₃ -TiO ₂		5–50	13.86	1	Ball milling; sintering at 700 °C for 1 h	Su et al. (2017)
Limonite		1–100	9.14	12	Mechanical activation with an added dispersion medium	Yan et al. (2019)
Zerovalent iron		1–20	9.12	6	Mechanical activation treatment	Zhang et al. (2021)

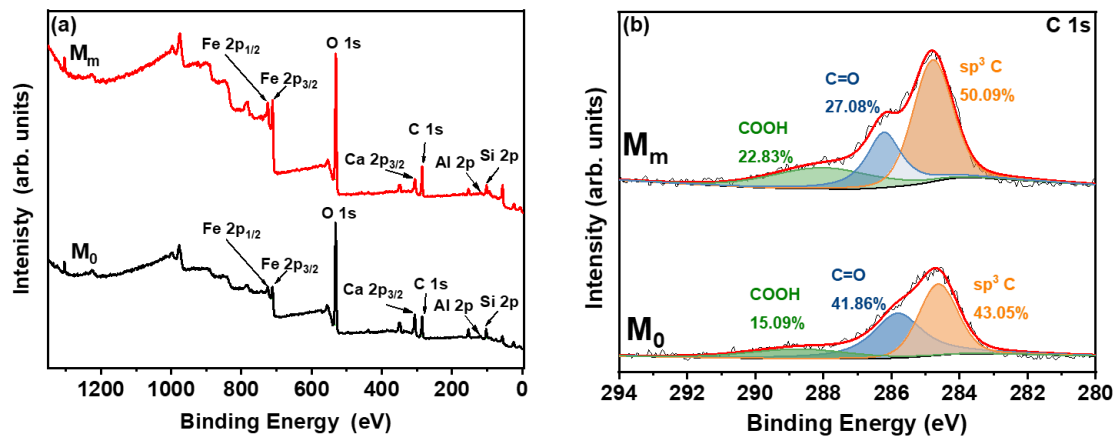
Magnetite		5–100	6.94	'	20	Ball milling	Present study
Hematite-coated Fe ₃ O ₄ particles	As(V)	0.01–0.1	2.1	'	9	Ball milling under Ar atmosphere and addition of heptane as a lubricant	Simeonidis et al. (2011)
Fe ₂ O ₃ -MnO ₂		0.2–2	3.08	'	10	Mechanical–chemical treatment	Andjelkovic et al. (2014)
Nanomagnetite-Zeolite		1–300	5.10	'	1	Synthetic nanomagnetite in an alkali media; ball milling under N ₂ atmosphere	Pizarro et al. (2015)
Fe ₂ O ₃ -TiO ₂		5–50	15.73	'	1	Ball milling; sintering at 700 °C for 1 h	Su et al. (2017)
Magnetite enriched particles		1–50	13.88	'	2	Alkaline cleaning, drying, and grinding in the ball-milling system	Shahid et al. (2019)
Limonite		1–100	8.26	'	12	Mechanical treatment with an added dispersion medium	Yan et al. (2019)
Magnetite		5–100	3.16	'	20	Ball milling	Present study

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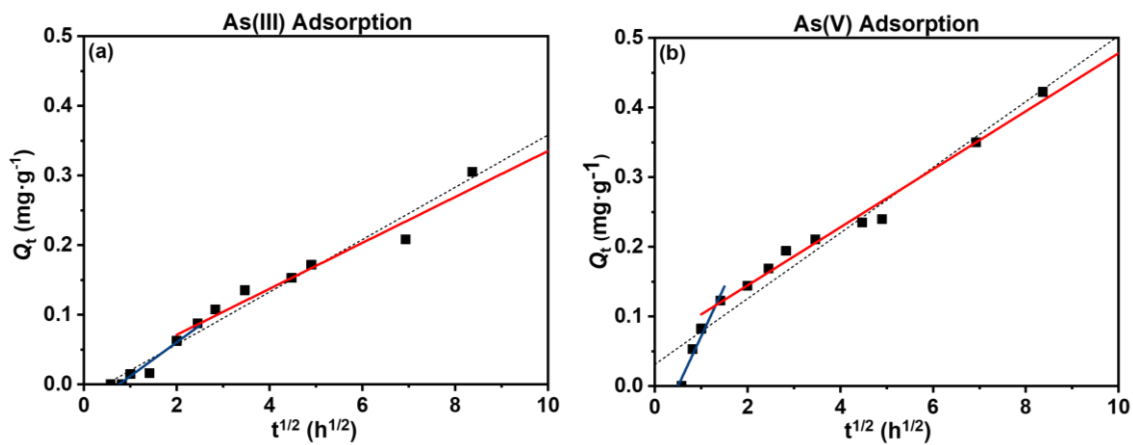


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934 **Fig. S1** Full (a), and C 1s (b) spectra signals recorded via XPS. M_0 and M_m denote natural

935 magnetite and ball-milled magnetite, respectively.

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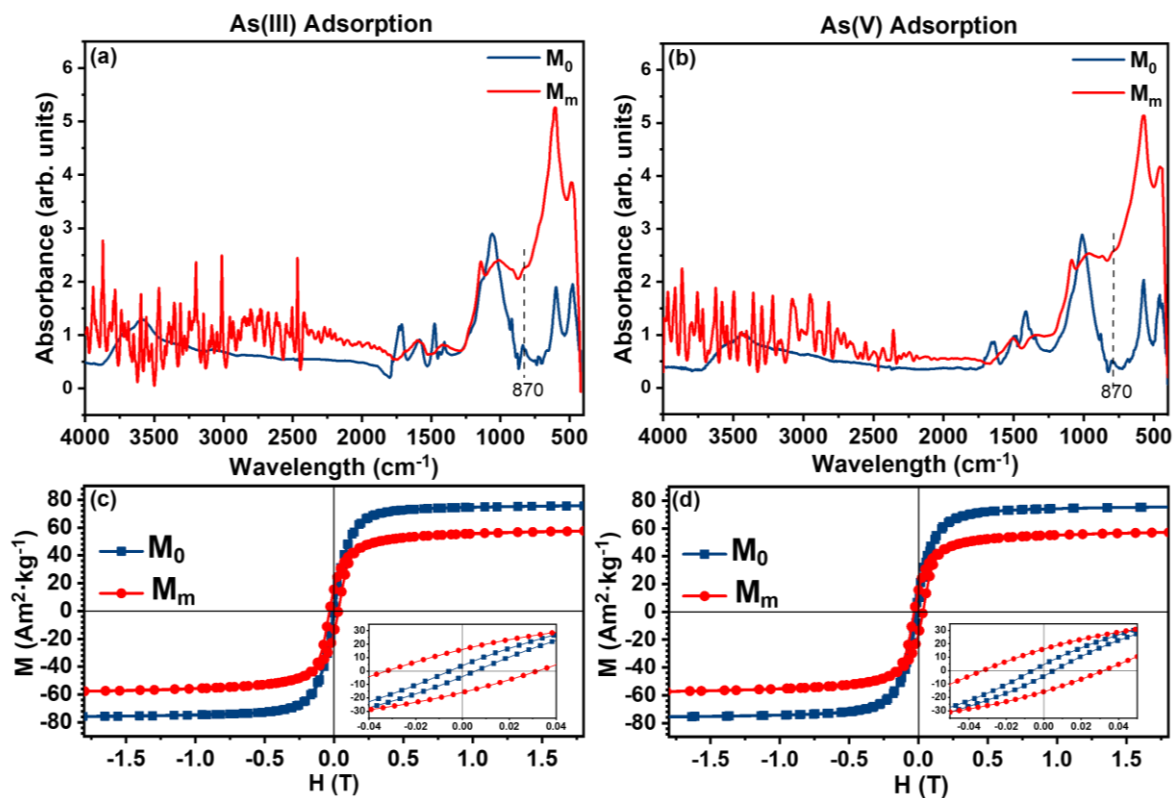


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Fig. S2 Weber–Morris model plots of As(III) and As(V) on natural magnetite (M_0).

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Fig. S3 Variations in the surface chemistry of adsorbents (a, b: FTIR spectra, c, d:

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magnetic properties recorded via VSM) before and after adsorption of As(III) and As(V). M_0

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and M_m denote natural magnetite and ball-milled magnetite, respectively.

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