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5 **Simulating uranium sorption onto inorganic particles:**
6 **the effect of redox potential**
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8

9 **Abstract**

10 An analytical expression is proposed to simulate the effects of pH and redox potential (E) on
11 the sorption of uranium onto model inorganic particles in aquatic environments instead of
12 following an experimental approach providing a list of empirical sorption data. The expression
13 provides a distribution coefficient (Kd) as function of pH, E and ligand concentration (complex
14 formation) applying a surface complexation model on one type of surface sites ($>SuOH$). The
15 formulation makes use of the complexation and hydrolysis constants for all species in solution
16 and those sorbed at the surface, using correlations between hydrolysis constants and surface
17 complexation constants, for the specific sorption sites. The model was applied for the sorption
18 of uranium onto aluminol, iron hydroxide and silanol sites, mimicking respectively 'clean' clay
19 or 'dirty' clay and 'clean' sand or 'dirty' sand ('dirty' referring to iron hydroxide
20 contaminated), in absence or presence of carbonates in solution. The calculated distribution
21 coefficients are very sensitive with the presence or absence of carbonates. The Kd values
22 obtained by applying the model are compared with values reported in the literature for the
23 sorption of uranium onto specific adsorbents. It is known that in surface water, U(VI) and its

24 hydroxides are the primary stable species usually observed. However, reduction to U(IV) is
 25 possible and may be simulated during sorption or when the redox potential (E) decreases.
 26 Similar simulations are also applicable to study the sorption of other redox sensitive elements.

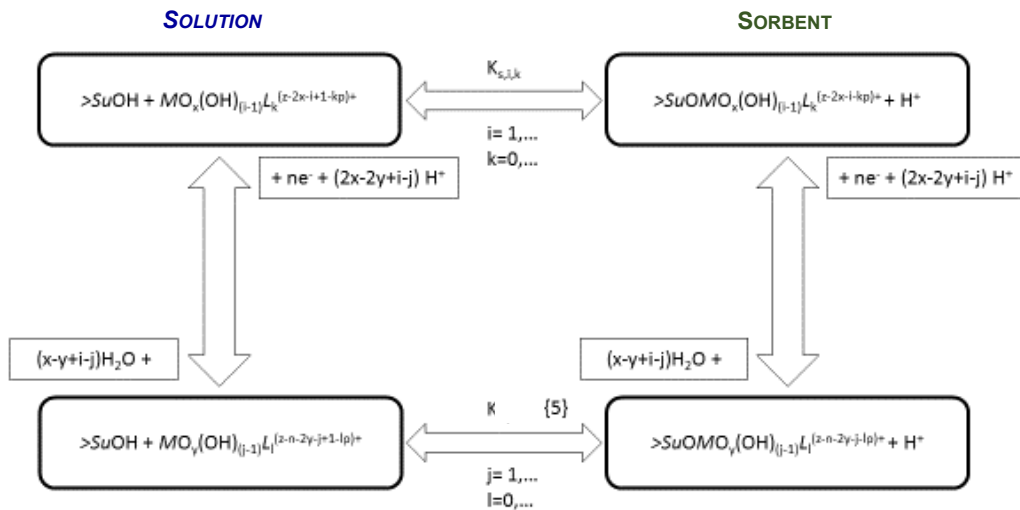
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28 Keywords: *uranium sorption, redox potential, surface complexation, distribution coefficient*

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30 Graphical abstract

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32

33 Reactions in **SOLUTION** and at the **SORBENT** interface that must be considered to derive the
 34 model as $K_d = f(\text{pH}, E, [L], d, \{>SuOH\}, \Delta)$ for the redox couple $M^{z+}/M^{(z-n)+}$, with ions
 35 complexed by hydroxyl (OH^-) and ligand (L) onto surface sorbing group ($>SuOH$) of
 36 density Δ on particles of size d at a given pH and for redox potentials E .

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40 **1. Introduction**

41

42 Issues associated with the environmental behaviour of uranium has been the topic of numerous
43 studies e.g. Selvakumar et al (2018); Gavrilesco et al (2008). The release of uranium from a
44 contaminated sediment and its local retention are governed by biochemical reactions including
45 factors such as acidity, redox potential, presence of ligand (inorganic, organic and bioorganic)
46 of the water e.g. Ulrich et al (2009). The sorption of uranium on specific sediment components
47 is consequently a relevant issue to investigate.

48

49 The sorption of actinides onto selected inorganic model alumina and goethite colloidal particles
50 has already been reported by Degueldre *et al.* (1994) and by Ulrich *et al.* (2006). Recently
51 specific studies were also carried out on magnetite (Fe₃O₄) by Singhal *et al.* (2017), on titanium
52 oxide (TiO₂) by Lefèvre *et al.* (2008) and by Li *et al.* (2019), on zircon by Lomenech *et al.*
53 (2003), on clayeous materials such as smectite by Chisholm-Brause *et al.* (2004), muscovite by
54 Richter *et al.* (2016) and zeolite (Na₂Al₂Si₃O₁₀.2H₂O) by Su *et al.* (2018). Most of these
55 sorption studies are **empirical** and a formal approach of distribution coefficient (*K_d*)
56 determination is missing.

57

58 In sorption studies, analytical expressions based on the relation of the distribution coefficient
59 (*K_d*) and the thermodynamic properties of the phases has been applied since the formula
60 derived in the pioneered work of Degueldre *et al.* (1994). The sorption includes surface
61 complexation with one type of sorbent surface site (>SuOH). The model has been completed
62 for redox effects considering the redox potential in solution for all hydrolysed species in
63 solution and on the surface. Complexation with ligands was also included in the formulation as

64 carbonate, or total inorganic carbon (TIC), which is expected to affect significantly the
65 speciation and the sorption of metal ions in waters at quasi neutral pH values. The sorption of
66 metal ions onto particles is affected by many parameters such as pH, redox potential (E),
67 sometime called Eh , ligands concentration, e.g. [TIC], or sorption kinetics. The influence of pH
68 in sorption is well established, but the effort made in studying the influence of redox potential
69 is limited, as reported for other actinide elements e.g. Degueldre & Bolek (2009).

70 The study of the redox potential effect in the sorption is especially relevant in environmental
71 science. However, it can be difficult to study the effect experimentally (Grenthe *et al.*, (1992)).
72 Fortunately, solutions (e.g. working electrode in-line polishing) have been suggested by
73 Degueldre *et al.* (1999).

74

75 The objective of this study is to calculate the distribution coefficient as a function of pH, redox
76 potential concentration of ligand and nature of the sorbent. This approach has been applied to
77 the sorption of uranium, a redox sensitive actinide, onto three selected inorganic model
78 particles (Al_2O_3 , $FeOOH$ and SiO_2). These model particles could mimic clean clay (Al_2O_3),
79 ‘dirty’ clay or sand (surface contamination with $FeOOH$) and clean sand (SiO_2) some key
80 components of the terrestrial environment. Organic material shall be considered in a separate
81 study.

82 The ultimate aim of this work is to develop a more multipurpose model of material sorption, as
83 part of the strategy suggested by Degueldre *et al.* (2019) to upgrade the nuclear fuel cycle
84 through regenerative extraction of uranium to become a renewable resource.

85

86

87 **2. Modelling species occurrence and their sorption properties**

88

89 The sorption process involves reactions ranging from ‘inner sphere’ complex formation with
 90 active surface sites to ion exchange. It is usually described by the distribution ratio, which at
 91 equilibrium yields a distribution coefficient (Kd) as given by Equation (1):

$$92 \quad Kd = \frac{[M]_{\text{sorbed}}}{[M]_{\text{solution}}} \frac{1}{[part]} \quad (1)$$

93 where $[part]$ is the particle concentration (e.g. in $\text{g}\cdot\text{mL}^{-1}$) and $[M]$ is the concentration of the
 94 element sorbed on the particles or present in solution (both in: $\text{mmol}\cdot\text{mL}^{-1}$). The inclusion of
 95 $[part]$ in this ratio is intended to generalise the more classical distribution coefficient
 96 formulation: $Kd = C(M)_{\text{part}}/[M]_{\text{sol}}$ (with $C(M)_{\text{part}}$ in $\text{mmol}\cdot\text{g}^{-1}$) to one where the sorbent is in the
 97 liquid matrix (suspension).

98

99 **2.1 Particles and sorption sites**

100

101 In this work metal ions e.g. $M(\text{OH})_i^{(z-i)+}$ are sorbed onto monodentate sites $>\text{SuOH}$, where Su
 102 represents the substrate material available at the surface of particles (part). The distribution
 103 coefficient in a Langmuir model is directly proportional to $[>\text{SuOH}]/[part]$, with $[>\text{SuOH}]$ the
 104 site concentration (e.g. mol mL^{-1}). In a simplified approach, if the particles are supposed to be
 105 spherical and monodispersed, the volume of one particle is given by $V = (4/3) \pi r^3$ with r the
 106 particle radius (cm or nm according to context). The particle mass (M) is consequently given by
 107 $M = \rho V$ with ρ the density of the particle material and the number of particle per volume unit
 108 (N) is given by $N = [part]/M$. The particle surface (S) is given by $S = 4 \pi r^2$ and if the particle
 109 surface is covered homogeneously by sites with the density Δ given in nm^{-2} . The number of
 110 site per particle (n_s) can be defined as and be easily calculated as $n_s = \Delta S$. From this, the
 111 number of site per suspension volume $N_{\text{sv}} = n_s N$ and consequently $[>\text{SuOH}] = \Delta S N/N_{\text{Av}}$
 112 where N_{Av} is the Avogadro constant.

113 This allows the $[>\text{SuOH}]/[part]$ ratio to be evaluated as $[>\text{SuOH}]/[part] = 3 \Delta N_{\text{Av}} / (\rho r)$.

114 The $[>SuOH]/[part]$ ratio may also be derived experimentally using the specific surface
 115 provided by BET measurements. The specific surface is given by $3/\rho r$ in the case of ideal
 116 spherical particles. This value may be affected by the particle porosity and the fractal of its
 117 interface.

118

119 2.2 Impact of site reactivity

120

121 Protonation and deprotonation of the $>SuOH$ sites could modify the sorption properties. These
 122 specific reactions {1} and {2} can be written:



125 The acid/base constants (K_{ai}) associated to the sites are:

$$126 \quad K_{a1} = \frac{[>SuOH][H^+]}{[>SuOH_2^+]} \quad (2) \quad \text{and} \quad K_{a2} = \frac{[>SuO^-][H^+]}{[>SuOH]} \quad (3)$$

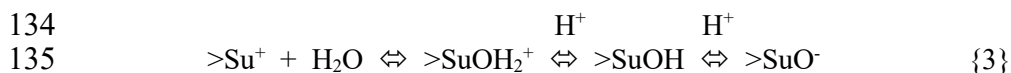
127 The total site concentration equals:

$$128 \quad [>SuOH]_{tot} = [>SuOH_2^+] + [>SuOH] + [>SuO^-] \quad (4)$$

129 which gives:

$$130 \quad [>SuOH] = \frac{[>SuOH]_{tot}}{\left(\frac{[H^+]}{K_{a1}} + 1 + K_{a2}[H^+]\right)} \quad (5)$$

131 Further to these protonation/deprotonation reactions, leaching effects due to dissolution of the
 132 structure become significant at pH around the respective pK_a values. The reactions follow the
 133 hydrolysis then deprotonations series:



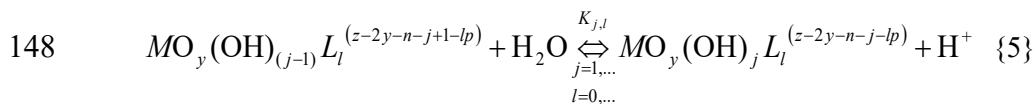
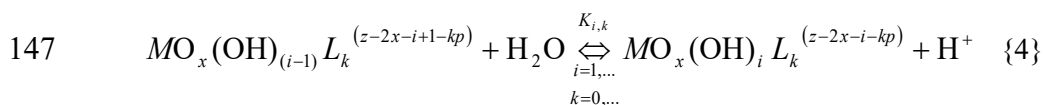
136 In reality, these effects are limited by solubility of Su in water e.g. with the soluble forms of
 137 $>Su^+$ and of $>SuO^-$. Consequently the reactivity of $>SuOH$ sites is accounted below.

138

139 **2.3 Complexes formation in the redox range**

140

141 The methodology follow the approach suggested earlier e.g. Degueldre (1997). The hydrolysis
 142 stability constants of both redox species ($K_{i,k}$ for oxidising and $K_{j,l}$ for reducing species) can be
 143 obtained on the basis of the stepwise reactions {4} and {5}. This notation is intended to include
 144 both oxo and non-oxocation species. Metal complexation reactions involving k -ligands or l -
 145 ligands (L^p) (e.g. carbonates) were also considered. The limits on all indices are fixed by the
 146 co-ordination properties of the appropriate element.



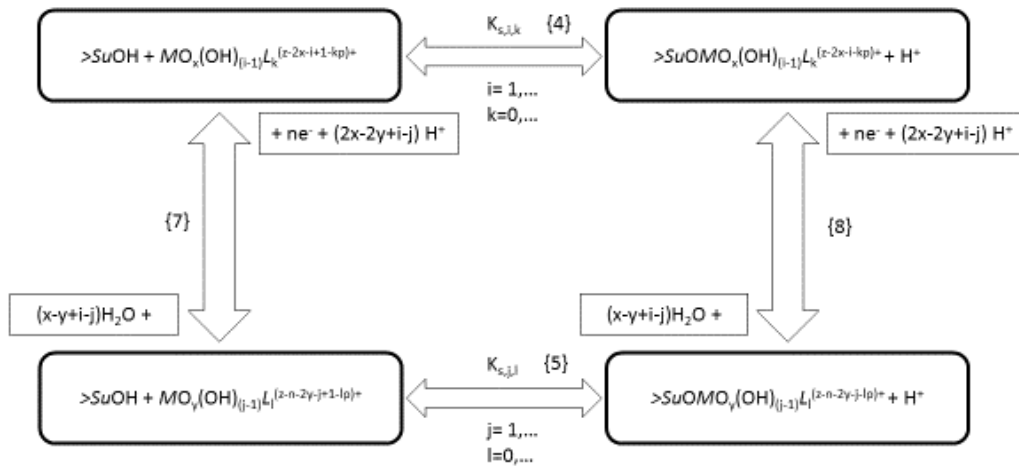
149 The redox couple $MO_x^{(z-2x)^+}/MO_y^{(z-n-2y)^+}$ reaction (where $MO_x^{(z-2x)^+}$ is the oxidised species and
 150 $MO_y^{(z-n-2y)^+}$ the reduced one), is described according to reaction {6}.



152 The surface complexation for the hydrolysed (and complexed) species is described (reactions
 153 {4} and {5}) considering the neutral sites $>SuOH$. The surface complexation constants are $K_{s,i,k}$
 154 for the oxidising species and $K_{s,j,l}$ for the reducing species. Their values are estimated by
 155 correlation with the hydroxo-complex constants (see Section 3.2) using a simple linear
 156 relationship:

157
$$\log K_{s,i} = A + B \log K_i \quad (6)$$

158 With A and B site specific constants. The indices k and l refer to the appropriate co-ordination
 159 number of the metal ions with the selected ligand. Effects of the redox potential in water and at
 160 the surface are also taken into account (reactions {7} and {8}).



162

163 When the reactions are written in terms of free metal M^{z+} , the cumulative constants (hydrolysis)
 164 are β_i and β_j respectively ($\beta_i = \prod K_i$).

165 The ratio between the concentrations of both redox species can be written as a function of the
 166 redox potential (E) applying the Nernst equation (2) for Reaction {7}.

$$167 \quad E = E^\circ + (2x-2y + i - j) \cdot RT \cdot (nF)^{-1} \ln [H^+] + RT \cdot (nF)^{-1} \ln \{ [MO_x^{(z-2x)+}] \cdot [MO_y^{(z-n-2y)+}]^{-1} \} \quad (7)$$

168 where the standard apparent redox potential is $E'^\circ = E^\circ + (2x-2y + i - j) \cdot RT \cdot (nF)^{-1} \ln [H^+]$ in
 169 water. A similar apparent redox potential at the sorbent/water interface E'° may be defined for
 170 Reaction {8}.

171 The K_d , considering surface complexation and including complexation with ligands as
 172 formulated in the above-mentioned equations and reactions, can be written in terms of the redox
 173 potential (Eq. 7).

$$K_d = \frac{\left\{ \sum_{i,k} \left[\frac{K_{s,i,k} \cdot \beta_{i,k} \cdot [L_k]^k}{[H^+]^i} \right] + \sum_{j,l} \left[\frac{K_{s,j,l} \cdot \beta_{j,l} \cdot [L_l]^l}{[H^+]^j} \right] \exp(A) \right\} \cdot \frac{[>SuOH]}{[H^+]}}{\left\{ \sum_{i,k} \left[\frac{\beta_{i,k} \cdot [L_k]^k}{[H^+]^i} \right] + \sum_{j,l} \left[\frac{\beta_{j,l} \cdot [L_l]^l}{[H^+]^j} \right] \cdot \exp(A) \right\} \cdot [part]}$$

174

175 (8)

176 where $A = \frac{(E'_{o} - E) \cdot nF}{RT}$ and $[>SuOH]$ is the free site concentration that can be expressed in
177 terms of the total surface site concentration $[>SuOH]_T$ and the (de)protonation acid dissociation
178 constants. The free ligand concentration $[L]$ also has to be written in terms of the total ligand
179 concentration.

180 The formulation (i.e. Eq. 8) implies linear adsorption isotherms and no saturation effects. No
181 electrostatic effects and no activity corrections were considered at this stage.

182

183

184 **3. Simulation results for uranium speciation and sorption onto particles.**

185

186 **3.1 Revisiting uranium speciation in solution**

187

188 Prior sorption modelling, it is necessary to perform speciation modelling before to draw the
189 uranium pH – E diagrams without and with carbonate.

190 The diagrams are drawn considering all the possible redox couples of U, namely, U(III)/U(IV),
191 U(III)/U(V) and U(III)/U(VI), see Silva *et al.*, (1995). In Table 1 the standard redox potentials
192 reported for these redox couples (Katz *et al.* (1986), actualized OECD (2001)) are presented.

193 The diagram calculation requires the stability constants of hydroxo species which are given in
194 Table 2. Analytical domains are calculated using the data from Table 1 and 2, and an Excel
195 spreadsheet software. Figure 1a presents the uranium pH – E diagrams calculated for a uranium
196 concentration of 1 nM without carbonate ($< 10^{-8}$ M CO_3 total) showing the stability domain of
197 U(IV) and U(VI) in water stability region. The hydroxo- complexes are namely the mono-, di-
198 and tri- hydroxo complexes for U(VI) and the mono-, di-, tri- and tetra-hydroxo complexes for
199 U(IV). It is well established that the regions in which the pentavalent oxidation state of U has

200 been proposed as a significant species are at pH<5. However, no hydrolysis of UO_2^+ would be
 201 expected under these conditions.

202 **Table 1:** Standard redox potentials (E°) for uranium, as recommended by OECD (2001) [20],
 203 Vs SHE. In **bold** data used in this study.

Redox Couple	E° / V
$\text{UO}_2^{2+}/\text{UO}_2^+$	0.0878 ± 0.0013
$\text{UO}_2^{2+}/\text{U}^{4+}$	0.2673 ± 0.0012
$\text{UO}_2^+/\text{U}^{4+}$	0.0447
$\text{UO}_2^+/\text{U}^{3+}$	0.053
$\text{U}^{4+}/\text{U}^{3+}$	-0.553 ± 0.004
$\text{UO}_2^{2+}/\text{U}^{3+}$	0.006

204

205

206 **Table 2:** Equilibrium constants for the hydrolysis of uranium species $[\text{M}^{z+}\text{O}_x](\text{OH})_i^{(z-2x-i)+}$ for
 207 U(III), U(IV), U(V) and U(VI). Note: the values are given for infinite dilution.

	$\log K_{\text{VI}, i, 0}$	$\log K_{\text{V}, i, 0}$	$\log K_{\text{IV}, i, 0}$	$\log K_{\text{III}, i, 0}$
$\log K_{X, i, 0}$	$[\text{UO}_2(\text{OH})_i]^{(2-i)+}$	$[\text{UO}_2(\text{OH})_i]^{(1-i)+}$	$[\text{U}(\text{OH})_i]^{(4-i)+}$	$[\text{U}(\text{OH})_i]^{(3-i)+}$
$\text{LogK}_{X, 1, 0}$	-5.25 ± 0.500 ^b	-11.30 ^b	-0.54 ± 0.060 ^a	-6.80 ± 0.300 ^b
$\text{LogK}_{X, 2, 0}$	-6.9 ^b	-12.30 ^b	-0.70 ^a	-7.30 ^b
$\text{LogK}_{X, 3, 0}$	-8.10 ^b		-3.60 ^a	-11.60 ^b
$\text{LogK}_{X, 4, 0}$	-12.15 ^b		-5.3 ± 0.500 ^a	-14.35 ^b
$\text{LogK}_{X, 5, 0}$	-		-13.10	-

208 ^a Neck & Kim (2001), ^b OECD (2001)

209

210 The data available for the equilibrium constants for the carbonate complexes are presented in
 211 Table 3. Most of the data is based on a semi-empirical model calculation (Neck & Kim (2000)).

212 The stability constants of carbonato and hydroxo carbonato species are also given in Table 3.

213 The uranyl (U(VI)) species are mainly carbonate species while U(IV) species remain hydroxo

214 species. Figure 1b presents the uranium pH – *E* diagrams for 2×10^{-2} M of CO_3 total. Analytical
 215 domains are calculated using the data from Table 1, 2 and 3, and an Excel spreadsheet software.
 216 The pH-*E* diagram calculated for a uranium concentration of 1 nM. In Figure 1b the
 217 predominance pH-*E* diagram reveals that for a carbonate concentration of 2×10^{-2} M, in the
 218 water stability region, the stable oxidation states are U(VI), U(V) and U(IV). The carbonato
 219 complexes are namely the mono-, di- and tri- hydroxo complexes for U(VI) and the hydroxo
 220 complexes are the mono-, di-, tri- and tetra-hydroxo complexes for U(IV). The U(V) does not
 221 form complexes in the pH domain (2-6) for which it is observed

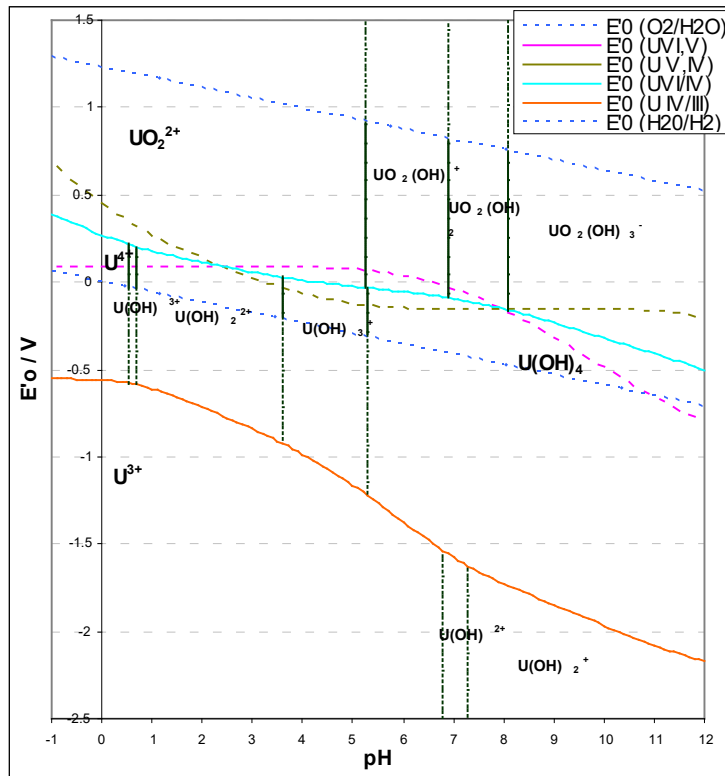
222
 223 **Table 3.** Stability constants for the formation and hydrolysis species of uranium carbonates.
 224 Data selected for $(\text{UO}_2)^{+2}(\text{OH})_i(\text{CO}_3)_j^{(2-i-2j)+}$, $[\text{UO}_2]^+(\text{OH})_i(\text{CO}_3)_j^{(1-i-2j)+}$, $\text{U}^{4+}(\text{OH})_i(\text{CO}_3)_j^{(4-i-2j)+}$,
 225 $\text{U}^{3+}(\text{OH})_i(\text{CO}_3)_j^{(3-i-2j)+}$.
 226

$\log K_{ij}$	U(VI)	U(V)	U(IV)	U(III)
$\log K_{01}$	9.94 ^c	5.120 ^c	13.7 ^b	6.5 ^a
$\log K_{11}$	-	-	-	-5.8 ^a
$\log K_{21}$	-	-	-	-7.9 ^a
$\log K_{02}$	6.67 ^c	1.8 ^c	10.6 ^b	5.3 ^a
$\log K_{12}$	-	-	-	-13.3 ^a
$\log K_{03}$	5.23 ^c	-1.895 ^c	7.6 ^b	1.6 ^a
$\log K_{04}$	-	-	3.3 ^b	-3.4 ^a
$\log K_{50}$	-	-	-1.2 ^b	-

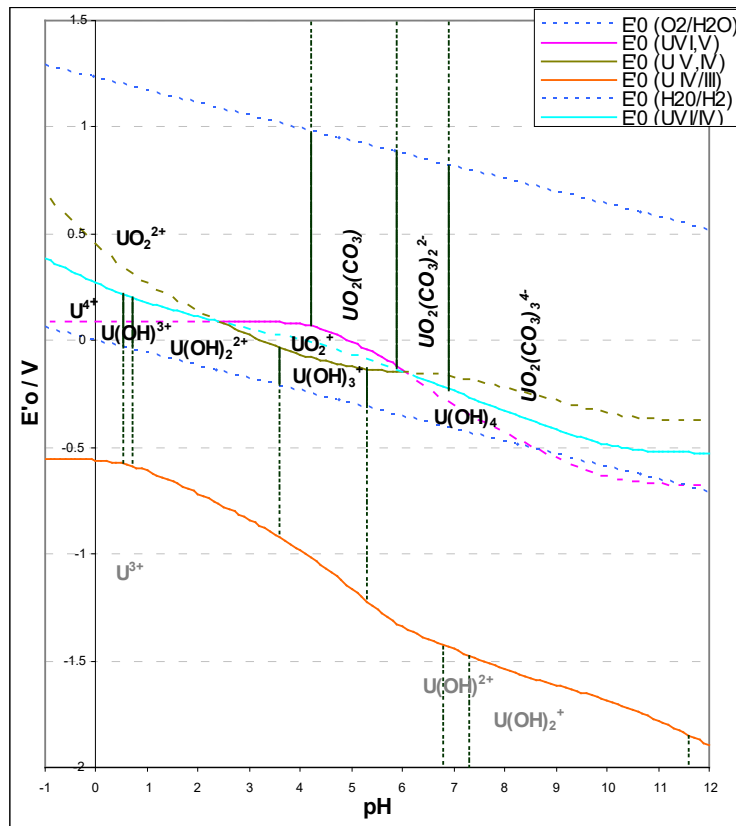
227
 228 ^aData for Am, Hummel et al., (2002); ^bData from Neck *et al.*, (2000); ^c OECD (2003).
 229

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a



b

236
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238
239

Fig. 1: Indicative uranium redox – pH plots for
a carbonate free and
b 2×10^{-2} M carbonate water

240

241 3.2 Simulation results for uranium sorption onto model particles

242

243 The uranium sorption onto Al₂O₃, FeOOH and SiO₂ has been simulated using Eq. 7.

244 The equilibrium constants $\log K_{i,0}$ for the hydrolysed species ($[M^{+z}O_x](OH)_i^{(z-2x-i)+}$) for the U(III),

245 (Degueldre *et al.* (1994), U(IV) (Hummel (2002)), U(V) (Neck *et al.*, (2001)) and U(VI)

246 (Thoenen (2000)) presented in Table 2 are systematically used for the calculations.

247 In Table 4 the correlation used for the calculation of the distribution coefficient of U using Eq.

248 7 for the three selected particulate materials: Al₂O₃, FeOOH and SiO₂, covered with >Al-OH,

249 >Fe-OH and >SiOH sites, are given to apply the methodology suggested earlier Degueldre

250 (1995) and Degueldre (1997). The applied correlations between the surface complexation

251 constants $K_{s,i-1,0}$ and the hydrolysis constants $K_{i,0}$ are the link between hydrolysis and surface

252 complexation. The $\log K_{s,i-1,0} - \log K_{i,0}$ correlations given in Table 4 clearly show that the

253 sorption on Al₂O₃, is stronger than on FeOOH and itself stronger than on SiO₂.

254

255 For the sorption, a site density of 3 nm⁻² e.g. James & Parks (1982); Villalobos *et al* (2004), a

256 particle size of 200 nm (specific surface ~ 10 m² g⁻¹), a particle concentration of 1.7x10⁻³ g l⁻¹

257 and density of 2 g cm⁻³ (arbitrary value) were used for the calculations. Distribution coefficients

258 can be calculated (Eq. 8) using other parametric values. The computations were also performed

259 using Excel spreadsheet software.

260

261

262

263 **Table 4:** Literature data used for the correlations between the surface complexation constants

264 ($K_{s,i-1,0}$) and the hydroxo complex stability constants ($K_{i,0}$) and surface site (>AlOH, >FeOH and

265 >SiOH) (de)protonation of the selected particles (Al₂O₃, FeOOH and SiO₂). Data from Hachyia

266 *et al* (1984) for Al₂O₃, from Balistieri *et al* (1981) for FeOOH and from Righetto *et al* (1991)

267 for SiO₂.

268

	Al_2O_3	FeOOH	SiO_2
$\log K_{s,i-1,0}$	$6.02 + 0.98 \log K_{i,0}$	$3.75 + 0.75 \log K_{i,0}$	$2.00 + 0.65 \log K_{i,0}$
$\text{p}K_{a1}$	5	4	-
$\text{p}K_{a2}$	10	10	7

269

270 The calculated distribution coefficients for uranium onto Al_2O_3 particles (without or with
 271 carbonates) at different pH values are presented respectively in Figs. 2, where the solid lines
 272 indicate values inside the water stability region, while the dotted ones are outside of this area.
 273 Data reported at pH 2 and 12 are indicative; they are limited by eventual leaching that amplify
 274 in more acidic or basic media respectively as discussed in Section 2.2. Basically the domain of
 275 model validity should be between pH values from $\text{p}K_{a1}$ to $\text{p}K_{a2}$ when the $>\text{SuOH}$ group
 276 predominate (see Table 4).

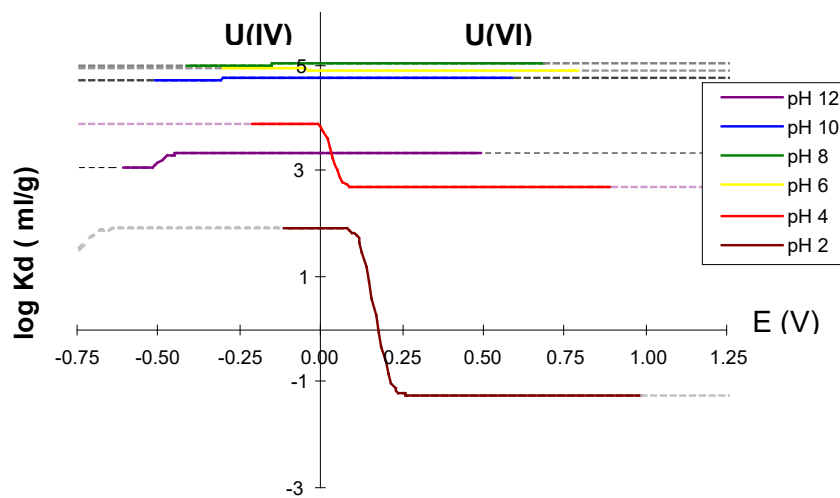
277 At pH 2 in a carbonate free system the redox effect of the U(III)/U(IV) couple is only visible
 278 (see Fig. 2a) around -0.75 V; whilst sorption increasingly above due to U(IV). A decrease is
 279 observed around +0.2 V due to U(VI) formation and its weaker sorption ability. At pH 4 the U
 280 sorption has increased and the U(IV) sorption takes place in reducing conditions (below $E = 0$
 281 V). Hexavalent uranium U(VI) sorbs (weakly) in oxidising conditions. At pH 6 the sorption of
 282 both U(IV) and U(VI) are strong with $\log Kd$ around 5. At pH 8 and 10 the situation is similar.
 283 While at pH 12 sorption has decreased due to uranium speciation ($\text{U}(\text{OH})_5^-$ and $\text{UO}_2(\text{OH})_3^-$
 284 which species does not sorb for stoichiometric reasons.

285

286 In carbonated system (see Fig 2b), the $\log Kd$ vs E plots are marked by the absence of U(IV)
 287 carbonato complexes and the strong formation of U(VI) carbonato-complexes. In reducing
 288 conditions U(IV) sorption reaches $\log Kd$ values of 5 for pH 6 to 10 and decreases for pH 12 in
 289 the same fashion as for dicarbonated systems.

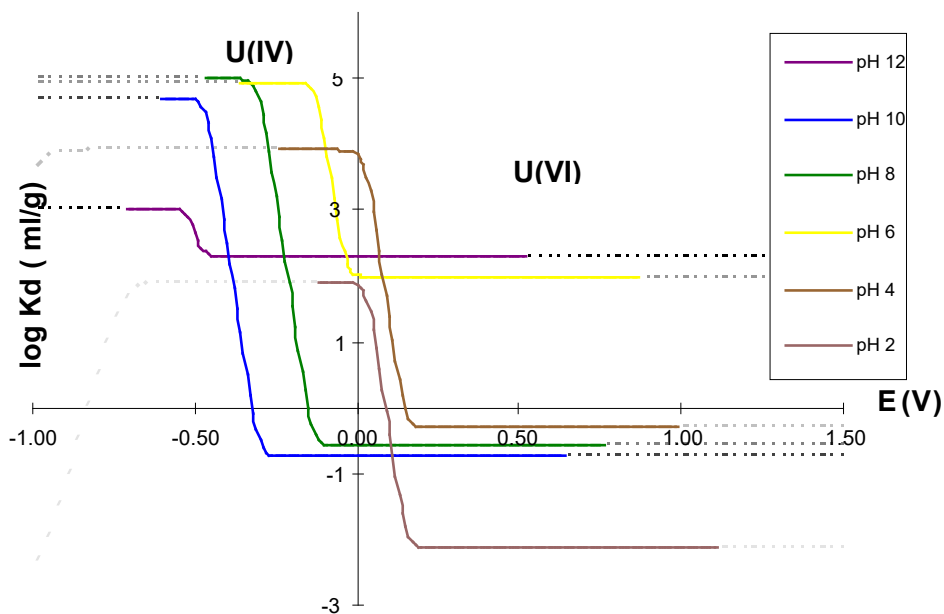
290

291 Fig 2
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 293



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a



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 302

b

Fig 2: Uranium sorption on Al_2O_3 : $\log K_d$ as a function of E and pH.
a carbonate free and
b 2×10^{-2} M carbonate water (indicative data for $pH < 6$)

303 The sorption of U onto **FeOOH** particles can be seen in Fig. 3, the nature of sorbed species is
304 suggested by the redox diagram presented in Fig 1.

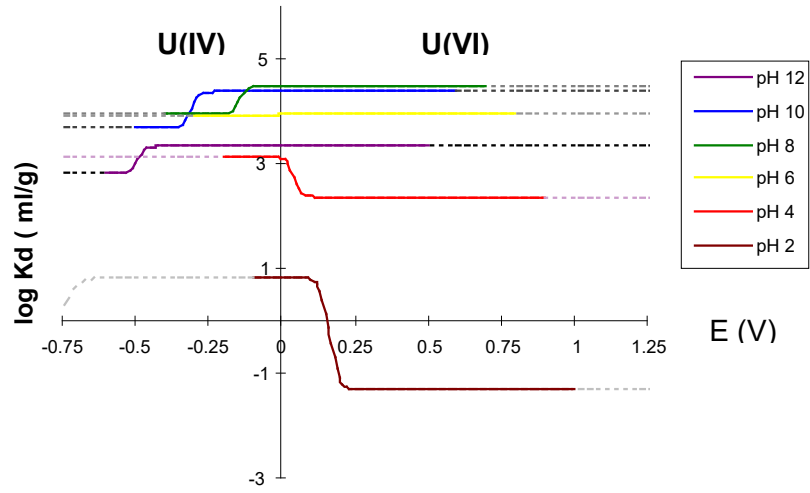
305 At pH 2 in carbonate free system the redox effect of the U(III)/U(IV) couple is only visible (see
306 Fig 3a) around -0.75 V, sorption increases with the E due to U(IV). A decrease is observed
307 around +0.2 V due to the increasing presence of U(VI). At pH 4 the U sorption has increased
308 with the U(IV) sorption taking place in reducing conditions while U(VI) undergoes (weaker)
309 sorption in oxidising conditions. At pH 6 the sorption of both U(IV) and U(VI) are strong with
310 $\log Kd$ around 4.0 to 4.5. At pH 8 and 10 the situation is similar, differentiated only by a slight
311 decrease under reducing conditions. At pH 12 sorption has decreased due to the U speciation
312 ($U(OH)_5^-$ and $UO_2(OH)_4^{2-}$ which do not sorb).

313

314 In carbonate system (Fig 3b), the $\log Kd$ vs E plots are marked by the absence of carbonato
315 complexes of U(IV) and the strong formation of U(VI) carbonato complexes. The $\log Kd$ vs E
316 plots are marked by the absence of U(IV) carbonato complexes and the strong formation of
317 U(VI) carbonato complexes. In reducing conditions U(IV) sorption reach $\log Kd$ values of 5 for
318 pH 6 to 10 and decreases for pH 12 is observed for the reason reported above (limit of
319 validation of our methodology).

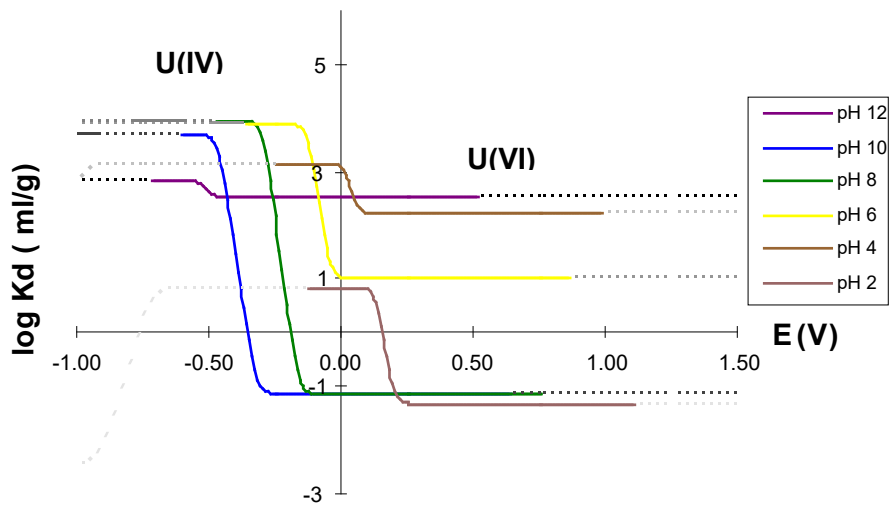
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Fig 3: Uranium sorption on FeOOH: $\log K_d$ as a function of E and pH.
a carbonate free and
b 2×10^{-2} M carbonate water (indicative data for $\text{pH} < 6$)

332

333 The uranium sorption behaviour onto **SiO₂** particles is depicted in Fig. 4. The sorbing species
334 distribution can be guided by the redox diagram presented in Fig 1.

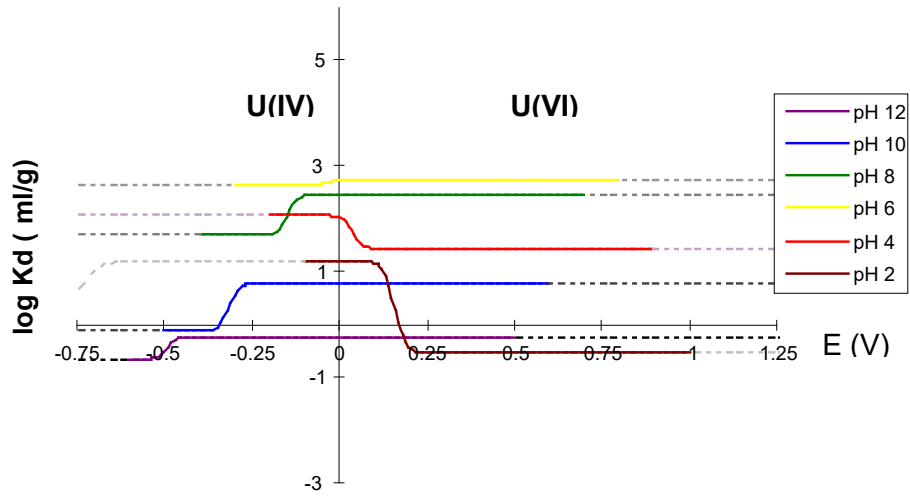
335 At pH 2 in carbonate free system the redox effect of the U(III)/U(IV) couple is also found (Fig
336 4a) around -0.75 V, the increase of sorption with *E* is due to the presence of U(IV). A decrease
337 is observed around +0.2 V due to U(VI). At pH 4 the U sorption has increased and the U(IV)
338 sorption takes place in reducing conditions while U(VI) sorbs (weaker) in oxidising conditions.
339 At pH 6 the sorption of both U(IV) and U(VI) are strong with log *Kd* around 2.0 to 3.0. At pH 8
340 and 10 the situation is similar, a slight decrease is observed in reducing conditions. At pH 12
341 sorption has decreased due to the U speciation (U(OH)₅⁻ and UO₂(OH)₄²⁻ which do not sorb.

342 In carbonate system (Fig 4b), the log *Kd* vs *E* plots are marked by the absence of carbonato
343 complexes of U(IV) and the strong formation of U(VI) carbonato complexes. In reducing
344 conditions U(IV) sorption reach log *Kd* values of 5 for pH 6 to 10 and decreases for pH 12 for
345 the reason reported above.

346

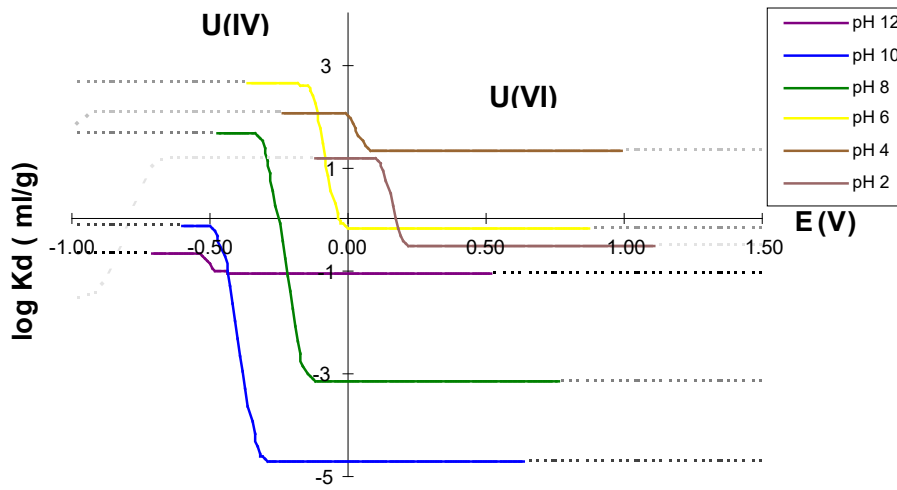
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Fig 4: Uranium sorption on SiO₂: log *K_d* as a function of *E* and pH.

- a** carbonate free and
- b** 2x10⁻² M carbonate water (indicative data for pH<6)

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363 **4. Discussion**

364

365 The main species that drive the sorption on materials are those found in water and those at the
366 surface of the sorbing phase. As displayed in the pH- E diagram of U, these are mainly the
367 U(IV) and U(VI) species that are found in the stability domain of water. The U(III) species may
368 be observed outside the stability domain of water while U(V) may be found marginally, as its
369 concentration in its possible stability domain is low. In practice, the most useful redox
370 parameter is the standard apparent redox potential E° , which is defined as the potential at
371 which in water 50% of the soluble forms are U(VI) and 50% U(IV), or, for the solid 50% of
372 the sorption sites are occupied by U(VI) and 50% by U(IV). These issues had to be examined
373 prior any discussion of the sorption results keeping in mind that the quality of the modelled
374 speciation results is closely linked to the thermodynamic data as discussed by Mühr-Ebert *et al.*
375 (2019).

376

377 **4.1 Speciation in TIC free solution and their effect on sorption**

378

379 The uranium speciation in aqueous solution plays a relevant role. Under normal saline (e.g.
380 NaCl waters) conditions, it complexes from UO_2^{2+} to $[\text{UO}_2(\text{OH})_i]^{2-i}$ according to its pH.
381 Therefore the pH is an important parameter for the species in solution (see Fig.1) and after
382 sorption at the surface of the particles. The log Kd increases from acidic to neutral solution for
383 the 3 model materials and the 200 nm size show that the maximum sorption is observed in the
384 pH domain 6 to 8 (see Table 5). The maximum log Kd increases from SiO_2 2.7 (pH 6, $E > 0$ V)
385 to 5.0 (pH 6 - 8, E [-0.5 - +0.7] V) for Al_2O_3 as could be anticipated from the data displayed in
386 Table 4.

387 In contrast, the standard apparent redox potential E'° in solution is less oxidising at pH 2 than
 388 on the substrates because U(IV) sorbes ($\log Kd > 0$) while U(VI) does not ($\log Kd < 0$). At pH 6,
 389 all E'° values are comparable, and for higher pH the E'° values on substrates become slightly
 390 more negative than that of the solution due to increasing activity of U(VI) compared to U(IV).

391

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395 **Table 5:** Standard apparent redox potential E'° (V vs SHE) of the U(VI)/U(IV) couple in
 396 carbonate free solution and on the studied substrates as well as the $\log Kd$ (Kd 's in mL g⁻¹)
 397 values for U(VI) and U(IV) on these substrates for given pH.

.pH	2	4	6	8	10	12
E'° /Solution	+0.115	+0.026	-0.039	-0.128	-0.295	-0.474
$\log Kd$ U(VI)	-0.54	+1.44	+2.73	+2.47	+0.78	-0.23
E'° /SiO ₂	+0.160	+0.041	-0.028	-0.150	-0.318	-0.505
$\log Kd$ U(IV)	+1.20	+2.06	+2.63	+1.69	-0.12	-0.66
$\log Kd$ U(VI)	-1.32	+2.36	+3.94	+4.49	+4.37	+3.33
E'° /FeOOH	+0.163	+0.051	-0.051	-0.143	-0.296	-0.490
$\log Kd$ U(IV)	+0.83	+3.14	+3.90	+3.94	+3.68	+2.82
$\log Kd$ U(VI)	-1.25	+2.68	+4.90	+5.04	+4.76	+3.32
E'° /Al ₂ O ₃	+0.177	+0.042	-0.052	-0.156	-0.313	-0.490
$\log Kd$ U(IV)	+1.91	+3.91	+4.95	+4.99	+4.70	+3.04

398

399

400 4.2 Speciation in TIC solution and their effect on sorption

401 As for the TIC-free aqueous solution, the uranium speciation in solution plays a central role. It
 402 goes from UO₂²⁺ to UO₂(OH)_i]²⁻ⁱ under saline (NaCl) water conditions, or [UO₂(CO₃)₃]⁴⁻ in
 403 solution with NaHCO₃, potentially [Ca(UO₂)(CO₃)₃]²⁻ and [Ca₂(UO₂)(CO₃)₃] in a Na(Ca)HCO₃
 404 water as reported by Moulin *et al.* (1990). This was confirmed for artificial seawater by Beccia
 405 *et al.* (2017).

406 The largest log Kd values for the 3 model materials and the 200 nm size show that the
 407 maximum sorption is observed in the pH domain 4 to 6 (see Table 6). The maximum log Kd
 408 increases from SiO₂ 2.6 (pH 6, $E < 0V$) to 5.0 (pH 6, $E < 0.1V$) for Al₂O₃. Note that for pH < 6
 409 TIC becomes very small and data are sketched, given in grey, for information.
 410 The standard apparent redox potential E° in solution is less oxidising at pH 2 than on the
 411 substrates because U(IV) sorbes (log $Kd > 0$) while U(VI) does not (log $Kd < 0$). Below pH 6,
 412 TIC is very low. At pH 6, E° values on substrates are slightly more positive than that of the
 413 solution due to larger activity of U(VI) compared to U(IV), and for higher pH the E° values on
 414 substrates remain slightly more positive up to pH 12.

415 **Table 6:** Standard apparent redox potential E° (V vs) of the U(VI)/U(IV) couple in 2×10^{-2} M
 416 carbonated solution and on the studied substrates as well as the log Kd (Kd 's in mL g⁻¹)
 417 values for U(VI) and U(IV) on these substrates for given pH. Data for pH < 6 are sketched.

pH	2	4	6	8	10	12
$E^{\circ}/\text{Solution}$	+0.117	+0.011	-0.128	-0.309	-0.468	-0.521
logKd U(VI)	-0.54	+1.31	-0.19	-3.16	-4.72	-1.04
E°/SiO_2	+0.163	+0.042	-0.081	-0.233	-0.419	-0.500
logKd U(IV)	+1.20	+2.06	+2.62	+1.68	-0.12	-0.66
logKd U(VI)	-1.32	+2.23	+1.02	-1.14	-1.12	+2.52
E°/FeOOH	+0.166	+0.041	-0.097	-0.235	-0.401	-0.525
logKd U(IV)	+0.83	+3.14	+3.89	+3.94	+3.68	+2.82
logKd U(VI)	-2.13	-0.31	+1.98	-0.59	-0.74	+2.28
$E^{\circ}/\text{Al}_2\text{O}_3$	0.185	0.080	-0.080	-0.225	-0.375	-0.500
logKd U(IV)	+1.91	+3.91	+4.94	+4.99	+4.70	+3.01

418

419

420 4.3 Comparison of simulated and experimental sorption data

421

422 In environmental science, sorption has been treated originally as empirical, with data derived
 423 from batch tests and data listed for specific solid and liquid materials e.g. Puls *et al.* (1989).

424 Despite already existing body of works such as (Degueldre *et al.* 1994) applying actinide
425 surface complexation for calculation of distribution coefficients, uranium sorption studies have
426 been reviewed to assess the surface area normalisation for interpreting distribution coefficients,
427 e.g. Payne *et al.* (2011) and completed by suggesting guidelines for thermodynamic sorption
428 modelling in the context of radioactive waste disposal (Payne *et al.* (2013)). There have been
429 some attempts to apply surface complexation for describing the sorption of Am(III) on model
430 Al₂O₃ and SiO₂ as well as on clay particles, **Ref** Alonso & Degueldre (2003). Usually, Am(III)
431 may be considered as an analogue of U(VI) and Th(IV) of U(IV).

432

433 The comparison of the uranium sorption properties on the studied model particles (e.g. 200 nm)
434 of sorbent Fig's 2, 3 and 4 reveals that the uranium sorption onto Al₂O₃ particles is stronger
435 (with a maximum of $\log K_d = \sim 5$) than onto FeOOH (with a maximum of $\log K_d = \sim 4$) or onto
436 SiO₂ particles (with a maximum of $\log K_d = \sim 3$), because different semi-empirical correlations
437 for relating the surface complex constants with the hydrolysed ones (Table 4) were applied
438 driven by decreasing intercept terms (for $\log K_s = 0$). This is presumed to be due to the
439 decrease of electronegativity of the matrix surface structural elements within >Su. Each of the
440 semi-empirical correlations (Table 4), used to evaluate a specific distribution coefficient,
441 relates the surface constants (unknown) with the hydrolysed ones (known). The comparison of
442 experimental sorption data (from the cited literature) with the modelled data using Eq. 8 for the
443 specific case is reported in Table 7.

444

445 The uranium sorption was found to be strong on **alumina** particles. The sorption behavior of
446 uranium was justified by Froideval *et al.* (2006) on the basis of TRLFS and XAFS spectroscopy
447 data identifying strong surface complexes. This sorption can be amplified by the synergism
448 effect of phosphate as reported by Guo *et al.* (2009) and Galindo *et al.* (2010). Guo found
449 U(VI) K_d of 80 mL g⁻¹ ($\log K_d \sim 2$) for a particle specific surface of 130 m² g⁻¹ (corresponding

450 to ~50 nm particles) at pH 4.4. This pH is however below the identified log Kd plateau of
451 U(VI) on alumina but the log Kd value is comparable with its modelled value (Eq. 7). The
452 americium sorption was found to be strong on alumina with log $Kd = 3$ for particle sizes ~50
453 μm and pH 7- 8 by Moulin *et al.* (1992). The Am(III) log Kd is around 3 between pH 6 and 8
454 for specific surface of $0.07 \text{ m}^2 \text{ g}^{-1}$.

455 The binary and ternary surface complexes (hydroxo- carbonato) of U(VI) on the gibbsite/water
456 interface were subsequently studied by Gückel *et al.* (2012) using vibrational and EXAFS
457 spectroscopy. The U concentration is rather high and uranium dimers complexes are observed.
458 This work was completed by Müller *et al.* (2013) investigating by in situ spectroscopy the
459 surface reactions of U(VI) on $\gamma\text{-Al}_2\text{O}_3$ up to the transition from surface complexation to surface
460 precipitation as studied for Th(IV) by Degueldre & Kline (2007) for Th(IV). These reactions
461 (dimer- polymer- formation and surface precipitation) enhance the Kd values.

462 The reversibility of uranium and thorium binding on a modified bauxite refinery residue was
463 investigated Clark *et al.* (2015). These authors found Kd values of 3000 mL g^{-1} in the pH above
464 4 and below 7. Finally, Mei *et al.* (2015) reported about the effect of silicate on U(VI) sorption
465 to $\gamma\text{-Al}_2\text{O}_3$. However this batch study focusing mainly on U EXAFS, the U(VI) concentration is
466 quite high ($6 \times 10^{-5} \text{ M}$) for $1 \text{ g l}^{-1} \gamma\text{-Al}_2\text{O}_3$ colloids ($d \sim 20 \text{ nm}$) which saturates the sites and which
467 reduces apparently sorption (excess soluble) with an apparent log $Kd = 3.3$.

468 The approach followed for Al_2O_3 model particles may be applied for the sorption of U onto
469 montmorillonite and illite particles that have strongly reactive aluminol groups ($>\text{AlOH}$) on the
470 edges (Degueldre *et al.*, 1994). On montmorillonite, Bradbury & Baeyens (2005) found log $Kd =$
471 5.3 at pH 7 for particle sizes $<500 \text{ nm}$ (e.g. 200 nm) which also is comparable with our
472 modelling result see Table 7. To complete the picture, Marques Fernandes, *et al* (2012) studied
473 the sorption of U(VI) on montmorillonite in the absence and presence of carbonate and
474 observed that the sorbed U(VI) fraction decreases with the carbonate concentration.

475

476 Uranium has also been investigated on **iron oxo-hydroxide** substrates. Murphy *et al.* (1999)
477 reported about the sorption of thorium (IV) and uranium (VI) to hematite in the presence of
478 natural organic matter. On 9 g l^{-1} $66 \text{ nm Fe}_2\text{O}_3$ they found 50% sorption at pH 4 or a log Kd of
479 about 2.0 while modelling (with Eq. 7) predicts $\log Kd = 1.5$; the equilibrium is however not
480 reached in these tests. Similarly, Missana *et al.* (2003) investigated experimentally and by
481 modeling the U(VI) sorption on goethite. They found log Kd of 5.2 for goethite needles of
482 $50 \times 50 \times 5000 \text{ nm}$ ($d \sim 1000 \text{ nm}$) at $\text{pH} > 5$. Similar work was also performed by the same group
483 (Missana *et al.* (2003)) with U(VI) sorption on **magnetite** particles under anoxic environment.
484 For batch data (pH 4, 100 nm colloids, $M/V = 2 \text{ g l}^{-1}$, $[\text{U(VI)}] = 4 \times 10^{-7} \text{ M}$) Values of log Kd (3.3)
485 are calculated from the batch data (pH 4, 100 nm colloids) and compared to the modelled one
486 (3.2) for 200 nm particles, for sorbed U(VI) the log Kd would be 2.5. This indicates that
487 reduction can take place during surface complexation. Wang *et al.* (2015) investigated the
488 sorption of U(IV) on magnetite. Values of log Kd (3.3) are calculated from the batch data (pH
489 4, 100 nm colloids, $M/V = 2 \text{ g l}^{-1}$, $[\text{U(IV)}] = 10^{-8} \text{ M}$) and compared to the modelled one (3.2) for
490 200 nm particles.

491 Uranium partitioning tests were also performed on ferrihydrite by Hiemstra *et al.* (2009), by
492 Foerstendorf *et al.* (2012) and more recently by Dublet *et al.* (2017). Dalvi *et al.* (2014) found
493 that the Th(IV) / U(VI) Kd ratio was of the order of 17 (± 5) between pH 7.78 and 8.42 for
494 sediment samples. This is very difficult to compare the results gained with the proposed model
495 at pH 8 (see Fig. 2,3,4) because the calculation results are very sensitive with carbonate
496 concentration and this data is not fixed in Dalvi *et al.* (2014).

497

498 Finally, sorption work of uranium was also carried on **SiO₂**. Dent *et al.* (1992) reported on a
499 EXAFS study of uranyl ion in solution and sorbed onto **silica** and montmorillonite clay

500 colloids. On 80 nm silica colloids, at pH 4 the experimental log K_d was found to be 2.5 and the
501 modelled data using Eq.8 gives a log K_d of 2.8 for the data describe earlier and for pH 4. Table
502 7 presents other results from Dent et al (1992)[55] and the modelled log K_d data for
503 comparison.

504 Since Th(IV) can be considered as an analogue of U(IV) one can also report the work of
505 Östhols (1995) on thorium sorption on amorphous silica to support the data. Quartz that is less
506 sorbing that silica was investigated by Froideval *et al.* (2003). The U(VI) sorption on silica was
507 also more recently tested for its effect by complexing anions by Kar *et al.* (2012). On silica like
508 on other substrate materials, phosphorous derived groups may act as specific ligand such as
509 silica-tethered phosphonic acid sorbents for uranium species from aqueous solution as
510 investigated by Dudarko *et al.* (2015).

511 Finally, Stamberg, *et al* (2003), also studied uranyl ion sorption on silica of mesoporous nature.
512 They also applied surface complexation modeling to investigate the processes occurring in the
513 batches focusing on the effect of carbonate. Without carbonate at pH 7.5, 98.6% uranium sorbed,
514 while with 0.015 M carbonate the sorption dropped to 88.2% on the porous silica.

515

516

517 **Table 7:** Comparison of the $\log Kd_e$ (± 0.5) experimental and $\log Kd_m$ (Kd 's in mL g^{-1})
 518 modelled for the studied sorbing materials (size, particle; density 2 g cm^{-3} , site density 3
 519 nm^{-2} , * clay) and solution of given pH, TIC.

Substrate M (g l^{-1})	An(X)	pH	TIC (M)	Size (nm)	$\log Kd_e$	Log Kd_m	Conditions Size (nm)	References
Al_2O_3	U(VI)	4.4	-	50	2.0	2.8	pH 4	Guo et al (2009)
Al_2O_3	Am(III)	6-8	-	50,000	3.0	3.2	20,000 pH 6	Moulin et al (1992)
Al_2O_3	U(VI)	6	-	(20,000)	3.3	3.0	20,000 pH 6	Clark et al (2015)
>AlOH*	U(VI)	7	-	(200)	3.3	3.0	200 pH7	Bradbury et al (2005)
>AlOH*	U(VI)	6	-	(200)	3.3	3.0	200 pH 8	Marques et al (2012)
>AlOH*	U(VI)	8	5×10^{-3}	(200)	1.5	0.0	200 pH 8	Marques et al (2012)
FeOOH	U(VI)	>5	-	1000	5.2	4.5	200	Missana et al (2005)
Fe_3O_4	U(VI)	4	-	100nm	3.3	3.2	200	Missana et al (2005)
Fe_3O_4	U(IV)	4	-	100nm	3.3	3.2	200	Wang et al (2011)
SiO_2	Am(III)	6-8	-	50,000	2.5	2.8	200	Moulin et al (1992)
5000 SiO_2	U(VI)	4	-	80	2.5	2.8	200	Dent et al (1992)
5000 SiO_2	U(VI)	6	-	80	4	2.9	200	Dent et al (1992)
500 SiO_2	U(VI)	4	-	30	3.1	2.4	20	Dent et al (1992)
5000 SiO_2	U(VI)	4	-	30	2.8	2.4	20	Dent et al (1992)

520

521 In the case of **composite** minerals, the above studied methodology can be applied. This is
 522 confirmed in Manoj *et al.* (2020) work, $\log Kd$ increases up to pH 6 after a plateau it gradually
 523 decreases for higher pH (see data in Tables 5 and 6). Their $\log Kd$ values are lower than us
 524 because their particle sizes are larger than our model particles. One important body of work to
 525 note concerning redox reactions of uranium at the surface of inorganic sorbents is the work of
 526 Descorte *et al.* (2010). It concerns direct reduction in the context of **pyrite** interaction with
 527 U(VI). In this case data show a maximal cation uptake above pH 5.5. Concentration isotherms

528 for U(VI) sorption on pyrite indicate specific behaviours. In the U(VI) case, sorption seems to
529 occur on two different sites with a total saturation concentration of $4.5 \times 10^{-8} \text{ mol g}^{-1}$. At lower
530 concentration, uranyl reduction occurs in U(IV), limiting the concentration of dissolved
531 uranium to the solubility of $\text{UO}_2(\text{s})$ and the formation of a hyperstoichiometric $\text{UO}_{2+x}(\text{s})$. The
532 results are consistent with a chemistry of the pyrite surface governed by S groups which can
533 either sorb cations and protons, or sorb and reduce redox-sensitive elements such as U(VI).

534 To complete this study it must be mentioned that the model presented is unfortunately not
535 designed to deal with uranium sorption on calcite. This is due to co-precipitation and formation
536 of specific Ca-UO₂-CO₃ phases that are identified by advanced spectroscopic techniques such
537 as EXAFS e.g. Reeder *et al.* (2004), Elzinga *et al.* (2004). However, Butchins *et al.* (2006)
538 found that uranium has a high affinity for calcite over a wide range of initial uranium
539 concentrations (10^{-12} to 10^{-3} M) with $20 < K_d < 90 \text{ (ml g}^{-1}\text{)}$. The authors however do not specify
540 the pH and the particle size of the material. In addition, Sturchio *et al.* (1998) reported on
541 tetravalent uranium in calcite using XAFS and micro-XAS.

542 Field studies were conducted by Curtis *et al.* (2004) in an alluvial aquifer at a former U mill
543 tailings site, by suspending approximately 10 g samples for periods of 3 to 15 months.
544 Adsorbed U(VI) on these samples was determined by extraction. In situ K_d values calculated
545 from the measurements of adsorbed and dissolved U(VI) ranged from **0.50 to 10.6 mL g⁻¹** and
546 the K_d values decreased with increasing groundwater alkalinity. Curtis *et al.* (2004) found a
547 good agreement between the predicted K_d 's from surface complexation modeling and from
548 measured in situ K_d values.

549 Experimental and modelled log K_d data are comparable. However, the quality of data is
550 affected by their precision and accuracy. The main factors that are relevant for data calculation
551 are the site density which may vary from 1 to 10 nm^{-2} , the state of the surface since the bulk
552 composition (density) may be different from the surface (contaminations by other active groups
553 than the expected one) and the uncertainty in the reported particle size. Actually, particles are

554 seldom mono-dispersed but poly-dispersed and their size distributions are not always accurately
555 surface weighted. Particle specific surfaces are currently determined by gas sorption however
556 these derived data are not provided by ionic sorption.

557 The model applied considers also the correlation between the stepwise hydrolysis constants and
558 the stepwise surface complexation constants. It is consequently impossible to calculate the
559 surface complexation constant for the last hydrolysed species. The lack of surface constants in
560 the calculations limits the applicability of the model in the high pH range where the last
561 hydrolysed species is predominant (justifying our pH upper limit to 12), but in spite of this
562 limitation the model gives satisfactory results in a wide range of conditions.

563 Uranium contamination of soil has been a major concern with respect to its toxicity and
564 persistence in the environment, Selvakumar *et al* (2018). Owing to these problems, remediation
565 of uranium-contaminated soils has been investigated by various techniques and the authors
566 hope that this study can help to remediate contaminated sites.

567

568 **5. Conclusions**

569

570 A model that relates the distribution coefficient with the redox potential was developed for
571 evaluating the effect of the redox potential on the sorption of uranium onto model substrates.
572 The model includes surface complexation and complexation with ligands. It also considers the
573 effect of the redox potential for all the species at the surface and in solution. The model was
574 applied to uranium, as an important safety relevant redox sensitive element, and the calculated
575 distribution coefficient values confirmed that the redox potential does affect the sorption of U
576 in the site stability domain and in the water stability region and outside. The calculated values
577 are in relative agreement with scarce experimental values reported in the literature. This model is
578 applicable to other redox sensitive elements.

579 The sorption analysis so far provides good predictive values for a limited subset of the
580 experimental data, allowing approximate predictive modelling of the partition coefficients for a
581 variety of groundwaters. Such data may help to understand the formation of ore deposits (U(VI)
582 => U(IV)) or contribute to search a versatile U extraction protocol from seawater. Effect of
583 organics shall be discussed in a future study. This last target would require to expanding the
584 variety of absorption substrate being considered.

585 Finally, work is to be undertaken to represent oxidation/reduction systems within the
586 modelling, to represent reductive deposition on the surfaces to complete U sorption by UO₂
587 precipitation onto the substrate.

588

589 **Appendices**

590 Six "logKd Vs E" EXCEL spreadsheets are included: 3 for carbonate free solutions and 3 for
591 carbonate solution. They concern Kd calculations for the sorption of U on Al₂O₃, FeOOH and
592 SiO₂. Each spreadsheet includes sub-sheets for pH: 0, 2, 4, 6, 8, 10 and 12, as well as one
593 resume. Each pH sub-sheet presents the detailed data calculations. The resumes sub-sheet
594 present the "logKd Vs E" graphs for pH 2 to 12 for the substrates and for the carbonated
595 solution conditions.

596

597 **References**

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