

Optimized split-flow deflector design for airflow drying systems using BP neural network coupled with NSGA-II algorithm

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Abstract: The non-uniform distribution of hot airflow and the high intensity of turbulence critically affect the effectiveness of airflow drying systems. In this study, numerical simulations were conducted to analyze the internal flow field characteristics of an airflow dryer. A novel split-flow deflector plate structure was designed and optimized using Response Surface Methodology (RSM) integrated with a backpropagation (BP) neural network and the NSGA-II algorithm. The results indicated that the designed split-flow deflector structure demonstrated superior performance compared with conventional arc-shaped designs. The optimized performance was achieved with a rotation speed of 190 r/min, deflector plate angle of 92°, and split-flow plate length of 380 mm. Compared to both the arc-shaped and pre-optimized configurations, the optimized split-flow deflector increased average airflow velocity by 4% and 39.2% and improved the airflow uniformity index by 11.8% and 14.5%, respectively. Furthermore, transient thermal analysis confirmed enhanced thermal stability as the outlet

26 temperature rapidly converges to the experimental benchmark (160°C), effectively mitigating
27 thermal oscillations and intensifying gas-solid heat exchange. The findings provide both
28 theoretical insight into the dynamic control of particle flows in dryers and a practical basis for
29 the structural optimization of industrial airflow drying equipment.

30 **Keywords:** Airflow dryer; Structural optimization; Airflow uniformity; BP Neural network;
31 NSGA-II

32 **1. Introduction**

33 Drying equipment is extensively applied across diverse sectors, including food processing^[1],
34 pharmaceuticals^[2], chemical engineering^[3], and agriculture^[4]. These systems primarily utilize
35 hot airflow to remove moisture efficiently, thereby enhancing both product quality and
36 production efficiency. Depending on the underlying drying principles and specific application
37 requirements, various configurations have been developed. Based on the heat source, common
38 classifications include airflow drying^[5], solar drying^[6], and heat pump drying^[7]. Among these,
39 airflow drying is particularly favored due to its compact design, high heat transfer efficiency,
40 rapid drying rate, and strong operational adaptability^[8]. However, in practical applications,
41 airflow dryers experience non-uniform distribution of hot air within the drying chamber. This
42 uneven airflow leads to inconsistent heating and moisture removal across the material, causing
43 variations in moisture content and localized agglomeration. Such issues detrimentally affect
44 drying uniformity and ultimately compromise product quality consistency.

45 Improving airflow uniformity has become a major focus and persistent challenge in modern
46 dryer research. Amjad et al. ^[9] conducted simulation studies on three distinct grain turner designs,
47 revealing that a serrated structure significantly improved drying uniformity and dehydration
48 efficiency. Chen et al. ^[8] designed and optimized an air distribution system for a microwave–
49 infrared–hot air combined dryer. It was found that the drum-bed structure improved airflow

50 uniformity by 52.1%. Li et al. ^[10] investigated the effects of various airflow supply modes on
51 sludge drying behavior and reported that a bottom-up flow combined with lateral auxiliary
52 airflow substantially enhanced the drying efficiency and airflow uniformity. Ross et al. ^[11]
53 focused on the spatial uniformity of the microwave field in a hybrid microwave-hot air dryer,
54 effectively mitigating local overheating. Lan et al. ^[12] developed a CFD–DEM–IBM model to
55 simulate gas–solid two-phase behavior in fluidized bed drying, demonstrating a high accuracy
56 in predicting complex flow field uniformity. Recent studies indicated that conventional drying
57 equipment frequently experienced uneven airflow distribution and material agglomeration.
58 Nevertheless, these challenges can be effectively addressed through internal structural
59 optimization and the integration of multi-field coupling designs, leading to improved flow
60 uniformity and enhanced drying performance.

61 Introducing internal deflector plate structures has proven to be an effective strategy for
62 improving the flow field uniformity in drying systems. Gai et al. ^[13] analyzed nine types of baffle
63 configurations in a heat pump cabinet dryer, where the optimized design improved the airflow
64 and the temperature uniformity by 52.7% and 85.3%, respectively, significantly enhancing the
65 consistency and quality of fruit drying. Ahmad et al. ^[14] demonstrated that installing windbreak
66 deflector plates in poultry house ventilation systems markedly enhanced the uniformity of both
67 airflow and temperature distribution. Lv et al. ^[15] integrated V-shaped deflector plates into a
68 microwave–hot air vibration dryer, reducing the air velocity variation from 1.1 m/s to 0.36 m/s
69 and thereby substantially improving flow uniformity. Cao et al. ^[16] achieved improved airflow
70 deflection and system uniformity by installing rectangular deflectors at the outlet of perforated
71 air ducts and optimizing outlet angles. Wang et al. ^[17] enhanced airflow uniformity in drying
72 chambers by adjusting deflector configurations in the air distribution chamber and adding
73 deflector plates between material layers. Sabyasachi et al. ^[18], through CFD analyses, designed
74 deflector screens with varying porosities; the optimal configuration improved airflow uniformity

75 by 64% in a fiber dryer, increasing the yield of high-quality fibers by 5%. Liu et al. [19] proposed
76 a V-shaped perforated deflector that enhanced airflow uniformity by approximately 30%
77 compared to conventional designs. Collectively, these studies highlighted the pivotal role of
78 internal deflector structures in optimizing airflow distribution within drying systems.

79 The optimization of deflector structure parameters is inherently complex, often involving
80 nonlinear, multi-objective problems. Artificial Neural Networks (ANNs) have gained
81 widespread application in recent years due to their effectiveness in addressing structural
82 optimization challenges across various engineering domains^[20-22]. Notably, the Back
83 Propagation (BP) neural network is particularly well-suited for establishing nonlinear mapping
84 relationships between input design variables and output performance metrics^[23]. For instance,
85 Le et al. ^[24] combined a deep neural network with the artificial hummingbird algorithm to
86 analyze the influence of material properties, thickness, and strain gradient parameters on the
87 optimal design of functionally graded micro-scale structures. Zhang et al. ^[25] developed a
88 surrogate strength model via a BP neural network to capture the nonlinear relationship between
89 design parameters and structural response, subsequently integrating a genetic algorithm with
90 reliability theory for multi-objective optimization. Similarly, Qi et al. ^[26] employed ANN-based
91 optimization to refine the geometric parameters of a biomimetic shark skin riblet heat exchanger,
92 achieving significant enhancements in airflow distribution and heat transfer performance.

93 The Genetic Algorithm (GA) was widely recognized for its effectiveness in optimizing the shape
94 of deflector structures^[27], while the improved Non-dominated sorting genetic algorithm II
95 (NSGA-II) reduces computational complexity and achieves superior Pareto-optimal solutions^[28].
96 The integration of the Back Propagation (BP) neural network with NSGA-II synergistically
97 enhances model accuracy, minimizes trial-and-error costs, and accelerates the design process.
98 This hybrid approach had been extensively applied to structural parameter optimization
99 problems across diverse engineering fields^[29-31]. For example, Liu et al. ^[32] employed the BP-

100 GA method to optimize L-shaped joints in composite sandwich structures, achieving a
101 maximum relative error below 8% between predicted and experimental results, thereby
102 substantially improving load-bearing capacity and stiffness. Jin et al. ^[33] developed a multi-
103 objective optimization model based on an artificial neural network and utilized NSGA-II to
104 optimize geometric parameters of an intercooler, resulting in a 20.2% enhancement in system
105 energy efficiency. Subsequently, Jin et al. ^[34] incorporated a BP neural network surrogate within
106 the NSGA-II framework for optimizing heat dissipation structures, yielding significant
107 improvements in heat transfer performance. Fu et al. ^[35] applied NSGA-II to optimize multiple
108 geometric parameters of a jet impingement cooling system, enhancing thermal performance
109 while reducing pressure drop. Additionally, Xie et al. ^[36] compared the predictive capabilities of
110 BP, GA-BP, and Support Vector Regression (SVR) models for evaluating the thermal
111 performance of solar cavity receivers, demonstrating that the GA-BP model achieved the highest
112 prediction accuracy. Collectively, these studies underscored the effectiveness of the BP-GA
113 hybrid approach in addressing complex nonlinear, multi-objective parameter optimization
114 challenges.

115 To summarize, uneven airflow distribution and thermal instability within drying equipment
116 significantly impair drying quality, highlighting the necessity of deflector structure optimization
117 for improving overall process stability and drying efficiency. This study investigates airflow
118 dryers by proposing a novel split-flow deflector plate and analyzing its impact on internal flow
119 characteristics and gas-solid heat exchange. Employing a D-optimal design of experiments, key
120 structural parameters including the left deflector plate angle, split-flow plate size, and rotation
121 speed were systematically varied, and corresponding performance metrics such as airflow
122 uniformity index and average velocity were compared. Utilizing these datasets, a Back
123 Propagation (BP) neural network coupled with the NSGA-II algorithm was developed to model
124 the nonlinear relationships between structural parameters and performance indicators. Crucially,

125 transient thermal analysis was integrated to verify the improvements in thermal stability and
126 temperature convergence of the optimized structure. The resulting optimization identified the
127 deflector configuration that maximizes airflow uniformity and intensity, thereby providing an
128 effective strategy to enhance the drying quality of materials.

129 **2. Physical and Mathematical Models**

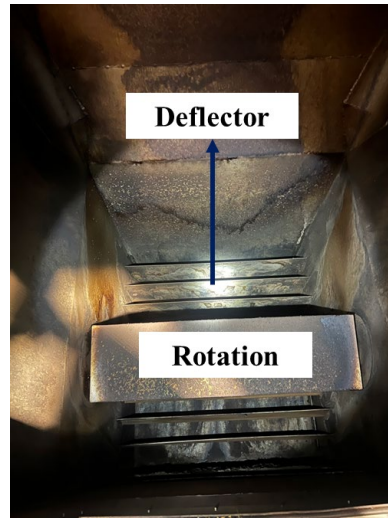
130 **2.1 Structural Design of the Airflow Dryer**

131 The physical structure of the SH23A airflow dryer is presented in Figure 1, where Figure 1(b)
132 specifically details the internal original arc-shaped deflectors. Based on these structural
133 characteristics, three three-dimensional models were developed: a baseline model without any
134 deflector structure, a model featuring the original arc-shaped deflector plates, and a model
135 incorporating the proposed split-flow deflector structure, as illustrated in Figure 2. Figure 2(a)
136 depicts the original dryer configuration, wherein arc-shaped deflector plates are evenly spaced
137 within the drying chamber, while Figure 2(b) presents the optimized split-flow deflector design.
138 In this arrangement, a distribution roller driven by a motor rotates to evenly disperse the material
139 inside the chamber. Simultaneously, heated air enters through the inlet and is redirected upward
140 to facilitate drying.

141 To clarify the specific airflow mechanism of the optimized design, the detailed working principle
142 is illustrated in Figure 3. In this novel configuration, the inlet hot air is mechanically bifurcated
143 by a horizontal split-flow plate. One portion of the airflow is guided through a series of small
144 semi-circular deflectors to ensure uniform dispersion, while the remaining portion is directed by
145 conventional angled deflectors. Crucially, the length of the split-flow plate serves as a vital
146 governing parameter; it determines the volumetric distribution of hot air between the left and
147 right regions, thereby directly influencing the overall flow field balance.



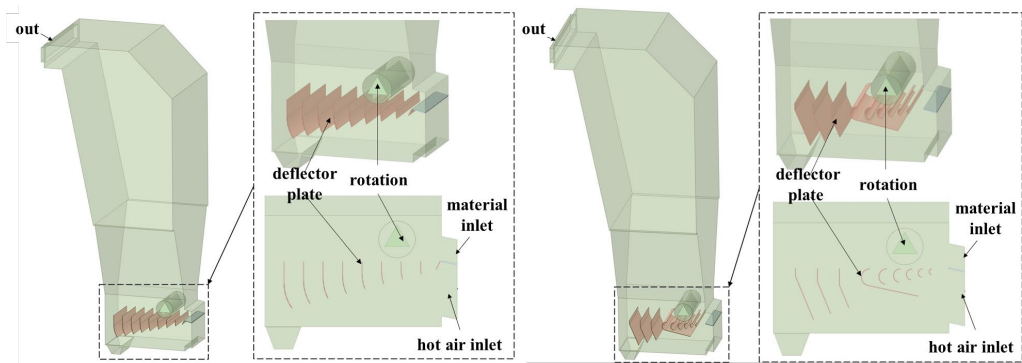
(a) photograph of the SH23A dryer



(b) internal view of the original arc-shaped deflectors

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Figure 1. Physical structure of the airflow dryer

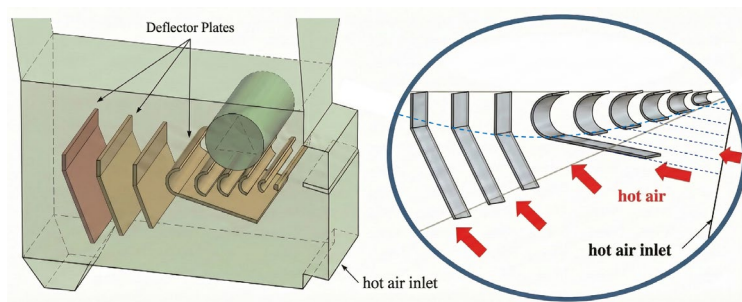


(a) Airflow dryer with original deflector structure

(b) Airflow dryer with split-flow deflector structure

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Figure 2. Three-dimensional models of the airflow dryer



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Figure 3. Schematic diagram illustrating the design principle of the split-flow deflector structure.

152 **2.2 Mathematical Model and Boundary Conditions**

153 **2.2.1 Governing Equations**

154 Given the high complexity of the drying process involving hot air and shredded tobacco within
155 the airflow dryer, the following reasonable assumptions are made to simplify the analysis:

156 (1) The fluid is treated as an incompressible gas with constant density ρ . This simplification is
157 adopted because the maximum airflow velocity corresponds to a mach number well below 0.3,
158 and the relative density variation caused by the temperature drop (approx. 20°C) and species
159 mixing during the stable operating phase is less than 5%, which is considered negligible for the
160 flow field analysis;

161 (2) The drying process involves coupled heat and mass transfer. Therefore, the energy equation
162 is incorporated to solve for the temperature field. The moisture content and temperature of the
163 material change during the process, while the particle shape is assumed to remain constant to
164 simplify the tracking;

165 (3) The ambient pressure is uniform and constant.

166 To characterize the internal flow behavior and thermal characteristics, and moisture transport
167 within the dryer, the conservation equations for mass, momentum, energy, and species transport
168 are employed. In the momentum equations, body forces are neglected, and only the viscous
169 effects of air are considered. The incompressible Navier–Stokes (N–S) equations govern the
170 flow analysis, while the energy conservation equation and species transport equation are
171 introduced to solve for the temperature field and moisture distribution, respectively.

172 As hot air enters the drying chamber, it generates a complex flow field influenced by the
173 deflector plates. Notably, significant turbulence, swirl, and flow separation occur near the
174 deflector surfaces. To accurately resolve these complex flow characteristics, the Realizable k - ϵ

175 turbulence model is applied. Near-wall turbulence is modeled using standard wall functions. The
 176 continuity equation for incompressible flow is expressed as:

$$177 \quad \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = S_m \quad (1)$$

178 where S_m is the mass source term due to moisture evaporation from the particles.

179 Momentum Conservation Equation:

$$180 \quad \rho \left(\frac{\partial \bar{\mathbf{u}}}{\partial t} + \bar{\mathbf{u}} \cdot \nabla \bar{\mathbf{u}} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}_{pf} \quad (2)$$

181 The energy conservation equation is expressed as:

$$182 \quad \frac{\partial(\rho h)}{\partial t} + \nabla \cdot (\rho \mathbf{u} h) = \nabla \cdot (\lambda \nabla T) + S_h \quad (1)$$

183 Turbulent kinetic energy equation:

$$184 \quad \frac{\partial(\rho k)}{\partial t} + \nabla \cdot (\rho k \mathbf{u}) = \nabla \cdot \left[\left(\mu + \frac{\mu_t}{\sigma_k} \right) \nabla k \right] + G_k - \rho \varepsilon \quad (2)$$

185 Dissipation rate equation:

$$186 \quad \frac{\partial(\rho \varepsilon)}{\partial t} + \nabla \cdot (\rho \varepsilon \mathbf{u}) = \nabla \cdot \left[\left(\mu + \frac{\mu_t}{\sigma_\varepsilon} \right) \nabla \varepsilon \right] + \rho C_1 S \varepsilon - \rho C_2 \frac{\varepsilon^2}{k + \sqrt{\nu \varepsilon}} \quad (3)$$

187 Species transport equation:

$$188 \quad \frac{\partial(\rho Y_i)}{\partial t} + \nabla \cdot (\rho \mathbf{u} Y_i) = -\nabla \cdot \mathbf{J}_i + S_i \quad (4)$$

189 **2.2.2 Governing Equations for the Discrete Phase**

190 In the Lagrangian frame of reference, the motion and thermodynamic state of the tobacco
 191 particles are tracked individually. The trajectory of a discrete phase particle is predicted by
 192 integrating the force balance on the particle (Newton's second law).

193 Particle motion equation:

$$194 \quad \frac{d\mathbf{u}_p}{dt} = F_D(\mathbf{u} - \mathbf{u}_p) + \frac{\mathbf{g}(\rho_p - \rho)}{\rho_p} + \mathbf{F}_{other} \quad (5)$$

195 where \mathbf{u}_p is the particle velocity, \mathbf{u} is the fluid velocity, and F_D is the drag force per unit
196 particle mass.

197 Heat and mass transfer equations:

$$198 \quad m_p c_p \frac{dT_p}{dt} = h_{conv} A_p (T_\infty - T_p) + \frac{dm_p}{dt} h_{fg} \quad (6)$$

199 where h_{conv} is the convective heat transfer coefficient, A_p is the particle surface area, h_{fg}

200 is the latent heat of vaporization, and $\frac{dm_p}{dt}$ represents the rate of moisture evaporation.

201 2.2.3 Boundary Conditions

202 Air at atmospheric pressure enters the computational domain through the designated air inlet.

203 The particulate phase, representing the material particles, is characterized by a density of 120
204 kg/m³ and a particle diameter of 2 mm. In the simulation, the initial velocity of the particles is
205 assumed to be equal to that of the inlet gas phase. The detailed inlet boundary conditions are
206 summarized in Table 1.

207 Air at atmospheric pressure enters the computational domain through the designated air inlet.

208 The particulate phase, specifically representing shredded tobacco, is characterized by a density
209 of 120 kg/m³ and a particle diameter of 2 mm, parameters selected based on actual factory
210 production data. In the simulation, the initial velocity of the particles is assumed to be equal to
211 that of the inlet gas phase. The inlet velocities are derived from the mass flow rates and the
212 cross-sectional areas of the inlets. The detailed inlet boundary conditions, including temperature

213 and geometric parameters, are summarized in Table 1.

214 Table1. Inlet boundary conditions

Boundary	Temperature (°C)	Inlet Area (m ²)	Flow rate (kg/h)	Velocity (m/s)	Boundary type
Hot air inlet	180	0.5	51450	23.34	Velocity inlet
Material inlet	180	0.1814	1600	2.00	Velocity inlet

215 The gas-phase outlet boundary is modeled as a fully developed flow condition, with the outlet
216 section extended both vertically and horizontally to ensure complete flow development. The
217 outlet boundary is specified as a pressure outlet. For the particulate phase, the outlet boundary
218 condition is defined as escape, permitting particles to exit the computational domain freely.

219 No-slip boundary conditions are imposed on all solid surfaces. For the dryer walls, deflector
220 plate surfaces, and the bottom surface of the dryer, the discrete phase boundary condition is set
221 to reflect, enabling particle rebound upon collision. Near-wall turbulence is addressed using an
222 enhanced wall function approach. The turbulent viscosity ratio is a dimensionless quantity
223 representing the ratio of turbulent to molecular viscosity (μ_t / μ), indicating the degree of
224 turbulence development. The boundary conditions utilized in the simulation is detailed in Table
225 2.

226 Table 2. Boundary conditions and parameters

Boundary condition	Parameter	Boundary condition	Parameter
Turbulence intensity at material inlet (%)	2.90	Turbulence intensity at hot air inlet (%)	2.61
Turbulent viscosity ratio at material inlet	9.68	Turbulent viscosity ratio at hot air inlet	1968

227 2.3 Numerical Solution Approach

228 The airflow inside the dryer is modeled as an unsteady, viscous flow to capture the transient

229 behavior of the drying process accurately. To simulate this, a time-dependent solver is employed,
230 which allows for the dynamic evolution of the flow field and interaction with the internal
231 structures such as deflector plates. The governing Navier–Stokes equations, coupled with the
232 energy conservation equation, species transport equation, and discrete phase model (DPM), are
233 solved iteratively at each time step to account for the complex, time-varying flow phenomena.
234 A two-way coupling scheme is adopted to account for the exchange of mass, momentum, and
235 energy between the continuous airflow and the discrete tobacco particles.

236 Pressure–velocity coupling, a critical component in incompressible flow simulations, is handled
237 using the SIMPLE algorithm. This algorithm efficiently resolves the coupling by iteratively
238 correcting the pressure and velocity fields to satisfy the continuity equation, ensuring mass
239 conservation throughout the domain. The transient approach is particularly important in this
240 study because the interaction of hot airflow with the rotating distribution roller and deflector
241 plates generates unsteady flow patterns that cannot be captured through steady-state simulations.
242 This approach allows for a detailed investigation of turbulence fluctuations, flow separation, and
243 recirculation zones that directly influence drying uniformity and efficiency.

244 In terms of numerical discretization, the spatial terms in the governing equations are discretized
245 to ensure both accuracy and stability of the simulation. Diffusion terms, which represent viscous
246 and conductive transport, are discretized using a second-order central difference scheme. This
247 scheme provides a balanced and accurate approximation by considering the values at
248 neighboring grid points symmetrically, minimizing numerical diffusion and preserving the
249 physical fidelity of the gradients. For convection-dominated terms, such as those in the density
250 momentum, energy, turbulence quantities, and species transport equations, a second-order
251 upwind scheme is applied. The upwind discretization improves numerical stability by biasing
252 the differencing in the direction of the flow, which helps to prevent non-physical oscillations
253 and ensures robust convergence, especially in turbulent and high-velocity regions. To determine

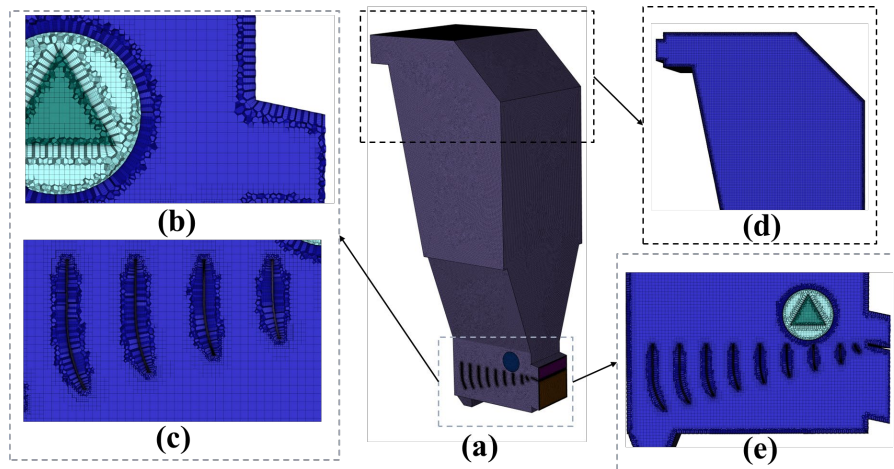
254 the end of each iterative time step, a convergence criterion based on the residuals of the
255 governing equations is imposed, with a threshold of 1×10^{-5} for all residuals. This ensures that
256 the numerical errors are sufficiently minimized before advancing in time, leading to stable and
257 reliable simulation results.

258 **2.4 Grid Independence Verification**

259 Prior to initiating the numerical simulations, it is crucial to verify that the mesh resolution does
260 not significantly influence the accuracy of the results. While increasing the number of mesh cells
261 generally enhances solution precision by better resolving flow features, it also substantially
262 raises computational time and resource requirements. To achieve an optimal balance between
263 accuracy and efficiency, a grid independence study was conducted.

264 Figures 4 and 5 illustrate the hexcore mesh topology employed for the airflow dryer, featuring
265 a hybrid structure of hexahedral cores and tetrahedral transitions. To capture complex flow
266 gradients, local refinement was applied in critical regions. Figure 4 details the grid distribution
267 for the original arc-shaped deflector, while Figure 5 presents the optimized split-flow
268 configuration. Specifically, Figure 5(b-e) highlights the generation of 12 prism inflation layers
269 adjacent to both the deflector surfaces and the dryer inner wall. This structural arrangement
270 ensures the precise resolution of near-wall velocity gradients and turbulent boundary layer
271 effects, while meeting the requirements of standard wall functions.

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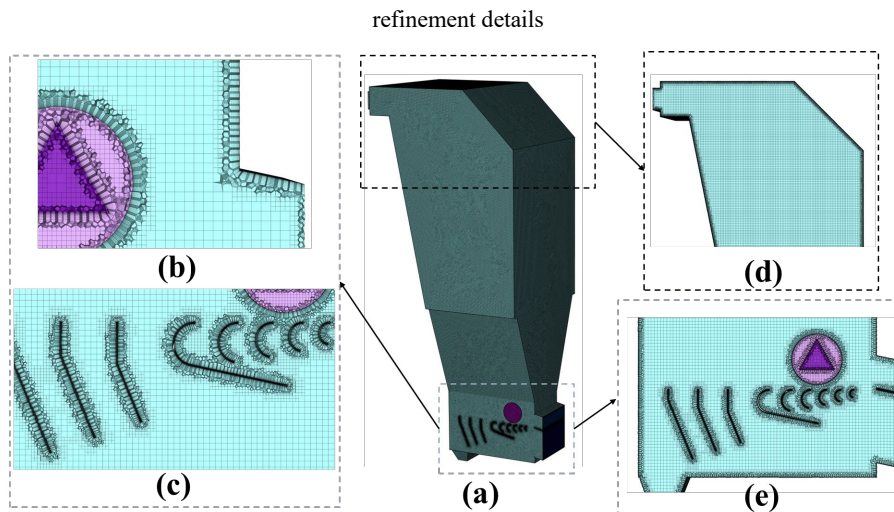


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Figure 4. Hexcore mesh topology for the original arc-shaped deflector: (a) Global view; (b–e) Local

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Figure 5. Detailed mesh for the optimized split-flow deflector: (a) Global view; (b–e) Prism inflation layers

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and near-wall refinement

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For this verification, simulations are performed using the split-flow deflector plate configuration,

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and the uniformity index—an important metric reflecting the consistency of airflow

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distribution—is evaluated at three representative cross-sections located 1 meter (section a), 2.5

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meters (section b), and 4.9 meters (section c) downstream from the distribution roller. The

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uniformity index at these sections is monitored while systematically increasing the total number

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of mesh cells. The results, summarized in Table 3, demonstrate the effect of mesh refinement on

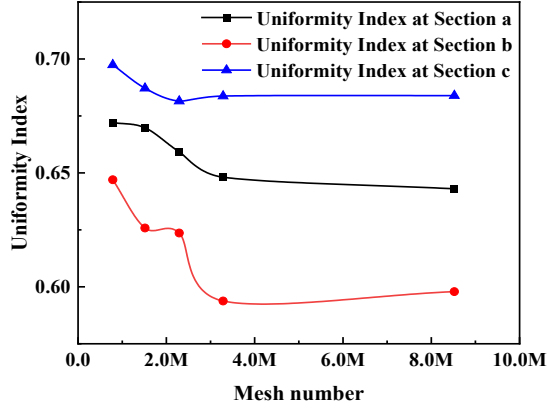
285 predicted airflow uniformity.

286 As depicted in Figure 6, the relative difference in the uniformity index between the solutions
287 with approximately 3.28 million and 8.52 million mesh cells is less than 5%, indicating that
288 further mesh refinement yields only marginal improvements in accuracy. Based on these
289 observations, a mesh size of about 3.28 million cells is chosen for all subsequent simulations.
290 This choice ensures that the numerical results are reliable and sufficiently independent of mesh
291 size while maintaining computational efficiency, thereby enabling detailed and cost-effective
292 analysis of the airflow dynamics and optimization of the deflector plate design.

293 Furthermore, to ensure the applicability of the standard wall functions used in conjunction with
294 the Realizable k - ϵ turbulence model, the non-dimensional wall distance y^+ was strictly
295 monitored. For the selected mesh configuration (approx. 3.28 million cells), the first-layer grid
296 height near the deflector surfaces was set to 0.5 mm. Post-processing inspection confirms that
297 the average y^+ value on the deflector walls is maintained within the valid range of 30 to 300,
298 with an area-weighted average of approximately 104 in high-velocity regions. This range
299 perfectly satisfies the logarithmic law requirements of the standard wall function, ensuring
300 accurate resolution of the turbulent boundary layer effects without demanding excessive
301 computational resources.

302 Table 3. Results of grid independence verification

Mesh number	Uniformity index at a	Uniformity index at b	Uniformity index at c
786344	0.672	0.646	0.697
1515245	0.669	0.625	0.687
2292031	0.659	0.623	0.681
3285826	0.648	0.593	0.683
8523286	0.642	0.597	0.683



303

304

Figure 6. Grid independence verification

305 **2.5 Evaluation of Flow Field Uniformity**

306 To evaluate the uniformity of the airflow inside the dryer and quantitatively analyze the
 307 distribution characteristics of the deflector plate structure, relevant indicators related to airflow
 308 uniformity and flowability are introduced. The average velocity is calculated by the following
 309 formula:

$$310 \quad \overline{|\mathbf{u}|} = \frac{\int_A |\mathbf{u}(x, y)| dA}{\int_A dA} \approx \frac{\sum_i |\mathbf{u}_i| A_i}{\sum_i A_i} \quad (7)$$

311 Where, $|\mathbf{u}(x, y)| = \sqrt{u^2 + v^2 + w^2}$ is the velocity magnitude at each point on the cross-
 312 section.

313 The uniformity index evaluation metric can comprehensively reflect the velocity distribution
 314 characteristics across the entire flow cross-section. It has the advantages of strong comparability
 315 and wide applicability. The expression for γ_v is:

$$316 \quad \gamma_v = 1 - \frac{1}{2n} \sum_{j=1}^n \frac{\sqrt{(v_j - \bar{v})^2}}{\bar{v}} \quad (8)$$

317 In the equation, the uniformity index \mathcal{U}_v ranges from 0 to 1. A higher value of \mathcal{U}_v indicates
318 better flow uniformity. When $\mathcal{U}_v=1$, it represents an ideal uniform flow condition; when \mathcal{U}_v
319 $=0$, it means the fluid passes through only one measurement point. Both of these are hypothetical
320 conditions and do not occur in practical situations. Here, \bar{V} denotes the average velocity over
321 the cross-section, and V_j represents the velocity at each measurement point.

322 **2.6 Multi-Objective Optimization Process of deflector Structure Parameters**

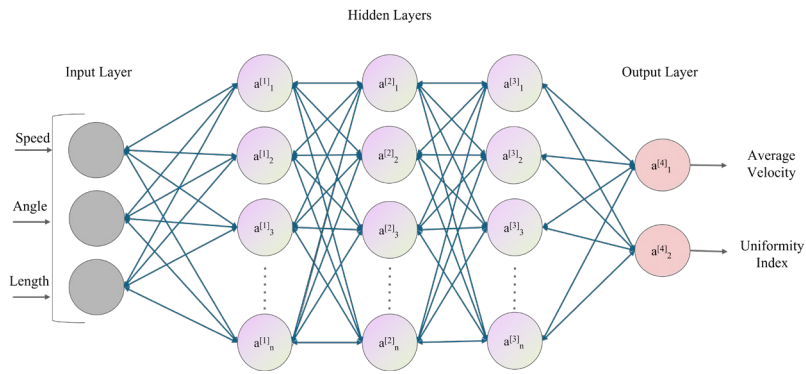
323 The Backpropagation (BP) neural network is a topological multi-layer feedforward network
324 trained using the error backpropagation algorithm. Compared with classic neural network
325 frameworks, such as single-layer perceptrons which are limited to linearly separable problems,
326 the BP model demonstrates superior advantages in non-linear mapping capabilities and self-
327 adaptive learning. By utilizing gradient descent to minimize the error between predicted and
328 actual outputs, the BP network can theoretically approximate any complex continuous function
329 with arbitrary precision. This characteristic is particularly critical for this study, as the
330 aerodynamic relationship between the deflector structural parameters and the internal flow field
331 uniformity is inherently coupled, non-linear, and difficult to describe using explicit analytical
332 equations.

333 In this study, a multi-layer BP neural network model featuring three hidden layers is developed
334 to predict and optimize the performance of the airflow dryer based on key structural parameters
335 of the deflector system. The neural network's input layer comprised the three critical design
336 variables: the angle of the left-side deflector plate, the length of the split-flow plate, and the
337 rotation speed of the distribution roller. These input parameters are essential because they
338 directly influence the airflow patterns and drying efficiency within the chamber. The output layer
339 of the network consists of two key performance indicators: the airflow uniformity index and the

340 average airflow velocity inside the drying chamber. These indicators are chosen because they
341 effectively reflect the quality of the airflow distribution and the drying performance, respectively.

342 To determine the optimal number of neurons in the hidden layer, the Hecht–Nelson empirical
343 method is applied as an initial theoretical reference. With $n=3$ input variables, the baseline
344 recommendation is 7 neurons. However, considering the high complexity and strong
345 nonlinearity of the turbulent flow field inside the dryer, a larger capacity is often required to
346 ensure prediction accuracy. Therefore, based on the theoretical baseline and determined through
347 extensive iterative trial-and-error testing, the number of neurons is increased to 11 for each of
348 the three hidden layers. This specific configuration (3-11-11-11-2) is found to provide the
349 optimal balance, effectively capturing high-dimensional nonlinear relationships while avoiding
350 overfitting and excessive computational complexity. The detailed architecture of the BP neural
351 network is graphically depicted in Figure 7.

352 To enhance the predictive accuracy and convergence speed of the BP neural network, a genetic
353 algorithm (GA) is utilized to optimize the network's weights and biases. GA is a population-
354 based stochastic optimization technique inspired by natural selection and evolutionary biology.
355 This integration helps overcome the BP network's sensitivity to initial parameters and reduces
356 the likelihood of becoming trapped in local minima during training. The entire optimization
357 framework combining BP and GA is implemented using MATLAB. Further, to address the
358 multi-objective nature of the deflector design problem, aiming to simultaneously maximize
359 airflow uniformity and velocity, the Non-dominated sorting genetic algorithm II (NSGA-II) was
360 employed.



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Figure 7. Structure diagram of BP neural network

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A comprehensive flowchart of the combined BP–NSGA-II optimization process is presented in

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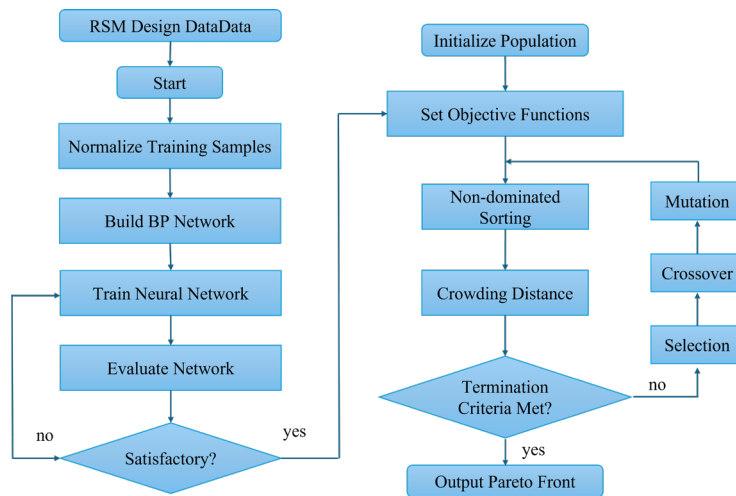
Figure 8, This flowchart outlines the sequential steps starting from population initialization,

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fitness evaluation via the BP model, non-dominated sorting, selection, crossover, mutation, and

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finally termination.



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368

Figure 8. Flowchart of BP-GA structure

369

The hybrid approach effectively utilizes the predictive power of the neural network with the

370

global search capability of NSGA-II, facilitating an efficient exploration of the design space and

371

identification of optimal deflector structure parameters. This methodology offers a robust

372

framework for enhancing dryer performance through intelligent structural optimization.

373 **3. Results and Discussion**

374 This chapter presents a comprehensive analysis of the airflow dryer's performance and structural
375 optimization. The discussion is systematically organized into three main phases. First, the
376 internal flow dynamics, thermal behavior, and particle drying characteristics are evaluated for
377 different deflector configurations. Second, a multi-objective optimization framework combining
378 RSM, BP neural network, and NSGA-II is implemented to determine the optimal structural
379 parameters. Finally, the predicted optimal structures are rigorously validated through
380 experimental comparison and detailed simulation analysis, confirming their superiority in
381 enhancing airflow uniformity, particle dispersion.

382 **3.1 Analysis of Flow Field Simulation Results**

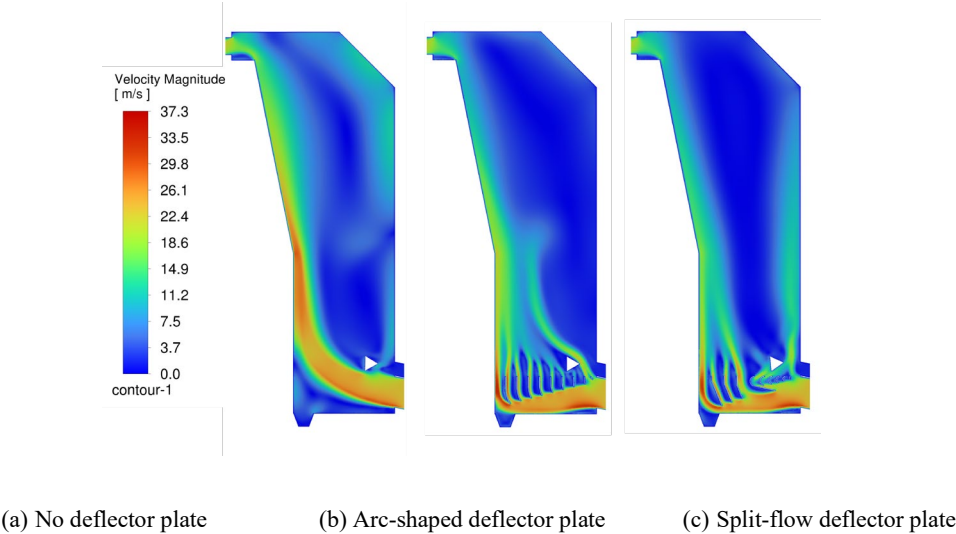
383 To evaluate the optimized split-flow design, comparative simulations are conducted against
384 baseline structures. The analysis focuses on aerodynamic characteristics and turbulence intensity,
385 thermal behavior, particle drying dynamics, and experimental validation, as detailed in the
386 following subsections.

387 **3.1.1 Velocity Field Characteristics under Different Deflector Structures**

388 Figure 9 presents the velocity contours of the internal flow field within the airflow dryer under
389 three different deflector configurations. As shown in Figure 9(a), after entering through the inlet,
390 the material particles mix with the hot air, and the velocity distribution is relatively uniform
391 before entering the main chamber. However, in the corner region, the mixed flow collides with
392 the wall surface, causing the airflow to shift toward the left side of the chamber. This leads to a
393 significant reduction in velocity in the central and right regions, forming a pronounced
394 recirculation zone. As a result, the overall flow field becomes non-uniform, and the airflow
395 uniformity is relatively poor. Figure 9(b) shows that after incorporating the arc-shaped deflector
396 structure, the hot air is more evenly directed toward the upper region of the chamber by the

397 deflector plates. These improve the overall drying performance; however, local recirculation
398 zones remain and are not entirely eliminated. In Figure 9(c), the introduction of the split-flow
399 deflector structure further improves the hot airflow distribution. The size of the recirculation
400 zones is noticeably reduced, the dispersion of material particles becomes more uniform, and
401 agglomeration is effectively alleviated.

402 Using the split-flow deflector structure (parameters: $n=230$ r/min, $\theta=90^\circ$, $d=400$ mm), the
403 average airflow velocity across five cross-sections on the XZ plane changed by +1.3%, +4.9%,
404 -6.0%, -8.3%, and -0.4% compared with the original structure. Correspondingly, the airflow
405 uniformity index increased by 12.6%, 12.7%, 3.8%, 4.0%, and 3.6%, respectively. These results
406 indicate that the split-flow deflector structure provides notable improvements in enhancing
407 airflow uniformity within the dryer.



408 Figure 9. Airflow velocity contours under three different deflector structures

409 **3.1.2 Comparative Analysis of Particle Spatial Distribution and Motion Behavior**

410 Figures 10 and 11 illustrate the spatial distribution and motion trajectories of particles within the
411 dryer under two different deflector structures. As shown in Figure 10, in the original structure,

412 particles are mainly concentrated on the right side of the dryer. After entering with the airflow,
413 they rapidly settle and accumulate in the lower region of the chamber. Local recirculation zones
414 and low-velocity stagnation areas are also observed, resulting in a relatively limited distribution
415 range. In contrast, the split-flow deflector structure significantly improves particle flow behavior.
416 The particle trajectories are more widely distributed within the drying chamber, with more
417 dispersed motion in both vertical and horizontal directions. Recirculation is effectively mitigated,
418 indicating that the structure enhances the spatial coverage of particle motion and promotes better
419 contact with the hot air for drying.

420 Figure 11 further compares the particle distribution characteristics of the two structures in the
421 XY plane. Under the original configuration, particles are mainly concentrated in the middle-
422 lower region with relatively unidirectional flow. Localized stagnation zones with low velocities
423 are evident. However, under the split-flow deflector structure, the particle trajectories cover the
424 entire cross-sectional area more uniformly. Airflow directionality is improved, and the overall
425 flow field becomes more homogeneous and coherent. This contributes to reducing particle
426 deviation and avoiding problems such as localized over-drying or insufficient drying.

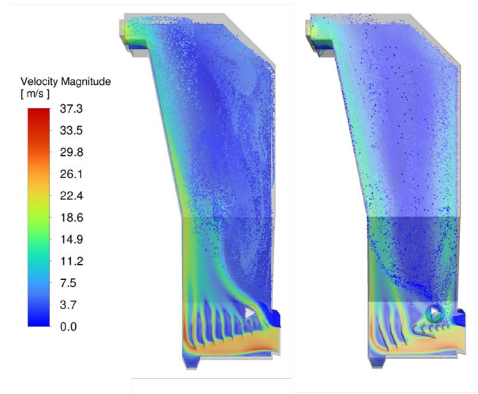


Figure 10. Particle distribution in the YZ plane for two airflow dryer structures

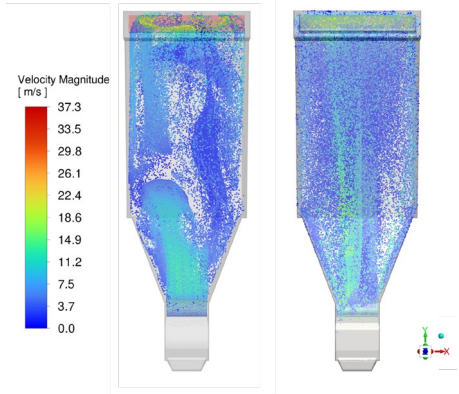


Figure 11. Particle distribution in the XY plane for two airflow dryer structures

427 Figures 12 and 13 compare the frequency distributions of particle residence time for the original
 428 and split-flow deflector configurations, respectively. As seen in Figure 12, the original structure
 429 shows a wide range of residence times, which reflects the presence of extensive turbulent zones
 430 and inefficient circulation regions. Consequently, particles experience prolong or irregular
 431 trajectories before exiting the chamber. Such conditions can lead to uneven drying with some
 432 particles being overexposed to hot air while others receive insufficient exposure. In contrast,
 433 Figure 13 demonstrates that the introduction of the split-flow deflector substantially narrows the
 434 residence time distribution. The majority of particles fall within the 1.0-2.5 s range, with
 435 markedly fewer particles experiencing extreme short or long residence durations. The
 436 corresponding frequency curve is smoother and more symmetrical, indicating a reduction in
 437 anomalous particle paths and a greater consistency in residence time. This behavior suggests
 438 that particle migration becomes shorter and more concentrated, thereby enhancing the stability
 439 and predictability of the drying process.

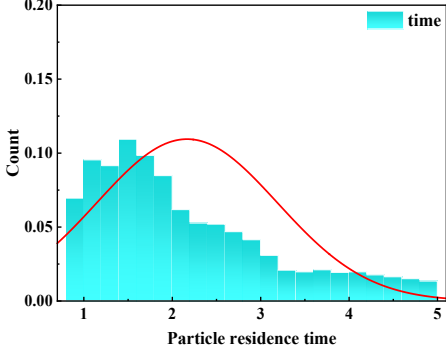
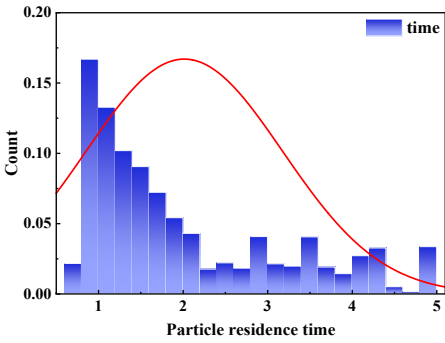


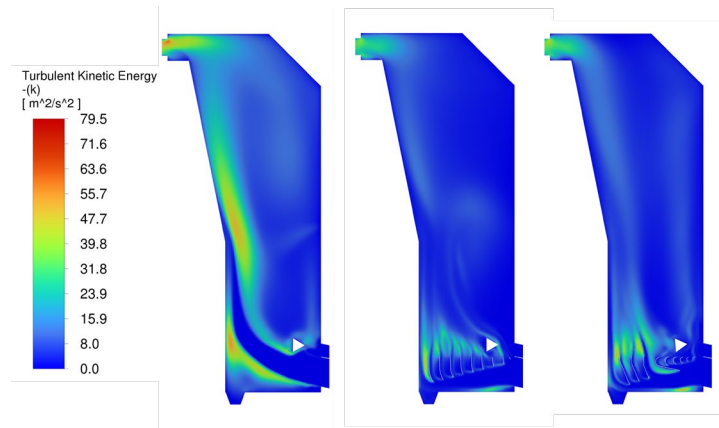
Figure 12. Residence time frequency distribution of particles in the original airflow dryer structure

Figure 13. Residence time frequency distribution of particles in the split-flow airflow dryer structure

440 **3.1.3 Evaluation of Turbulent Kinetic Energy Distribution and Flow Field Disturbance**
 441 **Characteristics**

442 Figure 14 compares the distribution characteristics of turbulent kinetic energy (TKE) under three
443 different deflector structures and evaluates their influence on flow field stability. In the structure
444 without deflectors, the maximum TKE reaches $61.4 \text{ m}^2/\text{s}^2$. High-TKE regions are primarily
445 concentrated near the wall surfaces, forming distinct energy dissipation zones that reduce overall
446 flow stability. With the arc-shaped deflector structure, the maximum TKE increases to
447 $75.57 \text{ m}^2/\text{s}^2$, while the area of high-TKE regions is the smallest among the three cases. This
448 suggests that the arc-shaped structure can effectively concentrate turbulent energy, although
449 local flow separation phenomena are still observed. The split-flow deflector configuration
450 exhibits the highest maximum TKE, reaching $79.5 \text{ m}^2/\text{s}^2$. Owing to its multi-channel flow-
451 splitting design, turbulent energy is more uniformly distributed throughout the chamber. This
452 configuration maintains sufficient turbulence intensity to promote effective particle dispersion,
453 while simultaneously improving the flow stability by preventing excessive localized energy
454 concentrations.

455 The results indicate that the split-flow deflector structure increases the maximum TKE by 29.5%
456 compared to the structure without deflectors, while simultaneously reducing the area of
457 ineffective turbulence regions by 60%. Although the arc-shaped deflector effectively limits the
458 spread of TKE, its overall turbulence intensity is lower than that of the split-flow structure,
459 which may compromise drying performance. Therefore, the split-flow configuration enables
460 more efficient use of turbulent energy, thereby contributing to improved drying efficiency.



(a) No deflector plate (b) Arc-shaped deflector plate (c) Split-flow deflector plate

461

Figure 14. TKE contours under three different deflector structures

462 3.1.4 Analysis of Temperature Field and Drying Characteristics

463 The evaluation of thermal uniformity and particle motion figures 15 and 16 present a
 464 comparative analysis of particle temperature distributions in the YZ and XY planes, respectively.
 465 In the structure with the original arc-shaped deflector, the temperature field exhibits significant
 466 non-uniformity. As observed in the figures, the particle distribution is dominated by yellow
 467 regions, indicating that a large portion of the material remains at a medium temperature level
 468 and fails to reach the optimal heating state. Specifically, the airflow velocity in the left region of
 469 the chamber is relatively low. This insufficient aerodynamic force causes some particles to settle
 470 or move sluggishly, hindering effective heat exchange with the hot air. Furthermore, a distinct
 471 phenomenon is observed near the wall surfaces where particles tend to overheat due to
 472 prolonged contact time caused by local stagnation, which poses a potential risk to material
 473 quality.

474 In contrast, the optimized split-flow deflector structure significantly improves thermal
 475 performance. The particles throughout the chamber exhibit a uniform high-temperature
 476 distribution, primarily represented by red and orange colors. This indicates that the split-flow

477 design effectively eliminates the low-velocity zones and ensures that hot air fully penetrates the
478 particle stream. Crucially, the improved flow aerodynamics significantly reduce the tendency of
479 particles to adhere to the wall surfaces. This reduction in wall attachment minimizes the risk of
480 localized overheating and material blockage, thereby ensuring both consistent heating and safer
481 operation.

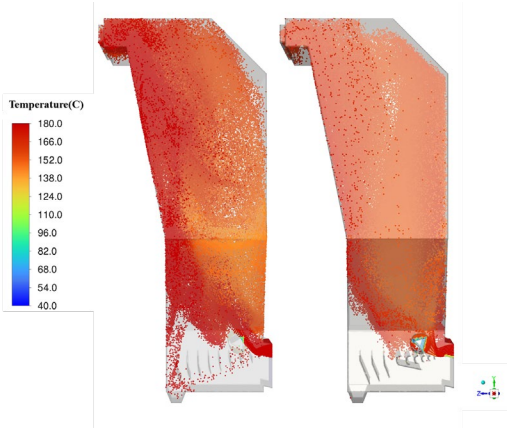


Figure 15. Comparative particle temperature profiles in the YZ plane

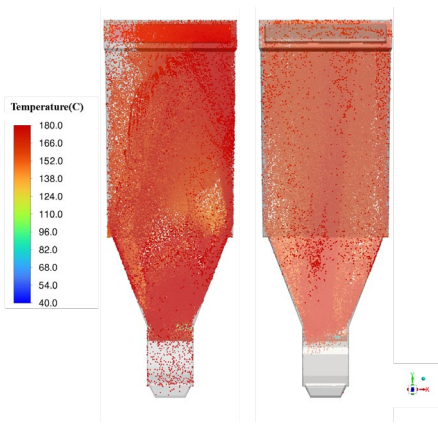
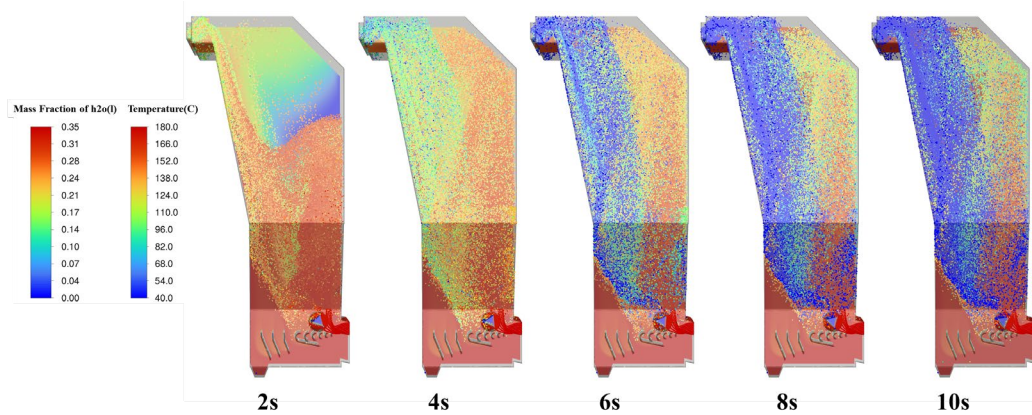


Figure 16. Comparative particle temperature profiles in the XY plane

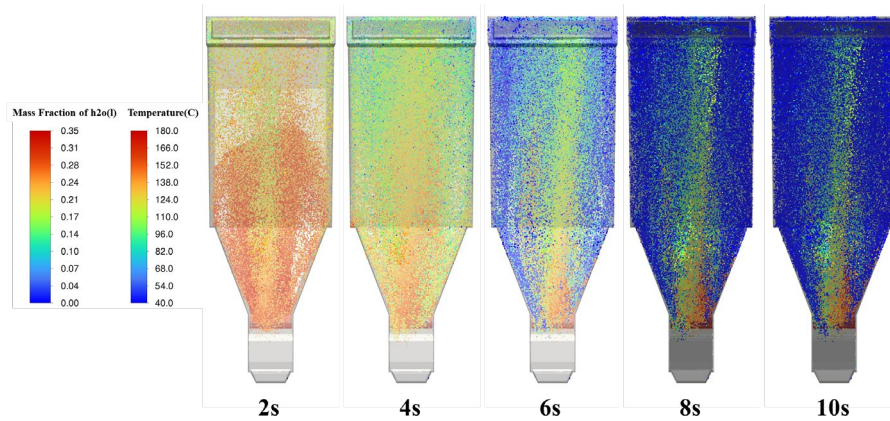
482 Driven by the optimized thermal environment, the drying kinetics follow the gas-solid
483 convective heat and mass transfer mechanism. Figures 17 and 18 illustrate the spatiotemporal
484 evolution of particle moisture content on the YZ and XY planes from 2s to 10 s. The color
485 gradient quantitatively represents the progress of the mass transfer process, marking the
486 transition from the initial high moisture content (red, mass fraction ~ 0.35) to the target range
487 (yellow, ~ 0.13). At the initial stage ($t=2s$), particles entering the chamber exhibit high moisture
488 characteristics. As they are transported upward under the guidance of the shunt guide vanes,
489 intense heat and mass exchange occurs. By the 4s to 6s interval, particles achieve uniform
490 dispersion across the XY and YZ planes with significantly attenuated moisture content,
491 indicating that the drying process is approaching stability.



492

493

Figure17 Spatiotemporal moisture evolution in the YZ plane for the split-flow structure (2–10 s)



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Figure 18. Spatiotemporal moisture evolution in the XY plane for the split-flow structure (2–10 s)

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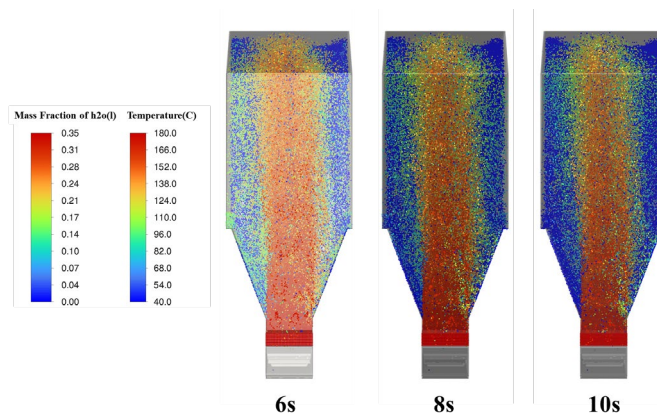
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Figure 19 further reveals the microscopic characteristics of particle moisture distribution in the negative YZ direction during the steady-state drying stage (6s to 10s), elucidating the separation of drying states governed by fluid dynamics. In the central mainstream region, the particle distribution exhibits a uniform yellow characteristic. This indicates that the vast majority of the material has successfully reached the target moisture content of approximately 0.13, verifying the effectiveness of the shunt-type structure in ensuring the consistency of drying quality for the bulk material.

However, a distinct phenomenon is observed in the near-wall region, indicated by a persistent blue layer. This region represents particles with extremely low moisture content, signaling the

505 occurrence of over-drying. The physical mechanism underlying this phenomenon is primarily
506 dominated by the boundary layer effect: due to fluid viscosity, a significant velocity gradient
507 forms near the wall, causing particles entrapped in this region or adhering to the surface to
508 experience velocity stagnation. Compared to particles in the mainstream, their significantly
509 prolonged residence time leads to excessive moisture loss. Notably, in contrast to the more
510 extensive stagnation zones in the original structure, the optimized shunt-type design effectively
511 confines this over-dried region to a very narrow near-wall layer, thereby ensuring that the bulk
512 tobacco material is maintained within the optimal drying range.



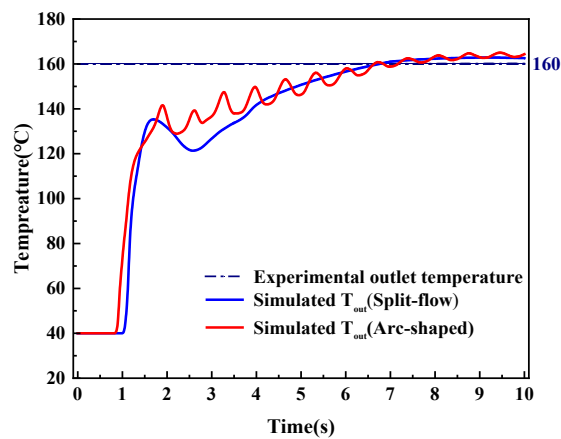
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514 Figure 19. Particle moisture distribution in the YZ negative direction during the stable drying phase (6s–10s)

515 3.1.5 Experimental Validation of Heat and Mass Transfer Model

516 Figure 20 compares the transient outlet temperature evolution of both structures against the
517 experimental benchmark (160°C). The close agreement between the simulated trends and
518 experimental data validates the accuracy of the CFD-DEM model. Distinct dynamic behaviors
519 are observed between the two designs. The arc-shaped structure (red line) exhibits pronounced
520 thermal oscillation with large amplitudes, indicating significant flow instability. In contrast, the
521 split-flow structure (blue line) demonstrates superior thermal stability. Although a minor
522 temperature dip occurs during the initial phase, this is attributed to the intensified gas-solid heat

523 exchange, where rapid heat absorption by cold particles causes a temporary thermal lag.
524 Subsequently, the profile converges rapidly with dampened fluctuations, confirming that the
525 optimized design effectively mitigates unsteady disturbances.



526

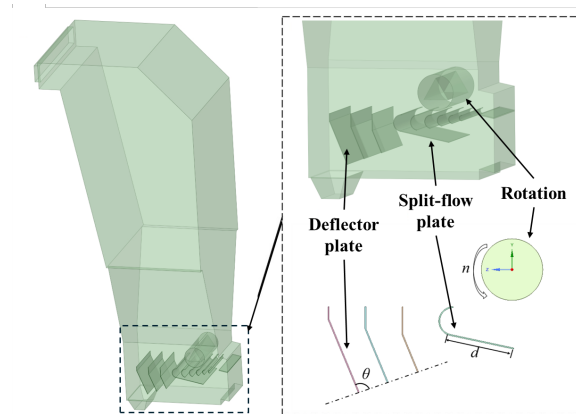
527 Figure 20. Comparison of simulated outlet temperatures against experimental data

528 3.2 Multi-Objective Optimization of deflector Structure Parameters

529 3.2.1 Response Surface Experimental Design

530 As shown in Figure 21, the simulation results for the airflow dryer with a split-flow deflector
531 structure indicate that three structural parameters, including the rotation speed of the distribution
532 roller (n), the inclination angle of the left deflector plate (θ), and the length of the split-flow
533 plate (d) have significant influence on both airflow uniformity and intensity.

534 Based on a comprehensive analysis of the simulation results, the value ranges and specific
535 settings for these parameters are determined. Detailed information is provided in Table 4.



536

537

Figure 21. Airflow dryer with split-flow deflector structure

538

Table 4. Structural parameters of the deflector components

Parameter	Rotation speed n (r/min)	Deflector plate angle θ ($^{\circ}$)	Split-flow plate length d (mm)
Values	60、150、180、210、230、 277、325	80、90、100	350、400、450、500

539

The experimental design is a three-factor, multi-level scheme based on the response surface methodology (RSM), using the D-optimal design approach. The D-optimal method selects the most informative experimental points algorithmically, minimizing redundancy and reducing the number of simulations. Compared to random sampling or orthogonal design, it is better suited for nonlinear modeling problems.

544

The plane located 4.9 meters downstream from the distribution roller exhibits minimal velocity fluctuation and is therefore selected as the monitoring surface for evaluating airflow uniformity within the dryer. The simulated dataset generated using the D-optimal design is presented in Table 5.

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Table 5. Simulated dataset based on D-optimal experimental design

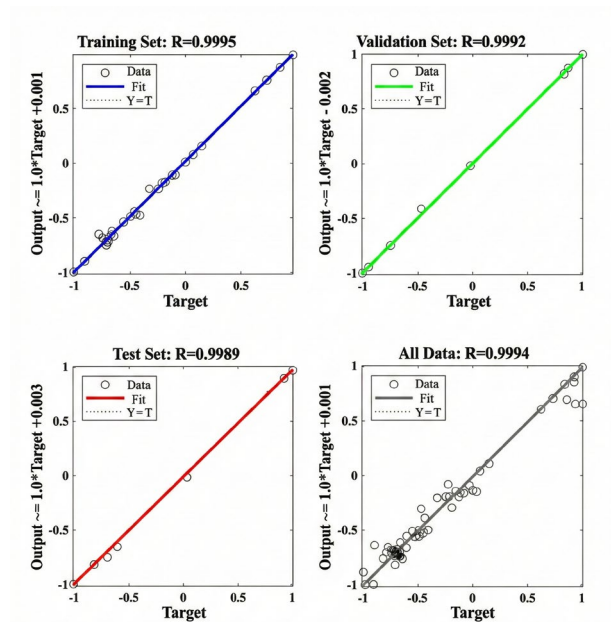
No.	Speed n (r/min)	Angle θ ($^\circ$)	Length d (mm)	Average velocity v (m/s)	Uniformity index
1	150	90	400	4.39	0.743
2	180	90	400	4.31	0.733
3	210	90	400	4.43	0.734
4	230	90	400	4.46	0.739
5	277	90	400	3.37	0.666
6	325	90	400	2.83	0.621
7	230	80	400	2.69	0.636
8	277	80	400	2.67	0.635
9	325	80	400	2.67	0.637
10	230	100	400	4.33	0.680
11	277	100	400	3.36	0.627
12	325	100	400	2.99	0.638
13	230	90	450	2.93	0.652
14	277	90	450	2.92	0.65
15	325	90	450	3.02	0.627
16	230	80	450	2.93	0.670
17	277	80	450	2.98	0.667
18	325	80	450	2.90	0.662
19	230	100	450	4.22	0.691
20	277	100	450	3.27	0.671
21	325	100	450	2.93	0.64
22	230	90	500	2.94	0.684
23	277	90	500	2.93	0.677
24	325	90	500	2.90	0.675
25	230	80	500	4.07	0.717
26	277	80	500	2.75	0.648
27	325	80	500	2.72	0.653
28	230	100	500	3.45	0.682
29	277	100	500	3.16	0.645
30	325	100	500	3.2	0.652
31	180	90	450	2.86	0.655
32	150	80	450	2.97	0.669
33	150	100	450	4.12	0.686
34	180	80	400	2.64	0.639
35	180	100	400	2.65	0.639

36	180	90	350	3.98	0.702
37	150	90	350	3.98	0.701
38	150	80	350	4.56	0.686
39	150	100	350	4.65	0.685
40	230	80	350	4.60	0.688
41	230	100	350	4.78	0.696
42	210	90	350	4.10	0.710
43	277	90	350	3.95	0.704

552 3.2.2 Validation of the Accuracy of the Neural Network Model

553 Firstly, the BP neural network is trained using the simulation data from Table 5. The network is
 554 designed with a three-layer architecture, including 3 input neurons, 4 neurons in the hidden layer,
 555 and 2 output neurons.

556 As shown in Figure 22, the coefficient of determination R^2 for the training set reaches 0.9990,
 557 while the R^2 for the testing set is 0.9978. The R^2 values for both datasets are very close (with a
 558 maximum difference of only 0.0012), indicating a uniform data distribution without significant
 559 outliers, which demonstrates successful model training and high prediction reliability.



560

561

Figure 22. Linear regression plot of the neural network

562 Figures 23 and 24 compare the predicted and actual values of the two optimization indicators:
 563 uniformity index and average velocity. The prediction error for the uniformity index remains
 564 within 5%, while for the average velocity, the error is within 10%, verifying the accuracy of the
 565 model.

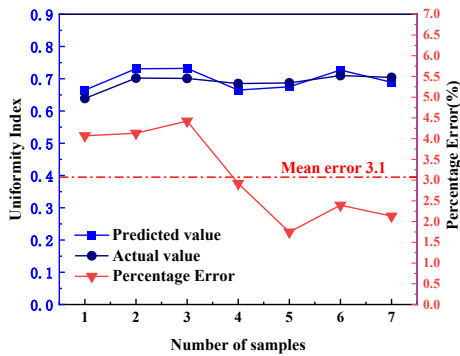


Figure 23. Predicted value vs. actual values of uniformity index by the neural network

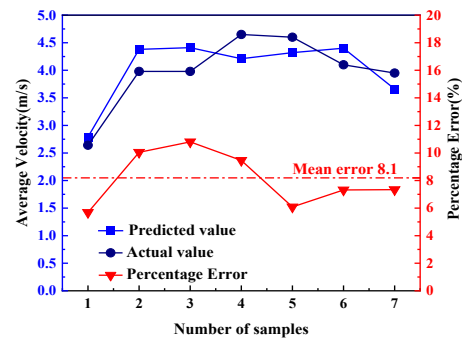


Figure 24. Predicted value vs. actual values of average velocity by the neural network

566 3.2.3 Optimization Results and Analysis of NSGA-II

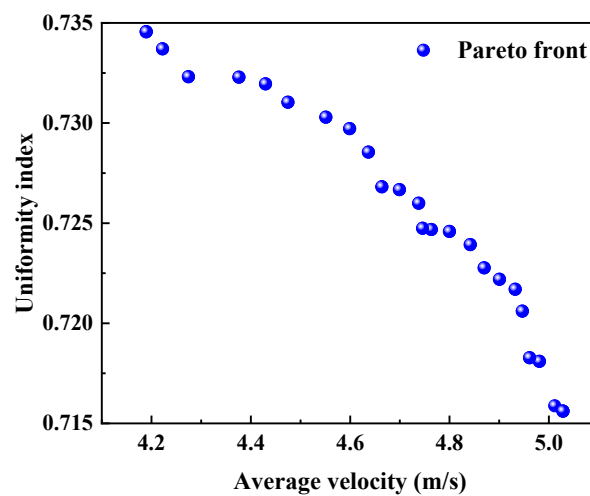
567 The selected input factors are rotation speed (n), angle (θ), and length (d). The selected output
 568 parameters include the surface uniformity index and average velocity, as shown in Table 6.

569 Table 6. Range of influencing factors

Variable	Influencing factor	Lower limit	Upper limit
x_1	Speed n	150	325
x_2	Angle θ	300	390
x_3	Length d	30	60

570 The elite preservation coefficient is set to 0.4, with a population length of 50 and a maximum of
 571 200 generations. The fitness function deviation threshold is defined as $1e-10$. Based on these
 572 settings, multiple optimized solutions are obtained through computation, as shown in Figure 25.

573 The Pareto front is a widely used tool in multi-objective optimization problems, particularly
574 effective for evaluating trade-offs between conflicting objectives. It represents a set of non-
575 dominated solutions, in which no individual objective can be improved without degrading
576 another under the given constraints. The final selection of an optimal solution depends on
577 specific requirements, constraints, and practical application scenarios. Representative Pareto-
578 optimal solutions are illustrated in Figure 25.



579

580

Figure 25. Pareto front of the multi-objective optimization results.

581 Several optimal reference solutions are selected from the optimization results, as listed in Table
582 7. The results indicate that adjusting the distribution roller speed, the inclination angle of the
583 left-side deflector plate, and the length of the split-flow plate can significantly improve both the
584 airflow uniformity and the average velocity inside the airflow dryer. These improvements
585 demonstrate that appropriate modifications to the three structural parameters lead to a more
586 uniform internal flow field and enhanced flow capacity, thereby improving both the quality and
587 efficiency of material drying.

588 Under identical hot air and material inlet conditions, compared with the original configuration
589 (parameters: $n=230$ r/min, $\theta=80^\circ$, $d=400$ mm), the airflow uniformity index predicted values of

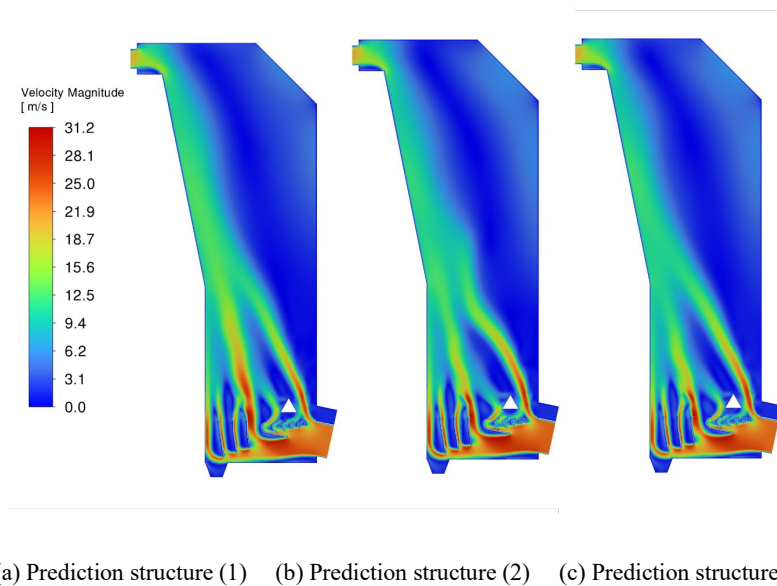
590 the three optimized structures improve by 12.7%, 12.6%, and 12.3%, respectively, and increases
 591 in average airflow velocity by 41.3%, 41.7%, and 42.6%.

592 Table 7. Selected optimal reference points from the optimization results

Reference structure	Speed n (r/min)	Angle θ ($^{\circ}$)	Length d (mm)	Average velocity v (m/s)	Uniformity index
Predicted structure (1)	180	92	380	4.59	0.729
Predicted structure (2)	190	92	380	4.62	0.728
Predicted structure (3)	190	92	370	4.69	0.726

593 **3.3 Validation of Predicted Results**

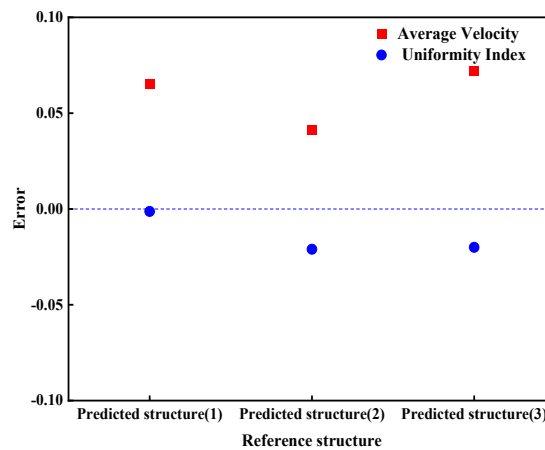
594 Figure 26 presents the airflow velocity contours for three predicted deflector structures. The
 595 results indicate that the constructed split-flow deflector configurations effectively guide hot
 596 airflow, resulting in a more uniform velocity distribution within the drying chamber. This leads
 597 to a more consistent drying environment for the dispersed material.



598 Figure 26. Velocity contour plots of airflow for the three predicted deflector plate structures

599 Figure 27 further analyzes the error between simulation predictions and experimental

600 measurements for the three configurations. The structure optimized using the BP-GA algorithm
 601 shows high predictive accuracy, with an average velocity error of 7% and a uniformity index
 602 error of only 2%. Compared to the original arc-shaped deflector plate structure, the three
 603 predicted structures show respective improvements in average airflow velocity of 0.9%, 4.0%,
 604 and 2.3%, and increases in uniformity index of 9.9%, 11.8%, and 11.5%. When compared with
 605 the pre-optimized split-flow structure ($n=230$ r/min, $\theta=80^\circ$, $d=400$ mm), the improvements in
 606 average velocity are 36.7%, 39.2%, and 38.2%, while the uniformity index increases by 12.6%,
 607 14.5%, and 14.2%, respectively. Among them, prediction structure (2) demonstrates the best
 608 performance across both key indicators.



609

610 Figure 27. Comparison of prediction and actual values for the three predicted structures

611 Figure 28 compares the particle spatial distribution and motion trajectories between the pre-
 612 optimized split-flow deflector structure (parameters: $n=230$ r/min, $\theta=90^\circ$, $d=400$ mm) and
 613 prediction structure (2). Although the split-flow structure already alleviates particle
 614 sedimentation and limited spatial coverage issues compared to the arc-shaped design, some
 615 localized aggregation and path deviation due to rotation-induced disturbances remain. In
 616 contrast, prediction structure (2) significantly expands the particle dispersion range within the
 617 chamber. The particle trajectories are more spatially divergent and uniform, the disturbance

618 effect from the rotation component is noticeably reduced, and problems such as stagnation and
619 accumulation in the lower region are effectively mitigated.

620 Figure 29 provides a cross-sectional comparison of particle distribution in the XY plane. The
621 optimized structure notably enhances particle coverage and distribution uniformity across the
622 section, with improved coordination between particle movement and airflow.

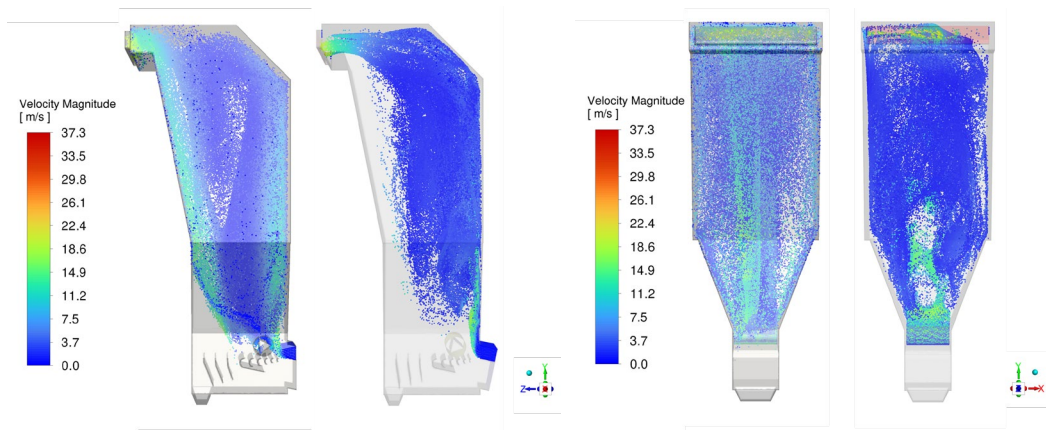


Figure 28. Comparison of particle distribution in the YZ direction between the original and predicted structure

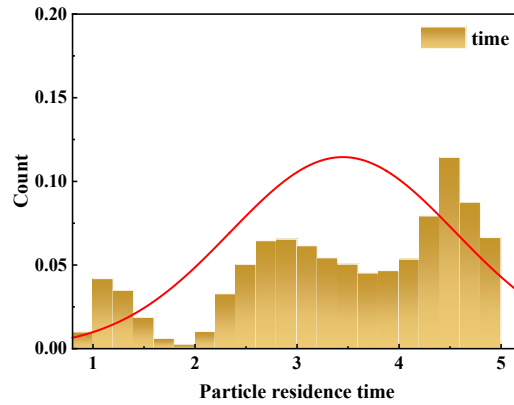
Figure 29. Comparison of particle distribution in the XY direction between the original and predicted structure

(2)

predicted structure (2)

623 Figure 30 shows the residence time frequency distribution of particles under prediction structure
624 (2). Compared with the pre-optimized design (as shown in Figure 13), prediction structure (2)
625 exhibits a slightly broader residence time range, primarily concentrated between 2–4.5s.
626 However, the frequency curve is smoother with smaller fluctuations. In contrast, the pre-
627 optimized structure presents a sharp frequency peak between 1–2.5s with more irregular
628 fluctuations, indicating greater dispersion in particle trajectories. The results from prediction
629 structure (2) suggest that internal flow disturbances are significantly reduced, particle paths are
630 more coherent, and the average residence time is extended. This contributes to a more uniform
631 spatial distribution and improved drying time efficiency, reducing the risk of localized under-

632 drying or over-drying and highlighting its superiority in particle drying quality control.

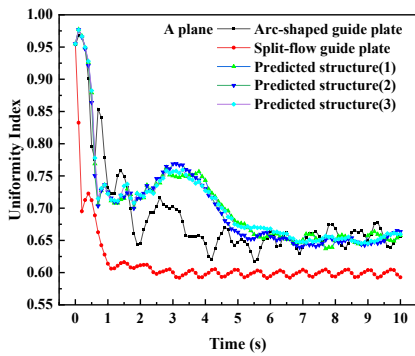


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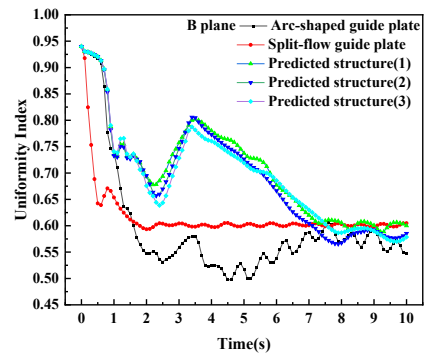
634 Figure 30. Residence time frequency distribution of particles inside the airflow dryer with the predicted
635 structure (2)

636 Figure 31 illustrates the temporal variation of the airflow uniformity index across five cross-
637 sections (A: 1 m from the roller center; B: 2 m; C: 3.5 m; D: 4.9 m; E: outlet plane) in the XZ
638 plane of the airflow-based tobacco dryer. Analysis indicates that in region A, which is closest to
639 the roller, all three optimized Deflector plate structures outperform the unoptimized split-flow
640 design. These optimized structures are more effective in directing hot air and mitigating
641 disturbances caused by the roller's rotation, thereby ensuring a more uniform drying effect for
642 newly entering tobacco particles.

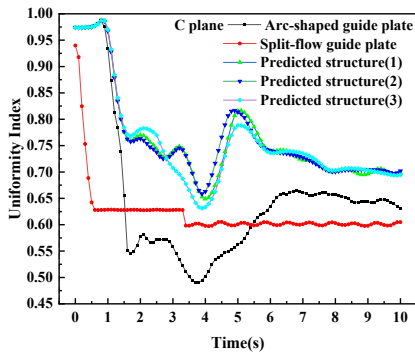
643 As the cross-sectional plane moves from A to D, the uniformity index exhibits a more stable
644 variation trend. The optimized split-flow Deflector structures demonstrate significantly better
645 performance in terms of hot air distribution uniformity compared to both the unoptimized split-
646 flow and the original arc-shaped designs. At the outlet plane E, although the uniformity indices
647 of different structures eventually converge with minor differences, the optimized structures
648 maintain superior overall stability throughout the drying process. This enhanced stability
649 provides critical assurance for the consistency and quality of tobacco drying.



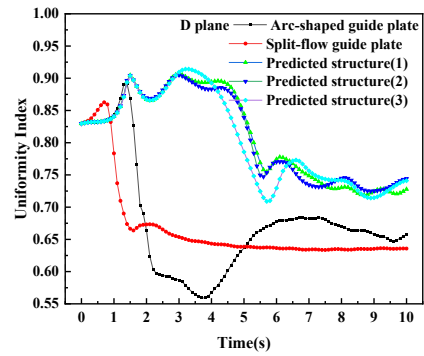
(a) Variation of uniformity index for five structures on plane A



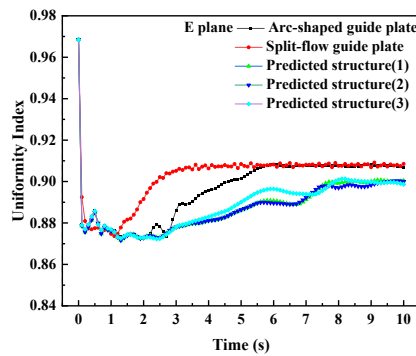
(b) Variation of uniformity index for five structures on plane B



(c) Variation of uniformity index for five structures on plane C



(d) Variation of uniformity index for five structures on plane D



(e) Variation of uniformity index for five structures on plane E

651 **4. Concluding Remarks**

652 This study proposed and evaluated a novel split-flow deflector plate configuration for airflow
653 dryers. By integrating flow field analysis with multi-objective optimization, the following key
654 conclusions were drawn:

655 (1) Hydrodynamic performance enhancement: Comparative analysis revealed that the
656 inadequate flow guidance in the conventional arc-shaped deflector plate leads to pronounced
657 velocity non-uniformities. In contrast, the optimized split-flow deflector plate enables more
658 efficient utilization of turbulent energy. Compared with the original arc-shaped deflector plate,
659 the optimized design improved the average airflow velocity by 4.0% and increased the
660 uniformity index by 11.8%. This improvement translates into more consistent particle
661 trajectories and reduced agglomeration.

662 (2) Thermodynamic stability and drying quality: The optimized structure demonstrates superior
663 performance in coupled heat and mass transfer. Unlike the pronounced thermal oscillations
664 observed in the arc-shaped deflector plate, the split-flow deflector plate exhibits excellent
665 thermal stability, with the outlet temperature rapidly converging to the experimental benchmark
666 (160°C). The initial thermal lag confirms the intensified gas-solid heat exchange facilitated by
667 the optimized design. Furthermore, spatiotemporal analysis indicates that this structure
668 effectively mitigates the over-drying phenomenon induced by the boundary layer effect. By
669 confining the low-velocity stagnation zone to a narrow near-wall layer, the design prevents
670 excessive moisture loss and ensures uniform drying quality for the bulk material.

671 (3) Optimization strategy and parameters: The coupling of BP-NSGA-II with flow field analysis
672 proved to be an effective strategy for identifying parameter combinations that balance turbulence
673 intensity with flow uniformity. The resulting prediction model achieved high accuracy (error <
674 5% for the uniformity index). The optimal performance was achieved with a rotation speed n of

675 190 r/min, Deflector plate angle θ of 92° , and Split-flow plate length d of 380 mm.

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