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13 **Facile one pot preparation of magnetic chitosan-palygorskite nanocomposite for**  
14 **efficient removal of lead from water**

15

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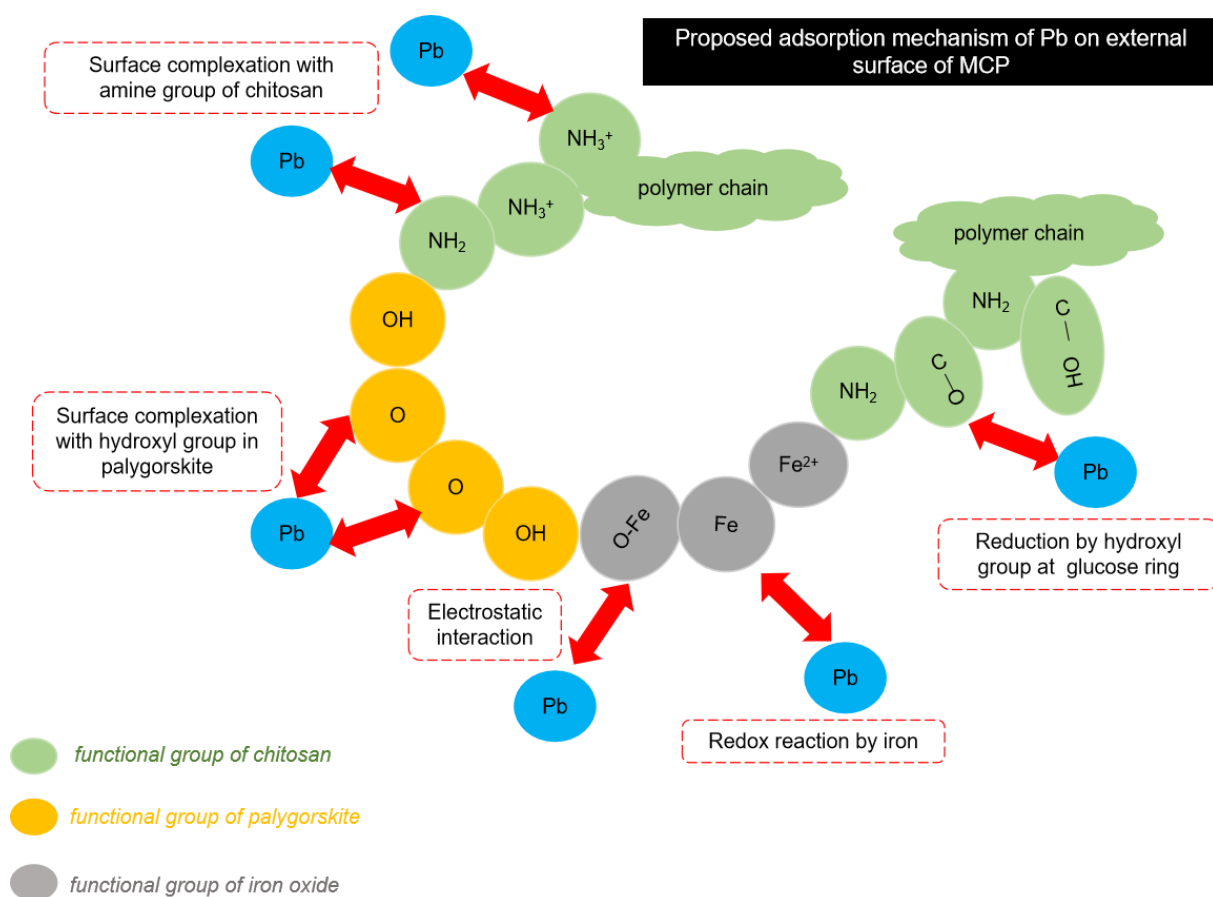
34

35 **Highlights**

- 36 • Magnetic chitosan-palygorskite (MCP) was fabricated in simple and green method.
- 37 • MCP removed 58.5 mg g<sup>-1</sup> of lead from water.
- 38 • Complexation and chemical reduction of lead on MCP surface was evidenced.
- 39 • MCP recorded 82% lead removal even following four regeneration cycles.
- 40 • MCP retained superparamagnetic nature after regeneration.

41

42 **Graphical abstract**



43

44

45 **Abstract**

46 Development of polymeric magnetic adsorbents is a promising approach to obtain efficient  
47 treatment of contaminated water. However, the synthesis of magnetic composites involving  
48 multiple components frequently involves tedious preparation steps. In the present study, a  
49 magnetic chitosan-palygorskite (MCP) nanocomposite was prepared through a straight-  
50 forward one pot synthesis approach to evaluate its lead ( $\text{Pb}^{2+}$ ) removal capacity from aqueous  
51 solution. The nano-architectural and physicochemical properties of the newly-developed MCP  
52 composite were described via micro- and nano-morphological analyses, and crystallinity,  
53 surface porosity and magnetic susceptibility measurements. The MCP nanocomposite was  
54 capable to remove up to  $58.5 \text{ mg Pb}^{2+} \text{ g}^{-1}$  of MCP from water with a good agreement of  
55 experimental data to the Langmuir isotherm model ( $R^2 = 0.98$ ). The  $\text{Pb}^{2+}$  adsorption process  
56 on MCP was a multistep diffusion-controlled phenomenon evidenced by the well-fitting of  
57 kinetic adsorption data to the intra-particle diffusion model ( $R^2 = 0.96$ ). Thermodynamic  
58 analysis suggested that the adsorption process at low  $\text{Pb}^{2+}$  concentration was controlled by  
59 chemisorption, whereas that at high  $\text{Pb}^{2+}$  concentration was dominated by physical adsorption.  
60 X-ray photoelectron and Fourier transform infrared spectroscopy results suggested that the Pb  
61 adsorption on MCP was governed by surface complexation and chemical reduction  
62 mechanisms. During regeneration, the MCP retained 82%  $\text{Pb}^{2+}$  adsorption capacity following  
63 four adsorption-desorption cycles with ease to recover the adsorbent using its strong magnetic  
64 property. These findings highlight the enhanced structural properties of the easily-prepared  
65 nanocomposite which holds outstanding potential to be used as an inexpensive and green  
66 adsorbent for remediating  $\text{Pb}^{2+}$  contaminated water.

67

68 **Keywords:** Adsorbent regeneration; Chitosan; Lead removal; Magnetic nanocomposite;  
69 Palygorskite; Wastewater treatment.

## 70        **1. Introduction**

71    The widespread occurrence of toxic heavy metal contaminants in water resources requires  
72    sustainable mitigation strategies to ensure the global water security. Lead (Pb) is one of the  
73    major heavy metals that enters into water streams from sources and activities such as battery  
74    industries, ceramic industries, e-wastes, mining, printing, pipes, and many others including  
75    household activities [1]. Human exposure of Pb through consumption of Pb-contaminated  
76    drinking water and food may severely affect the lung, kidney, brain and nervous system [2].  
77    Hence, the United States Environmental Protection Agency (USEPA) fixed the critical  
78    concentration of Pb as  $0.015 \text{ mg L}^{-1}$  in drinking water as a measure to control the fatality and  
79    long-term Pb exposure to humans caused by water contamination [3].

80    Natural adsorbents are regarded as a promising and environmentally benign group of  
81    materials for tackling the high cost of resources in treating contaminated water. Naturally  
82    available clay minerals such as kaolinite, bentonite, montmorillonite and palygorskite are  
83    widely used for the removal of a wide range of contaminants (e.g., heavy metals, dyes,  
84    pesticides) from aqueous systems due to the low cost, wide natural abundance, and desirable  
85    physico-chemical, thermal and mechanical properties of the mineral materials. The clay  
86    minerals have large specific surface area (SSA), high cation exchange capacity (CEC), high  
87    thermal stability and numerous surface functional groups useful for interacting with  
88    environmental contaminants [4], [5]. Palygorskite, in particular, has been used for heavy  
89    metal removal from aqueous solutions and found to be a good inorganic filler material in  
90    polymer-clay composite preparation [4], [6], [7], [8]. However, pristine palygorskite suffers  
91    from poor adsorption capacity, high desorption rate, and lack of standardized protocol to use  
92    [9], [10]. This necessitates the development of novel clay mineral-based functional materials  
93    for enhancing the contaminant adsorption and retention capacity while also upholding  
94    environmental sustainability in resource utilization.

95 In this direction, polymer-clay nanocomposites have emerged as one of the promising hybrid  
96 materials for developing environmentally friendly adsorbents for wastewater treatment [11].  
97 The incorporation of biopolymers such as chitosan (derived from shrimp and other crustacean  
98 organisms) and alginate in polymer-clay nanocomposites is of great environmental interest  
99 due to their wide natural abundance and non-toxic nature towards living organisms [12].  
100 Within the composite's structure, clay minerals can provide a support to the biopolymers  
101 which often suffer from low mechanical strength and high solubility in acidic solution.  
102 Removal of a wide range of organic and inorganic contaminants from wastewater using  
103 chitosan-clay composites were reported, including the novel magnetic feature of the  
104 composites [13], [14], [15], [16], [17]. For the recovery of spent adsorbent from water,  
105 magnetic polymer-clay composites have the advantage of easy magnetic separation via an  
106 external magnetic field as opposed to conventional centrifugation and filtration approaches.  
107 However, the preparation of magnetic clay nanocomposites involves notably tedious  
108 procedures such as pre-synthesis of the magnetic (e.g., iron oxide) nanoparticles, pre-  
109 treatment of the clay minerals, and dissolution of the polymer in a suitable solvent followed  
110 by cross-linking or precipitation for obtaining the final product [18], [19]. The above multi-  
111 step procedure can incur unfavourable operational expenditure, prolong the preparation time  
112 of the composite, and cause environmental threat due to excessive use of solvents and  
113 auxiliary chemicals. Thus, a straight-forward preparation procedure of magnetic clay  
114 nanocomposites is of great interest. To advocate the effectiveness of such green preparation  
115 approach, understanding the structural integration of the multidimensional components (i.e.,  
116 2D/3D clay minerals, polymeric molecules, and nanosized magnetic particles) within the  
117 magnetic polymer-clay nanocomposites is immensely important. In parallel, a systematic  
118 assessment of performance of the easily-prepared nanocomposites for removing contaminants  
119 from water would ascertain the materials' potential as a new-class of effective adsorbents.

120 In this study, a facile one-pot *in-situ* preparation of magnetic chitosan-palygorskite (MCP)  
121 nanocomposite was achieved by employing a straight-forward, green, and practical synthesis  
122 method. The synthesised MCP was characterised through state-of-the-art techniques, such as  
123 X-ray diffraction (XRD), Fourier transform infra-red (FTIR) spectroscopy, scanning and  
124 transmission electron microscopy (SEM and TEM), thermogravimetric analysis (TGA), X-  
125 ray photoelectron spectroscopy (XPS), and surface area, porous structure and magnetism  
126 analyses, to gain in-depth understanding of the molecular interactions of each assembled  
127 component (i.e., polymer, clay mineral and iron oxide). Furthermore, the MCP was evaluated  
128 for its potential application in Pb<sup>2+</sup> removal from aqueous solutions. The adsorption isotherm  
129 profiling, kinetic and thermodynamic studies were performed to postulate the removal  
130 mechanisms. Finally, the regeneration feasibility of the nanocomposite was assessed and  
131 compared with other similar magnetic nanocomposites.

132

## 133 **2. Materials and methods**

### 134 2.1 Materials and reagents

135 Chitosan (average molecular weight (MW) 400,000 g mol<sup>-1</sup>; maximum degree of  
136 deacetylation 85%) was purchased from Sigma-Aldrich, Australia. Palygorskite (particle size  
137 < 90 µm) originating in Western Australia was purchased from Hudson Resource Pty. Ltd.,  
138 Australia, and used as received (without purification). Lead (II) nitrate (Pb(NO<sub>3</sub>)<sub>2</sub>, MW =  
139 331.208 g mol<sup>-1</sup>) and ammonium hydroxide (NH<sub>4</sub>OH, ≥ 25% v/v purity) were procured from  
140 Fisher Scientific (United Kingdom), iron (III) chloride hexahydrate (FeCl<sub>3</sub>.6H<sub>2</sub>O, MW =  
141 270.30 g mol<sup>-1</sup>, 99% assay) from Chem-Supply (Australia), iron (II) chloride tetrahydrate  
142 (FeCl<sub>2</sub>.4H<sub>2</sub>O, MW = 198.81 g mol<sup>-1</sup>, 99% assay) from Sigma-Aldrich (Germany), calcium  
143 nitrate tetrahydrate (Ca(NO<sub>3</sub>)<sub>2</sub>.4H<sub>2</sub>O, MW = 236.15 g mol<sup>-1</sup>, 99% assay) and sodium nitrate  
144 (NaNO<sub>3</sub>, MW = 84.99 g mol<sup>-1</sup>, 99% assay) from Bio-Lab (Australia), and

145 ethylenediaminetetraacetic acid disodium salt (EDTA-Na<sub>2</sub>, MW = 198.81 g mol<sup>-1</sup>, 99% assay)  
146 from Sigma-Aldrich (USA). All the reagents were of analytical or laboratory grade.

147

## 148 2.2 Preparation of magnetic chitosan-palygorskite nanocomposite

149 Palygorskite (0.5 g) was first dispersed in 50 mL of Milli-Q water (resistivity ≥ 18 MΩ.cm)

150 overnight through continuous stirring on a magnetic stirrer (200 rpm). Chitosan solution (0.5

151 g L<sup>-1</sup>) in 2% (v/v) acetic acid was prepared under constant stirring (500 rpm) for 2 h at 40°C.

152 The chitosan solution was left to cool at 25°C until all the air bubbles disappeared. On the

153 other hand, FeCl<sub>3</sub>·6H<sub>2</sub>O (1.086 g) was dissolved in 10 mL Milli-Q water followed by the

154 addition of FeCl<sub>2</sub>·4H<sub>2</sub>O (0.416 g). The Fe<sup>3+</sup>-Fe<sup>2+</sup> (2:1 molar ratio of Fe<sup>3+</sup>: Fe<sup>2+</sup>) solution was

155 then immediately transferred to the chitosan solution, and the mixture was stirred rapidly

156 under an N<sub>2</sub> atmosphere at 60°C. The palygorskite suspension was added to the chitosan-

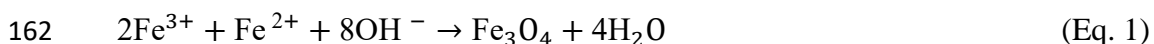
157 Fe<sup>3+</sup>-Fe<sup>2+</sup> solution and allowed to react for 90 min at 55 to 60°C upon continuous stirring.

158 Then, 5 mL of NH<sub>4</sub>OH (25% (v/v)) was added drop wise to the above mixture upon vigorous

159 stirring for 30 min. The NH<sub>4</sub>OH was added in excess (20:1 molar ratio of OH<sup>-</sup>: Fe<sup>2+</sup>/

160 Fe<sup>3+</sup> according to stoichiometric conversion to ensure a complete co-precipitation of Fe<sup>3+</sup>-Fe<sup>2+</sup>

161 mixture and solidification of the modified chitosan suspension (Eq. 1):



163 The black precipitate of the magnetic chitosan-palygorskite nanocomposite (MCP) was then

164 vacuum-filtered, and washed thoroughly with Milli-Q water and absolute ethanol in turns

165 before drying in a hot-air oven at 40°C overnight. The nanocomposite was grounded in an

166 agate mortar and pestled to pass through a sieve with 90-μm mesh size. For comparison

167 purpose, a pristine iron oxide was prepared using the similar procedure described above

168 without the addition of chitosan and palygorskite.

169



170 2.3 Material characterization

171 X-ray Diffraction (XRD) patterns of powdered samples were collected on a Malvern  
172 PANalytical Empyrean diffractometer using  $\text{CuK}\alpha$  ( $\lambda=1.54 \text{ \AA}$ ) radiation operating at 40 mA  
173 and 40 kV in the  $2\theta$  range of 4 to  $90^\circ$  with a step size of  $0.013 \text{ s}^{-1}$  using  $0.25^\circ$  and  $0.50^\circ$  fixed  
174 divergence and anti-scatter slits, respectively. Fourier Transform Infra-Red (FTIR) spectra  
175 were collected using a Nicolet 6700 series spectrometer (Thermo Scientific) in the range of  
176  $4000\text{--}400 \text{ cm}^{-1}$  wave number by co-addition of 16 scans with a resolution of  $8 \text{ cm}^{-1}$ . The  
177 sample pellets were prepared with dehydrated KBr at a 1:200 (w/w) sample:KBr ratio. The  
178 BET (Brunauer–Emmett–Teller) specific surface area (SSA) and BJH (Barrett-Joyner-  
179 Halenda) pore size distribution were determined through  $\text{N}_2$  adsorption-desorption isotherms  
180 at liquid nitrogen temperature ( $-196^\circ\text{C}$ ) on a Micromeritics Gemini 2380 Surface Area  
181 Analyser. The samples were degassed overnight at  $60^\circ\text{C}$  under vacuum at 2 Torr prior to SSA  
182 analysis. Zeta potential was measured (loading of 0.01% m/v) in duplicate on a zeta potential  
183 analyser (Nicomp<sup>TM</sup> 380 ZLS, USA). The magnetic measurement was conducted using a  
184 Vibrating Sample Magnetometer (VSM) (MicroMag<sup>TM</sup> Model 3900 Series). The  
185 measurement was conducted in triplicate at  $27^\circ\text{C}$  with approximately 10 to 45 mg powdered  
186 sample at 1 Tesla and averaging time of 100 to 200 ms. Thermo gravimetric analysis (TGA)  
187 was performed using a Mettler Toledo Thermogravimetric Analyser (TGA/DSC 1 model)  
188 equipped with STAR<sup>e</sup> system with a heating rate of  $10^\circ\text{C min}^{-1}$  from 25 to  $950^\circ\text{C}$  under  $\text{N}_2$   
189 environment (flow rate of  $50 \text{ mL min}^{-1}$ ).

190 The surface morphology of the nanocomposite was examined by using a FEI Quanta 450  
191 FEG Environmental Scanning Electron Microscope (SEM) equipped with an Apollo X SDD  
192 Energy Dispersive X-ray (EDX) detector. A drop of dilute sample suspension (in ethanol)  
193 was placed on a silicon wafer that was adhered to double-sided carbon tape and mounted on  
194 an aluminium stub. The air-dried samples were coated with pulsed carbon (30 nm thickness)

195 by a QUORUM Q150T E Carbon Coater. The SEM investigation was conducted in high  
196 vacuum (HV) mode using an Everhart-Thornley detector. Meanwhile, the Transmission  
197 Electron Microscope (TEM) image was recorded using a JEOL JEM-2100F-HR transmission  
198 electron microscope equipped with a field emission gun operated at 200 kV. The Scanning  
199 Transmission Electron Microscope (STEM) image of dispersed MCP (in diluted ethanol) was  
200 collected by the same instrument using the annular bright field (BF) and dark field (DF)  
201 detectors. X-ray Photoelectron Spectroscopy (XPS) analysis was performed on a Kratos  
202 AXIS Ultra DLD spectrometer with a monochromatic Al X-ray source at 225 W having a  
203 characteristic energy of 1486.6 eV. The analysis was conducted under vacuum ( $4 \times 10^{-9}$  Torr)  
204 with applied charge neutraliser during the scan. The wide survey scan was performed from 0  
205 with pass energy of 160 eV while for the high-resolution analysis, the pass energy was  
206 lowered to 20 eV. Analysis of the binding energy was calibrated with the C<sub>1s</sub> peak of the  
207 aliphatic carbons present at 284.4 eV.

208

#### 209 2.4 Adsorption and adsorbent regeneration experiments

210 The Pb<sup>2+</sup> stock solution was prepared by dissolving Pb(NO<sub>3</sub>)<sub>2</sub> in Milli-Q water and diluted to  
211 various working concentrations. Batch adsorption experiments were conducted by allowing  
212 the MCP to react with aqueous solutions of Pb<sup>2+</sup> (initial Pb<sup>2+</sup> concentration ranging from 50  
213 to 500 mg L<sup>-1</sup>, adsorbent loading 5 g L<sup>-1</sup>, initial pH 4, at 25°C) in capped polyethylene tubes  
214 under reciprocating shaking at 150 agitations per min. The Pb-loaded MCP was recovered  
215 magnetically, and the supernatant was filtered through a 0.45 µm membrane filter. The initial  
216 and equilibrium concentrations of Pb<sup>2+</sup> were determined using an Inductively Coupled  
217 Plasma Optical Emission Spectrometer (ICP-OES) (Perkin Elmer, Optima 5300V). All  
218 experiments were conducted in duplicate, and the mean values are reported. The adsorption  
219 of Pb<sup>2+</sup> on the wall of polyethylene tubes was negligible.

220 The amount of  $\text{Pb}^{2+}$  adsorbed onto the adsorbent was calculated using Eq. 2:

$$221 \quad q_e = \frac{(C_i - C_e) V}{m} \quad (\text{Eq. 2})$$

222 where,  $q_e$  is the amount of metal adsorbed at equilibrium ( $\text{mg g}^{-1}$ ),  $C_i$  and  $C_e$  are the initial  
223 and equilibrium  $\text{Pb}^{2+}$  concentrations ( $\text{mg L}^{-1}$ ), respectively,  $V$  is the volume (L) of the  
224 solution, and  $m$  is the mass (g) of the adsorbent.

225 The effect of pH on adsorption was investigated by adjusting the pH (3 to 7) of  $50 \text{ mg L}^{-1}$   
226  $\text{Pb}^{2+}$  solution using  $0.01 \text{ M}$  of  $\text{HNO}_3$  or  $\text{NaOH}$ . The influence of contact time was studied  
227 from 10 min to 24 h. The thermodynamic study (temperature effect) was pursued by  
228 conducting adsorption experiments at 25, 40 and  $55^\circ\text{C}$  with  $5 \text{ g L}^{-1}$  adsorbent loading at pH 4.  
229 The adsorption data were fitted to the Langmuir, Freundlich, Dubinin-Radushkevich (D-R)  
230 and Temkin isothermal models (Supplementary Data (SD1)) to understand the adsorption  
231 behaviour of  $\text{Pb}^{2+}$  on MCP. The kinetic adsorption behaviour was evaluated using the pseudo  
232 first order, pseudo second order, intra-particle diffusion and Elovich models in order to  
233 understand the mechanisms of  $\text{Pb}^{2+}$  adsorption (SD2). The standard Gibbs free energy change  
234 of adsorption ( $\Delta G^\circ$ ) was determined by the classic van't Hoff equation (SD3) to evaluate the  
235 effect of temperature on the adsorption process.

236 In the adsorbent regeneration study, the Pb-loaded MCP (initial  $\text{Pb}^{2+}$  concentration  $100 \text{ mg}$   
237  $\text{L}^{-1}$ ) was agitated in a  $0.01 \text{ M}$  EDTA- $\text{Na}_2$  aqueous solution (adsorbent loading  $5 \text{ g L}^{-1}$ ) for 30  
238 min upon reciprocal shaking (150 agitations per min) for four adsorption-desorption cycles.

239 The quantity of desorbed  $\text{Pb}^{2+}$  was determined by ICP-OES using Eq. 3:

$$240 \quad \text{Desorption \%} = \frac{\text{Amount of Pb desorbed}}{\text{Amount of Pb adsorbed}} \times 100 \quad (\text{Eq. 3})$$

241

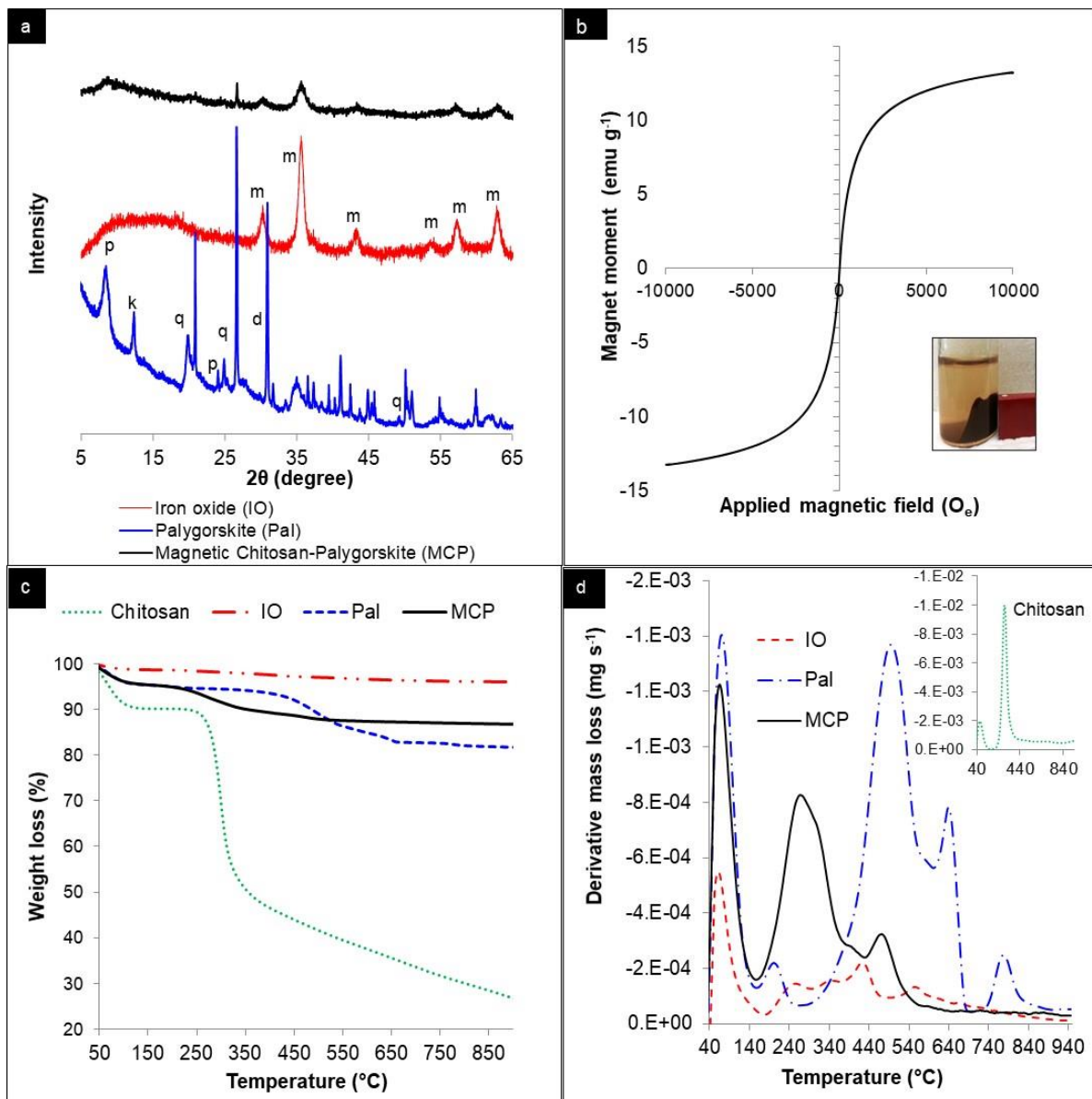
### 242 3. Results and discussion

#### 243 3.1 Structural and morphological characterization of magnetic chitosan-palygorskite 244 nanocomposite

245 The characteristic diffraction reflections of palygorskite were observed at  $2\theta = 8.5^\circ$  (10.39  
246 Å),  $19.6^\circ$  (4.52 Å) and  $24.9^\circ$  (3.57 Å) accompanied by reflections of kaolinite at  $2\theta = 12.3^\circ$   
247 (7.19 Å), and quartz at  $2\theta = 20.8^\circ$  (4.27 Å) and  $26.4^\circ$  (3.37 Å) (Fig. 1 a) [20]. A sharp  
248 reflection at  $2\theta = 30.8^\circ$  was assigned to dolomite (calcium magnesium carbonate) which was  
249 an impurity in the pristine palygorskite. Meanwhile, the iron oxide showed characteristics  
250 reflections at  $2\theta$  positions of  $30.1^\circ$ ,  $35.5^\circ$ ,  $43.1^\circ$ ,  $53.4^\circ$ ,  $57.0^\circ$ , and  $62.6^\circ$ , which corresponded  
251 to (220), (311), (400), (422), (511) and (440) diffraction planes of magnetite ( $\text{Fe}_3\text{O}_4$ )  
252 respectively (International Centre for Diffraction Data (ICDD<sup>®</sup>) File No. 04-008-8146) [21].  
253 Chitosan is amorphous in nature. The diffraction pattern of the MCP coincided with the  
254 patterns of the magnetite and palygorskite (Fig. 1 a) except for a broad reflection at  $2\theta = 10.39$   
255 Å due to incorporation of the amorphous chitosan component in the nanocomposite, as  
256 similarly observed in other chitosan-palygorskite nanocomposites [4], [22]. The dolomite  
257 reflection ( $2\theta = 30.8^\circ$ ) was absent in MCP (Fig. 1 a), which indicated that the acidic  $\text{Fe}^{2+}/\text{Fe}^{3+}$   
258 suspension (pH=2.1) at initial stage of the synthesis removed the carbonate impurity such as  
259 dolomite from the clay mineral.

260 When a permanent magnet (AlNiCo bar magnet) was placed close to the wall of a vial  
261 containing an aqueous suspension of MCP, the particles were attracted to the wall  
262 immediately, and the liquid became transparent within 60 to 180 sec (Fig. 1 b(inset)). The  
263 MCP showed a magnetic susceptibility ( $M_s$ ;  $\text{emu g}^{-1}$ ) value of  $14.3 \text{ emu g}^{-1}$  with coercivity

264 ( $H_c$ ) of  $0.7 \text{ O}_e (\text{k Am}^{-1})$ . The plot of  $M_s$  against the applied magnetic field (1 Tesla) (



265

266 Fig. 1 Fig. 1 b showed a “S” shaped curve with almost no measurable hysteresis loop, which  
 267 indicated a near-superparamagnetic characteristic of the MCP [23].

268 In thermogravimetric analysis (TGA), the MCP showed a total weight loss of 13.4% as the  
 269 temperature was elevated to  $950^{\circ}\text{C}$ . The loss was smaller than the pristine palygorskite  
 270 (18.5%) and chitosan (75.0%), indicating a higher thermal stability of the nanocomposite

271 (Fig. 1 c). The differential thermogravimetric (DTGA) profile of MCP showed three

272 endothermic weight loss steps (Fig. 1 d; step 1 (4.1% loss with a peak at  $68^{\circ}\text{C}$ ), step 2 (6.4%

273 loss with a peak at 200 °C), and step 3 (1.6% loss with a peak at 473 °C). Step 1 was assigned  
274 to the loss of physisorbed water and some zeolitic water (specifically from palygorskite). The  
275 step 2 was responsible for the elimination of the remaining zeolitic water and dehydration of  
276 structural water (in palygorskite) combined with a degradation of chitosan macromolecules  
277 [24]. A maximum degradation of chitosan was recorded at 390°C, as indicated by the  
278 stagnant weight loss (inset in Fig. 1 d). The peak at 635°C (dolomite or calcite decarbonation)  
279 and 760°C (dehydroxylation of structural Mg-OH groups observed in palygorskite were  
280 undetected in MCP [25], [26], [27]. These findings supported the XRD results that carbonates  
281 were removed from the clay mineral during the synthesis of MCP.

282 MCP had a specific surface area (SSA) of 18.3 m<sup>2</sup> g<sup>-1</sup>, which was lower than the pristine  
283 palygorskite (49.4 m<sup>2</sup> g<sup>-1</sup>) (Table 1) due to the macro/nonporous characteristics of chitosan.  
284 The MCP exhibited a type IV N<sub>2</sub> adsorption isotherm, which is associated with mesopores (2  
285 < d < 50 nm) with the presence of H3 hysteresis loop at P/P<sub>0</sub> between 0.4 to 0.9 (SD; Fig. S1  
286 a & b). The zeta potential analysis shows that the palygorskite had a negative surface charge  
287 throughout the pH range with no isoelectric point (IEP) displayed, whereas the MCP had an  
288 apparent IEP of 4.8 (Fig. S1c). The comparatively positive surface charge of MCP at below  
289 pH 5 could be partly contributed by the protonated magnetite nanoparticles (IEP = 5.6) and  
290 by chitosan adhered to the surface of MCP (Fig. S1c).

291 The SEM image revealed that the chitosan layer was mostly present on the outer surface of  
292 the MCP nanocomposite, and the palygorskite anchoring the iron oxide nanoparticles  
293 constituted the “core” of the nanocomposite (Fig. 2 a). The EDX spectra confirmed the  
294 presence of chitosan (ascribed by the N atoms, which represents the amide/amine groups of  
295 chitosan), palygorskite (represented by Al and Mg atoms) and magnetite (represented by Fe  
296 atoms) (Fig. 2 b). Both bright and dark field STEM images in Figure 2 showed the  
297 accumulation of palygorskite and magnetite within the chitosan polymer matrix, and some

298 palygorskite particles were seen projected outside the nanocomposite. It was previously  
299 reported that iron oxide (e.g., magnetite) could be encapsulated within the chitosan matrix  
300 following their co-precipitation in the presence of a strong base [19], [28]. Similarly,  
301 nucleation of  $\text{Fe}^{2+}/\text{Fe}^{3+}$  onto the negative surface of palygorskite during the synthesis was  
302 expected. Thus, in the system where both chitosan and palygorskite existed, the  $\text{Fe}^{2+}/\text{Fe}^{3+}$   
303 ions could disperse, nucleate and then grow by forming the crystalline iron oxide  
304 nanoparticles on either chitosan, palygorskite, or even at the chitosan-palygorskite interface.  
305 The spherical magnetite nanoparticles (particle size in the range of 6 to 40 nm) were  
306 distributed regionally in the order of chitosan-palygorskite > palygorskite > chitosan (Fig. 2 c  
307 & d). These observations could be associated with the negatively charged surface of  
308 palygorskite that provided a greater interaction and stability with iron cations. Thus,  
309 palygorskite played a significant role of a structural support for the deposition of magnetite  
310 nanoparticles within the nanocomposite. Based on the observation on the surface  
311 morphologies of MCP (Fig. 2), the schematic reaction mechanism was proposed, as in Fig. 3  
312 a.

313

### 314 3.2 Advantages of one-pot synthesis of magnetic chitosan-palygorskite

315 The flow diagram of MCP synthesis (Fig. 3 b) showed that the developed one-pot synthesis  
316 approach had five main advantages: (i) no pretreatment step (activation) for palygorskite was  
317 needed, (ii) co-precipitation of iron oxide (magnetite) could be achieved in-situ, (iii) all  
318 components (chitosan, palygorskite and iron oxide) could be simultaneously interacted  
319 (electrostatically) in one medium, (iv) precipitation (solidification) of MCP products could be  
320 achieved using a common base (i.e.,  $\text{NH}_4\text{OH}$ ), and (v) the solidified MCP could be separated  
321 from the reaction medium using an external magnetic field or simple filtration (Fig. 3 b). The  
322 methods applied in this study improves the previous approach in the synthesis of similar

323 nanocomposites by eliminating the use of potentially hazardous or expensive substances (e.g.,  
324 organic solvents, surfactants or crosslinkers) and minimized the waste [18], [29]. The  
325 synthesis was straight-forward, fast and accomplished under mild experimental conditions (at  
326 a temperature range of 25 – 60 °C and atmospheric pressure, no harsh solvent used). The  
327 applied method was thus much greener, and could potentially solve the issue of high-cost  
328 associated with conventional nanocomposite synthesis methods [19], [28].

329

### 330 3.3 Adsorption studies

#### 331 3.3.1 Effect of pH and adsorption isotherm

332 In aqueous systems, Pb ions could exist as mono ( $\text{Pb}^{2+}$ ) or polynuclear species (e.g.,  
333  $\text{Pb}_2(\text{OH})^{3+}$ ,  $\text{Pb}_3(\text{OH})^{4+}$ ) due to the solvation, hydrolysis and polymerisation effect [30]. The  
334 hydrolysed  $\text{Pb}^{2+}$  usually occurs at a higher pH and is prone to precipitation. Hence, the  $\text{Pb}^{2+}$   
335 adsorption was conducted at a pH range of 3 to 7 to avoid Pb precipitation. The MCP  
336 demonstrated a high percentage of  $\text{Pb}^{2+}$  removal (> 85%; at initial Pb concentration of 50 mg  
337  $\text{L}^{-1}$ ) at all the selected pH values (Fig. S2). Although MCP had IEP of 4.8, the consistent  $\text{Pb}^{2+}$   
338 removal performance over the entire pH range indicated that the adsorbent's affinity towards  
339  $\text{Pb}^{2+}$  could not be explained solely based on electrostatic interaction. The pH 4 was used as  
340 the working pH in remaining adsorption experiments in this study as this pH recorded the  
341 highest  $\text{Pb}^{2+}$  removal (>99%) (Fig. S2).

342 The maximum amount of  $\text{Pb}^{2+}$  adsorption onto MCP obtained in this study was 58.5 mg  $\text{g}^{-1}$   
343 (Table 2). The adsorption isotherm data were well fitted to the Langmuir model ( $R^2 = 0.98$  at  
344  $p < 0.05$ ) (Table 2), suggesting a monolayer adsorption on homogeneous adsorbent surface  
345 (MCP). The high adsorption capacity was most likely due to the synergic interplay of various  
346 functional groups (e.g.,  $-\text{NH}_2$ ,  $\text{Si-O}^-$ ,  $\text{FeO}^-$ ,  $\text{OH}$ ) contained in the MCP that enhanced the  
347 nanocomposite's affinity towards  $\text{Pb}^{2+}$ . Meanwhile, the  $E$  value calculated from the D-R



348 model was  $12.9 \text{ kJ mol}^{-1}$  (Table 2), which indicated that the adsorption was a chemisorption  
349 mechanism ( $E$  value between 8 to  $16 \text{ kJ mol}^{-1}$ ) [31].

350

### 351 3.3.2 Adsorption kinetics

352 The adsorption kinetic data were best fitted to the intra-particle diffusion model ( $R^2 = 0.96$ , at  
353  $p < 0.05$ ) among all the kinetic models tested (Table 3; Fig. 4 a). This could be attributed to  
354 the chitosan coating on the outer layer of MCP that significantly influenced the diffusion of  
355 the adsorbate ( $\text{Pb}^{2+}$ ) [32]. Hence, the adsorption of  $\text{Pb}^{2+}$  on the active sites of MCP external  
356 surfaces was likely followed by a diffusion process into the pores of the nanocomposite.  
357 Since the intra-particle diffusion plot did not cross the origin of diffusion (Fig. 4. Fig. 4 a),  
358 film diffusion might have played a key role as the rate-determining step for  $\text{Pb}^{2+}$  adsorption  
359 on MCP [33].

360 The intra-particle diffusion plot could be divided into three linear stages (Fig. 4 a). Stage 1  
361 was assigned for the film diffusion experienced during the fast transportation of the adsorbate  
362 ( $\text{Pb}^{2+}$ ) from bulk solution towards the external surface of MCP [34]. The gradual increase in  
363 adsorption (stage 2) and attainment of equilibrium (stage 3) were likely due to the pore (or  
364 particle) diffusion processes. By applying the intra- particle diffusion equation at each stage,  
365 the slope and intercept might represent the  $k_i$  (diffusion rate) and film thickness, respectively  
366 (Fig. 4 a). The greater the slope, the faster is the adsorption process [35]. The  $k_i$  parameter at  
367 each stage showed that the film diffusion (stage 1) was a slower process than the pore (or  
368 particle) diffusion (stage 2 and 3) (Fig. 4 a). Accordingly, the intercept values were reduced  
369 dramatically (from 7.09 at stage 1 to 0.929 at stage 3) which indicated a decrease in the  
370 boundary layer thickness (Fig. 4 a) [35]. The thickness value is usually correlated with the  
371 degree of mass transfer resistance; the thicker the boundary, the higher the resistance. Hence,  
372 the initial diffusion stage (stage 1) experienced the highest mass transfer resistance effect

373 (Fig. 4 a), most likely due to the chitosan coating deposited on the external surface [36]. This  
374 observation suggested that  $Pb^{2+}$  solute first interacted with active sites of chitosan ( $NH_2$  and  
375  $OH$ ) on the external surface of MCP. When the external surface was almost occupied, the  
376 solute travelled through the chitosan polymeric network to reach into internal pores of  
377 palygorskite and magnetite. As mentioned above, the diffusion rate at stage 2 ( $0.9214 \text{ mg g}^{-1}$   
378  $\text{min}^{0.5}$ ) and stage 3 ( $1.2071 \text{ mg g}^{-1} \text{ min}^{0.5}$ ) were faster than those rate in stage 1 ( $0.9122 \text{ mg g}^{-1}$   
379  $\text{min}^{0.5}$ ) (Fig. 4 a) because the diffusion of  $Pb^{2+}$  to mesoporous palygorskite and magnetite was  
380 easier than in the tortuous chitosan polymeric network. Furthermore, the rate was faster likely  
381 due to the tendency of achieving the equilibrium causing a rapid uptake [4], [37].  
382 To support the diffusion hypothesis, the Boyd model was applied to determine the actual rate  
383 determining step, either film (boundary-layer) diffusion or particle diffusion (SD2) [38]. The  
384 Boyd model analysis showed that the linear plot did not cross the origin (Fig. 4 b), which  
385 confirmed that the external mass transfer by film diffusion was the rate controlling  
386 mechanism in the  $Pb^{2+}$  adsorption system. Similar results were also reported in previous  
387 studies related to polymeric composite in which the kinetic data were well-described by the  
388 intra-particle diffusion model [34], [36], [39].

389

### 390 3.3.3 Thermodynamic study

391 The negative  $\Delta G^\circ$  values (Table S1) confirmed that the adsorption was spontaneous in nature  
392 and energetically favourable [40]. At a similar temperature (e.g.,  $25^\circ\text{C}$ ), the  $\Delta G^\circ$  became less  
393 negative at higher initial  $Pb^{2+}$  concentration. These findings suggested that the adsorption  
394 process at low solute ( $Pb^{2+}$ ) concentration was more favourable than at high solute  
395 concentration. The concentration gradient created greater driving force to reduce the mass  
396 transfer resistance for more collision with the active adsorption sites of MCP. Consequently,  
397 some steric effect could possibly present due to aggressive binding competition among  $Pb^{2+}$

398 crowd towards the active sites. The hindered access towards active sites thus reduced the  
399 spontaneity of the reaction. On the other hand, at a similar concentration (e.g., 100 mg L<sup>-1</sup>)  
400 the  $\Delta G^\circ$  became more negative at high temperature (Table S1), which indicated that the  
401 adsorption was more spontaneous with temperature increase. The  $\Delta G^\circ$  value also signified  
402 the type of mechanisms (electrostatic interaction (physisorption), ion-exchange, or charge  
403 sharing and/or transfer related to chemisorption) [41]. Physisorption usually shows a small  
404  $\Delta G^\circ$  value (between -20.0 to 0 kJ mol<sup>-1</sup>), while chemisorption involves  $\Delta G^\circ$  in the range of  
405 -80 and -400 kJ mol<sup>-1</sup> [42]. Based on this classification, the adsorption at 50 mg L<sup>-1</sup> ( $\Delta G^\circ < -$   
406 100 kJ mol<sup>-1</sup>) most likely occurred through chemisorption, while some physisorption also  
407 took place at a high Pb<sup>2+</sup> concentration (Table S1).

408 The positive  $\Delta H^\circ$  values for all systems indicated that the adsorption was endothermic in  
409 nature (Table S1) [43]. The adsorption at 50 and 100 mg L<sup>-1</sup> Pb<sup>2+</sup> displayed  $\Delta H^\circ$  values larger  
410 than 40 kJ mol<sup>-1</sup> (absolute), thus the adsorption mechanism was controlled mainly by  
411 chemisorption [43]. Meanwhile, physisorption ( $\Delta H^\circ < 40$  kJ mol<sup>-1</sup>) likely occurred at high  
412 Pb<sup>2+</sup> concentration (200 mg L<sup>-1</sup>) (Table S1), which signified the occurrence of multilayer  
413 adsorption. The positive standard entropy change ( $\Delta S^\circ$ ) (Table S1) signified the increasing  
414 randomness at the solid-liquid interface, which might be explained through the concept of  
415 desorption of pre-adsorbed water surrounding the MCP interface in an aqueous suspension,  
416 as proposed by Barshad [44]. As the Pb<sup>2+</sup> ions were adsorbed on the active sites, the pre-  
417 adsorbed water was displaced to accommodate Pb<sup>2+</sup>. Thus, the desorbed water molecules  
418 from the pre-adsorbed state to a free state increased the randomness in the system [44]. From  
419 another perspective, the adsorption of Pb<sup>2+</sup> on the active sites of MCP made them to be  
420 immobilised and static. Hence, the ions on the active sites were more ordered than those in  
421 the diffused layer. Thus, the decreased randomness at higher Pb<sup>2+</sup> concentration was  
422 associated with the saturation of active sites by the immobilised Pb<sup>2+</sup> ions. A similar idea was

423 proposed in explaining the endothermic nature of  $\text{Co}^{2+}$  and anionic dye adsorption on  
424 kaolinite and coffee waste-derived adsorbent [9], [45].

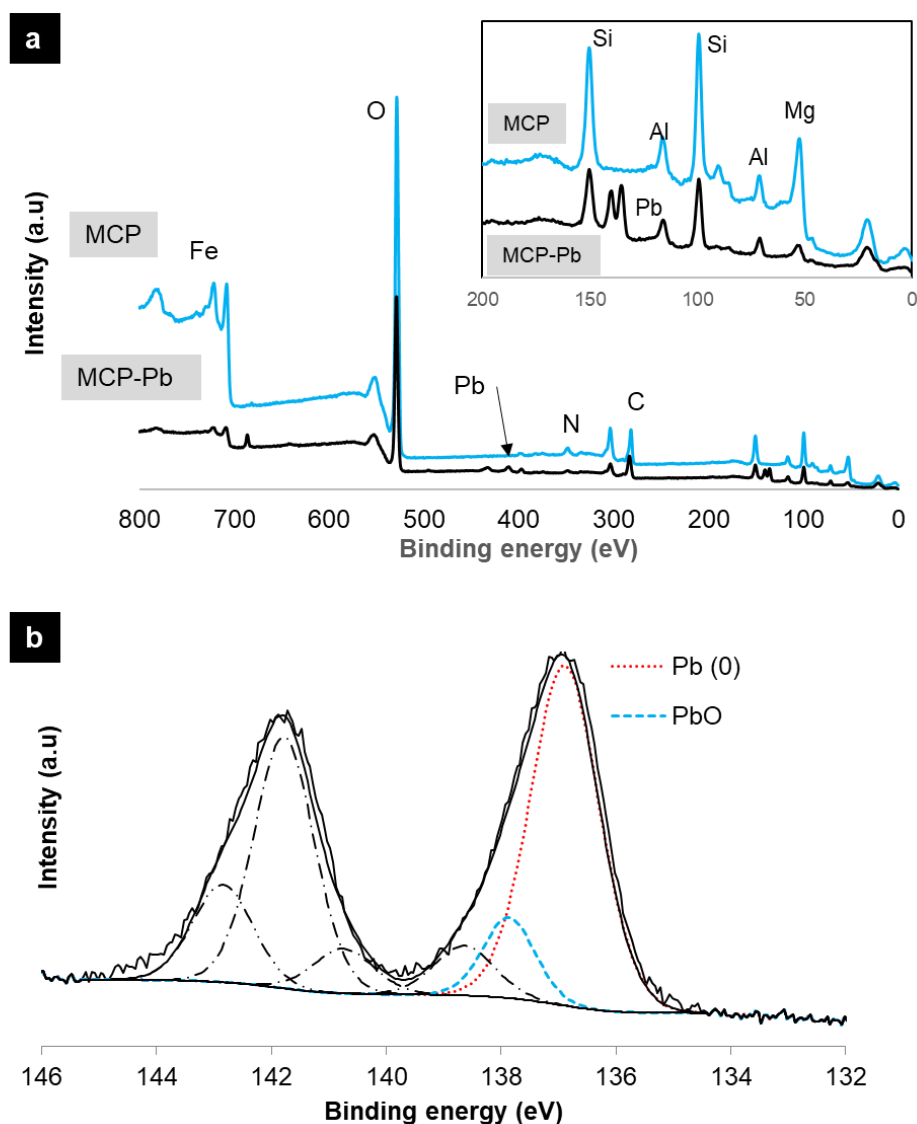
425

#### 426 *3.3.4 Adsorption mechanisms revealed through spectroscopic investigations*

427 In the FTIR spectrum of MCP, the -OH stretching band located at  $3712\text{ cm}^{-1}$  and  $3530\text{ cm}^{-1}$   
428 were the characteristic bands of palygorskite (Fig. 5) [46]. Accordingly, the Al-Al-OH  
429 bending, Si-O-Si asymmetric stretching and Si-O-Si bending accounted from the palygorskite  
430 were observed at  $910$ ,  $1030$  and  $471\text{ cm}^{-1}$ , respectively. Meanwhile, the bands at  $563\text{ cm}^{-1}$  and  
431  $428\text{ cm}^{-1}$  corresponded to the stretching mode of Fe-O in magnetite ( $\text{Fe}_3\text{O}_4$ ) [47], [48], [49].  
432 Chitosan showed a broad band (due to hydrogen bonding) at around  $3450\text{ cm}^{-1}$  and a sharp  
433 band at  $1650\text{ cm}^{-1}$  (Fig. 5). The above band positions were overlapping with the N-H  
434 stretching vibration of chitosan (normally occurs at  $3417\text{ cm}^{-1}$ ), while the N-H bending mode  
435 was observed at  $3621\text{ cm}^{-1}$ . The C-H stretching vibrations of the chitosan glucosamine ring  
436 were present at  $2919$  and  $2860\text{ cm}^{-1}$  [50].

437 In the  $\text{Pb}^{2+}$  loaded-MCP (denoted as MCP-Pb) IR spectrum, three regions experienced  
438 significant changes (Fig. 5). The first region at around  $3700$  to  $3500\text{ cm}^{-1}$  corresponded to the  
439 O-H stretching bands in the clay mineral shifted to a lower wavenumber, which implied an  
440 increase of bond length due to changes of electronegativity of neighbouring atoms, for  
441 example, via the formation of hydrogen bonds. In the IR spectrum of MCP-Pb, the broad  
442 band between  $3500$  to  $3000\text{ cm}^{-1}$  was sharpened likely due to the interaction with  $\text{Pb}^{2+}$ ,  
443 indicating a disruption of the internal hydrogen bonds existing within the -OH and N-H  
444 groups of chitosan. At the second region ( $1600$  to  $1300\text{ cm}^{-1}$ ) a more distinguished strong  
445 band at  $1381\text{ cm}^{-1}$  appeared in MCP-Pb, which was assigned to the bending of long chain  
446 aliphatic carbon ( $-\text{CH}_2$ ) of chitosan, C-N stretching band or the -C-OH stretching [51], [52].  
447 A strong band in this region signalled a large change in dipole moment (more polar).

448 Meanwhile, the band at  $563\text{ cm}^{-1}$  in the third region corresponding to the Fe-O stretching  
 449 vibration of magnetite shifted to a lower wavenumber ( $539\text{ cm}^{-1}$ ) and became weaker, which  
 450 suggested a possible  $\text{Pb}^{2+}$  interaction with the oxygen atoms of magnetite nanoparticles [53].  
 451 The XPS survey spectrum of MCP showed the presence of Al, Si, Mg (corresponding to  
 452 palygorskite), N and C (from chitosan), Fe (from magnetite) and O (associated with all these  
 453 components) (Fig. 6 a). The presence of Pb in Pb-loaded MCP (MCP-Pb) spectrum was  
 454 confirmed at the binding energy around 137 ( $\text{Pb}_{4f7/2}$ ) and 142 eV ( $\text{Pb}_{4f5/2}$ ) (Fig. 6 a) [54], [55].  
 455 The photoelectron peaks at 137.7 and 136.8 eV (



456  
 457 Fig. 6.6 b) corresponded to  $\text{PbO}$  and zero valent  $\text{Pb}$  ( $\text{Pb}^0$ ), respectively [56]. The presence of  
 458 both the  $\text{Pb}$  species indicated the adsorption and simultaneous reduction mechanisms for  $\text{Pb}^{2+}$

459 removal by the MCP, which is reported for the first time in this study compared to previous  
460 studies involving similar group of adsorbents.

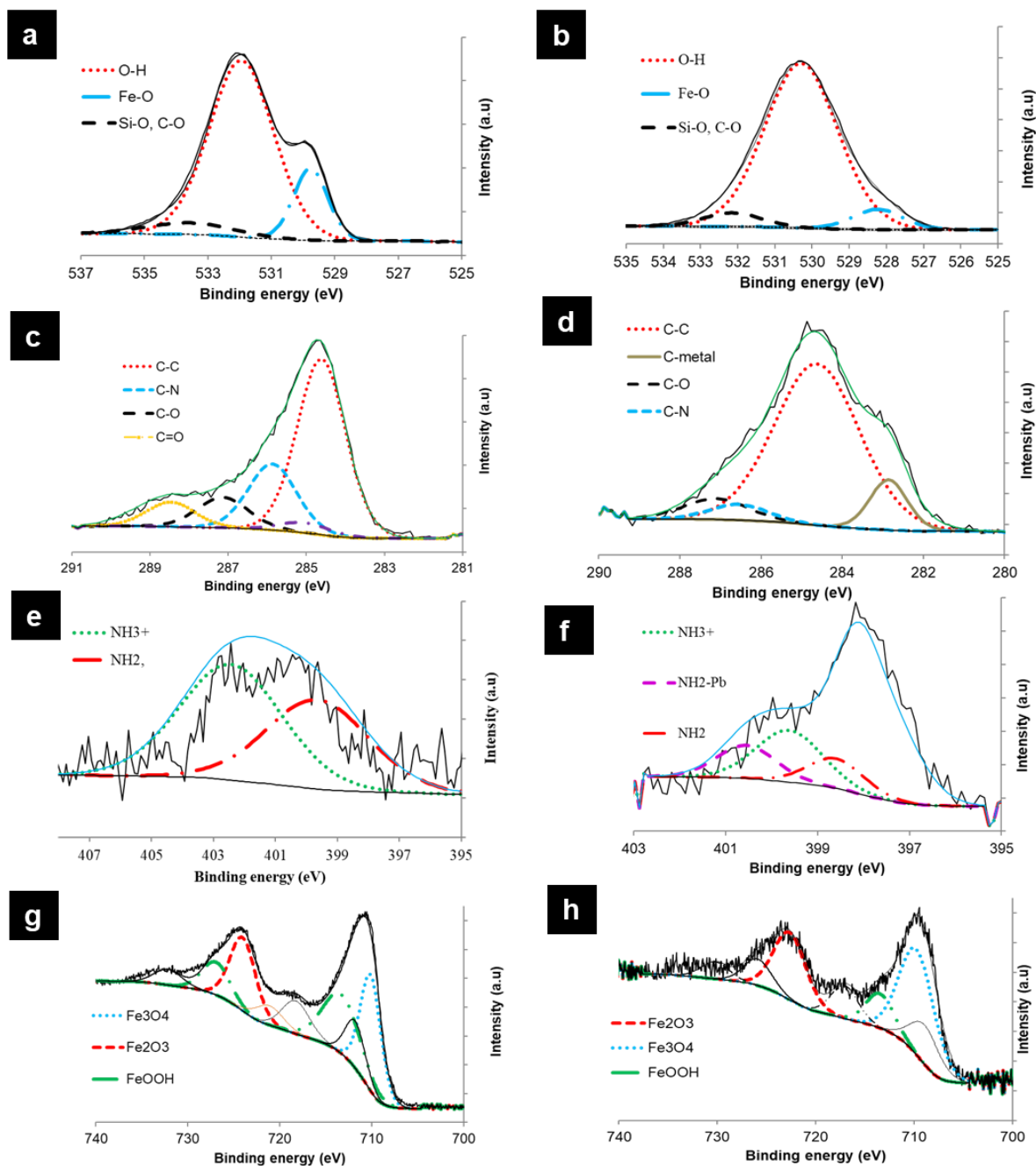
461 The O<sub>1s</sub> photoelectron peak at 531.9 eV (Fig. 7 a) corresponded to the hydroxyl groups  
462 (-OH) contributed by chitosan, clay mineral, iron oxide, and chemically or physically  
463 adsorbed water [57], [58], [59], [60]. The binding energy at 529.8 eV represented the oxygen  
464 bonded to Fe (Fe-O species), while the peak at 533.6 was designated to either Si-O or C-O  
465 (Fig. 7 a) [61]. In MCP-Pb, a slight shift for the peak at 531.9 (-OH) to 530.3 eV occurred,  
466 which suggested the changes of OH chemical environment in the nanocomposite due to Pb  
467 adsorption (Fig. 7 b). The shifting of O<sub>1s</sub> peak towards a lower binding energy region was  
468 also observed in previous heavy metal removal studies involving chitosan and iron oxide  
469 [59], [60], [61], [62]. In addition, a 55.9% reduction in peak area of Fe-O at 529.8 eV was  
470 observed (Fig. 7 b). These findings signified the involvement of OH groups and Fe-O species  
471 in the Pb<sup>2+</sup> removal mechanism, confirming chemisorption. Similarly, Fan et al. showed a  
472 shifting of O<sub>1s</sub> peak to higher binding energy in Pb-loaded palygorskite (thermally treated)  
473 [63]. However, the chemical environment of palygorskite assembled in the chitosan-iron  
474 oxide matrix (in MCP) in this study was greatly different from the palygorskite only system  
475 reported by Fan et al. [63]. Therefore, answering the question why O<sub>1s</sub> peak shift occurred in  
476 palygorskite in MCP requires further investigation.

477 The deconvolution of C<sub>1s</sub> spectra in MCP (Fig. 7 c) produced four peaks at 284.7, 285.9,  
478 287.1 and 288.5 eV, which were assigned for C-C, C-N, C-O and C=O species, respectively  
479 [64]. The peak fitting of MCP-Pb showed a new peak at 282.2 eV, which was associated with  
480 C-H groups from chitosan (Fig. 7 d) [65]. It was reported that the glucosamine unit (at the  
481 end chain of chitosan polymer) could act as the reducing agent through the hydroxyl groups  
482 at the position 1 of the glucose ring [66], [67]. The oxidation of this group had probably  
483 caused the glucose ring opening, resulting in a more “exposed” carbon on the surface, hence

484 produced a pronounced peak in MCP-Pb (Fig. 7 d). This organic molecule likely caused the  
485 reduction of  $\text{Pb}^{2+}$  to  $\text{Pb}^0$ .

486 The  $\text{N}_{1\text{S}}$  photoelectron spectrum of chitosan in MCP was split into two peaks located at 402.4  
487 and 399.6 eV (Fig. 7 e). The former peak could be attributed to  $\text{NH}_3^+$ , while the later could be  
488 attributed to  $-\text{NH}_2$  species [58], [68]. After  $\text{Pb}^{2+}$  adsorption, a respective 54.4 % and 11.6%  
489 reduction in the peak areas of  $\text{NH}_3^+$  and  $-\text{NH}_2$  in MCP-Pb were observed. In addition, a new  
490 peak at 400.7 eV could be attributed to  $\text{NH}_2\text{-Pb}$  bonding that would have compromised  
491 12.5% of the total  $\text{N}_{1\text{S}}$  peak area (Fig. 7 f). It is expected that upon the formation of nitrogen-  
492 metal complexes, the nitrogen atom would oxidise due to a decrease in electron density  
493 leading to a higher binding energy shift (more than 399 eV) [69], [70]. Therefore, overall  
494 changes observed on  $\text{N}_{1\text{S}}$  photoelectron spectra of MCP-Pb reflected the participation of  
495 nitrogen species of chitosan towards  $\text{Pb}^{2+}$  removal.

496 The photoelectron peaks around 722 and 708 eV were associated with the  $\text{Fe}_{2\text{p}1/2}$  and  $\text{Fe}_{2\text{p}3/2}$ ,  
497 respectively (



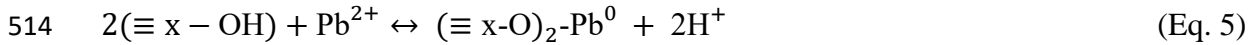
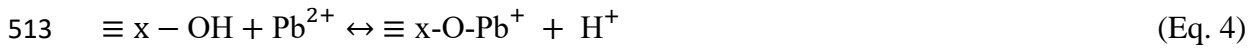
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499 Fig. 7 g). The presence of  $\text{Fe}_3\text{O}_4$  species was indicated by the photoelectron peak at 710.1 eV  
500 (Fig. 7 g) [71]. No significant peak shift was observed for  $\text{Fe}_{2\text{P}}$  in MCP-Pb, nevertheless a  
501 higher peak area for  $\text{Fe}_3\text{O}_4$  (39.5% increase) and a new peak at 708.5 eV (due to  $\text{Fe}_2\text{O}_3$ ) were  
502 identified (Fig. 7 h) [56]. These observations were probably due to the oxidation of FeO to  
503  $\text{Fe}_2\text{O}_3$  and/or  $\text{Fe}_3\text{O}_4$ , which happened on the surface of the iron oxide. As the standard  
504 reduction potential ( $E^\circ$ ) of the half-cell equation  $\text{Pb}_{\text{aq}}^{2+} + 2e^- \rightarrow \text{Pb}^0$  (-0.13 V) was more



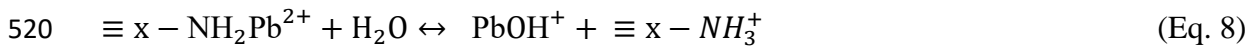
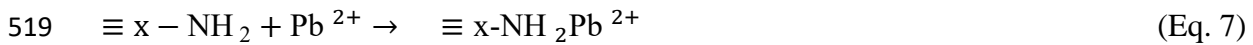
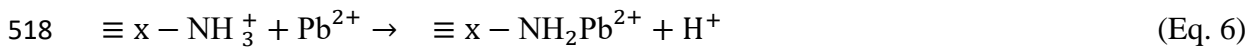
505 positive than the solid state oxidation potential for converting structural  $Fe_s^{2+}$  to  $Fe_s^{3+}$  (-0.65 to  
 506 -0.34 V), a spontaneous heterogeneous redox reaction was expected to take place [72]. The  
 507 reduction of  $Pb^{2+}$  to  $Pb^0$  was therefore possible by the resultant electron flow on the  
 508 magnetite surfaces [72], [73].

509 On the basis of the above data, the removal of Pb by MCP via adsorption and reduction  
 510 mechanisms could be postulated in a sequence of chemical reactions (Eq. 4 to 9). For  $Pb^{2+}$   
 511 adsorption, the surface complexation of Pb with the functional hydroxyl groups leads to a  
 512 decrease in pH, as described in Eq. 4 and 5, respectively:

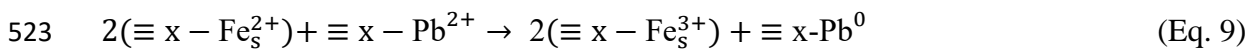


515 where,  $\equiv x-$  represents the active surface sites of MCP.

516 The surface complexation through the amine groups of chitosan could be proposed via the  
 517 following mechanisms (Eq. 6 to 8) [69], [73]:



521 The reduction of  $Pb^{2+}$  to  $Pb^0$  could be catalysed by the oxidation of  $Fe^{2+}$  on the magnetite  
 522 surface, as proposed by the following net cell equation (Eq. 9):



524 The idea of metal reduction phenomena by chitosan is relatively new. Previous studies  
 525 suggested that the reducing ends (functional groups) of chitosan might get oxidised under  
 526 acidic working solution (pH 4) and consequently undertake metal reduction, as proposed in  
 527 studies involving chromate decontamination [74], [75], [76].

528

#### 529 3.4 Adsorbent regeneration study

530 Four  $\text{Pb}^{2+}$  adsorption-desorption cycles on MCP using 0.01 M EDTA were successfully  
531 conducted where the final adsorption test recorded 82%  $\text{Pb}^{2+}$  removal from an initial 100 mg  
532  $\text{L}^{-1}$  adsorbate concentration (Fig. 8(a)). The  $\text{Pb}^{2+}$  desorption percentage decreased to 70% in  
533 the fourth cycle. The TEM image of fresh and spent MCP (after four cycles) (Fig. 8 b & c)  
534 showed the changes in the cohesion between chitosan layers and palygorskite/magnetite  
535 particles. The magnetite and palygorskite particles were distributed more randomly in the  
536 spent MCP than the fresh adsorbent. Nevertheless, the magnetite nanoparticles remained  
537 intact in the chitosan-palygorskite network, suggesting the polymer coating would have  
538 helped to prevent the leaching of iron from the nanocomposite. No significant dry weight loss  
539 of spent MCP was recorded in the final regeneration cycle, and the magnetic susceptibility of  
540 MCP was still preserved ( $M_s = 18.7 \text{ emu g}^{-1}$ ). These findings confirmed the stability of the  
541 nanocomposite in enduring multiple regeneration cycles without significantly losing the  
542 adsorption capacity [77].

543

#### 544 3.5 Comparison with other magnetic nanocomposites

545 The above characterisation and adsorption results provided strong evidence for the potential  
546 use of MCP as an efficient adsorbent to remove  $\text{Pb}^{2+}$  from water. To validate the MCP's  
547 performance, a comparison with other magnetic nanocomposites used for removing  $\text{Pb}^{2+}$  was  
548 conducted (Table 4). The MCP showed a good performance in terms of maximum adsorption  
549 capacity considering the wide initial  $\text{Pb}^{2+}$  concentration range, low adsorbent loading and  
550 high performance at acidic pH used in experiments (Table 4). Nevertheless, the magnetic  
551 susceptibility of MCP was relatively low compared to other magnetic adsorbents, which  
552 gives an opportunity for further research development in this area.

553

#### 554 **4. Conclusions**

555 A novel one-pot synthesis of magnetic chitosan-palygorskite (MCP) nanocomposite was  
556 achieved in this study avoiding the typical steps of clay pre-purification and without using  
557 any organic solvent, which otherwise were routinely needed in previously reported  
558 nanocomposite synthesis procedures. A suite of state-of-the-art characterization techniques  
559 provided evidences for the synergic roles of each component (polymeric chitosan, fibrous  
560 palygorskite and nanosized iron oxides) of the nanocomposite either as a structural  
561 reinforcement or reactivity enhancer towards  $\text{Pb}^{2+}$ . The palygorskite acted as an outstanding  
562 support for the nucleation of iron oxide nanoparticles and simultaneously provided stability to  
563 chitosan within the nanocomposite matrix. Hence, this research may escalate scientific  
564 interests for investigating palygorskite as a superior choice of clay minerals to prepare  
565 polymer-clay nanocomposites alongside other dominating mineral candidates such as  
566 montmorillonite, sepiolite and vermiculite that are frequently reported in literature.  
567 The MCP showed a considerable  $\text{Pb}^{2+}$  adsorption capacity ( $58.5 \text{ mg g}^{-1}$ ), occurring primarily  
568 via surface complexation and chemical reduction mechanisms, as revealed via fitting of the  
569 experimental adsorption data to fundamental isotherm, kinetic and thermodynamic models  
570 coupled with authentication through detailed spectroscopic and magnetic susceptibility  
571 analyses. The above approach could be employed to unravel removal mechanisms of aquatic  
572 contaminants using a range of adsorbents, and hence deciding the adsorbent's effective  
573 performance life and suitable disposal pathway following usage. Moreover, the  $\text{Pb}^{2+}$  removal  
574 performance of the MCP remained almost unaffected up to four adsorption-desorption cycles  
575 (using 0.01 M EDTA) with negligible loss of the adsorbent's magnetic susceptibility, which  
576 would help to mitigate uncertainties around the durability of magnetic adsorbents for water  
577 treatment in future studies.

578 Overall, this study provides a novel green approach for the preparation of magnetic  
579 nanocomposites using natural clay minerals and biowastes (chitosan) for potential  
580 applications in environmental heavy metal remediation. Future investigations are needed to  
581 further improve the magnetic susceptibility of the nanocomposite, assess its performance of  
582 heavy metal removal from real wastewater, and evaluate the nanocomposite's  
583 ecotoxicological impacts, if any.

584

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595

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- 833

834 **Figure legends**

835 Fig. 1. Characteristic features of chitosan, palygorskite (Pal), iron oxide (IO) and magnetic  
836 chitosan-palygorskite nanocomposite (MCP): (a) XRD pattern (p = palygorskite, q= quartz, d  
837 = dolomite, k = kaolinite, m = magnetite), (b) magnetisation curve of MCP, (c) TGA curves,  
838 and (d) DTGA profiles. Inset in Fig. 1(b) is the photo of magnetically separated MCP.

839 Fig. 2. Back scattered SEM image (a), EDX spectra (b), Bright Field (c) and Dark Field (d)  
840 STEM images of MCP

841 Fig. 3. Schematic illustration (not to scale) on the proposed reaction mechanism (a) and the  
842 flow diagram (b) for the synthesis of MCP

843 Fig. 4. Adsorption kinetics analysis of Pb adsorption by MCP: (a) intra-particle diffusion plot,  
844 (b) Boyd plot

845 Fig. 5. FTIR spectra of MCP (before adsorption) and Pb<sup>2+</sup> loaded-MCP (MCP-Pb) (after  
846 adsorption)

847 Fig. 6. XPS spectra of MCP and Pb-loaded MCP (MCP-Pb): (a) survey scan, (b) high  
848 resolution scan for Pb<sub>4f</sub>

849 Fig. 7. High Resolution XPS spectra of MCP and Pb-loaded MCP (MCP-Pb): (a-b) O<sub>1s</sub>, (c-d)  
850 C<sub>1s</sub>, (e-f) N<sub>1s</sub>, and (g-h) Fe<sub>2p</sub>

851 Fig. 8. Adsorption-desorption cycle of MCP: (a) Comparison on Pb<sup>2+</sup> adsorption and  
852 desorption (in percentage) by MCP during four subsequent regeneration cycles (error bars  
853 represent the standard error at 95% confidence level, n = 2), (b & c): TEM images of fresh (b)  
854 and spent MCP after a four adsorption-desorption cycles (c)

855



856 **Title of tables**

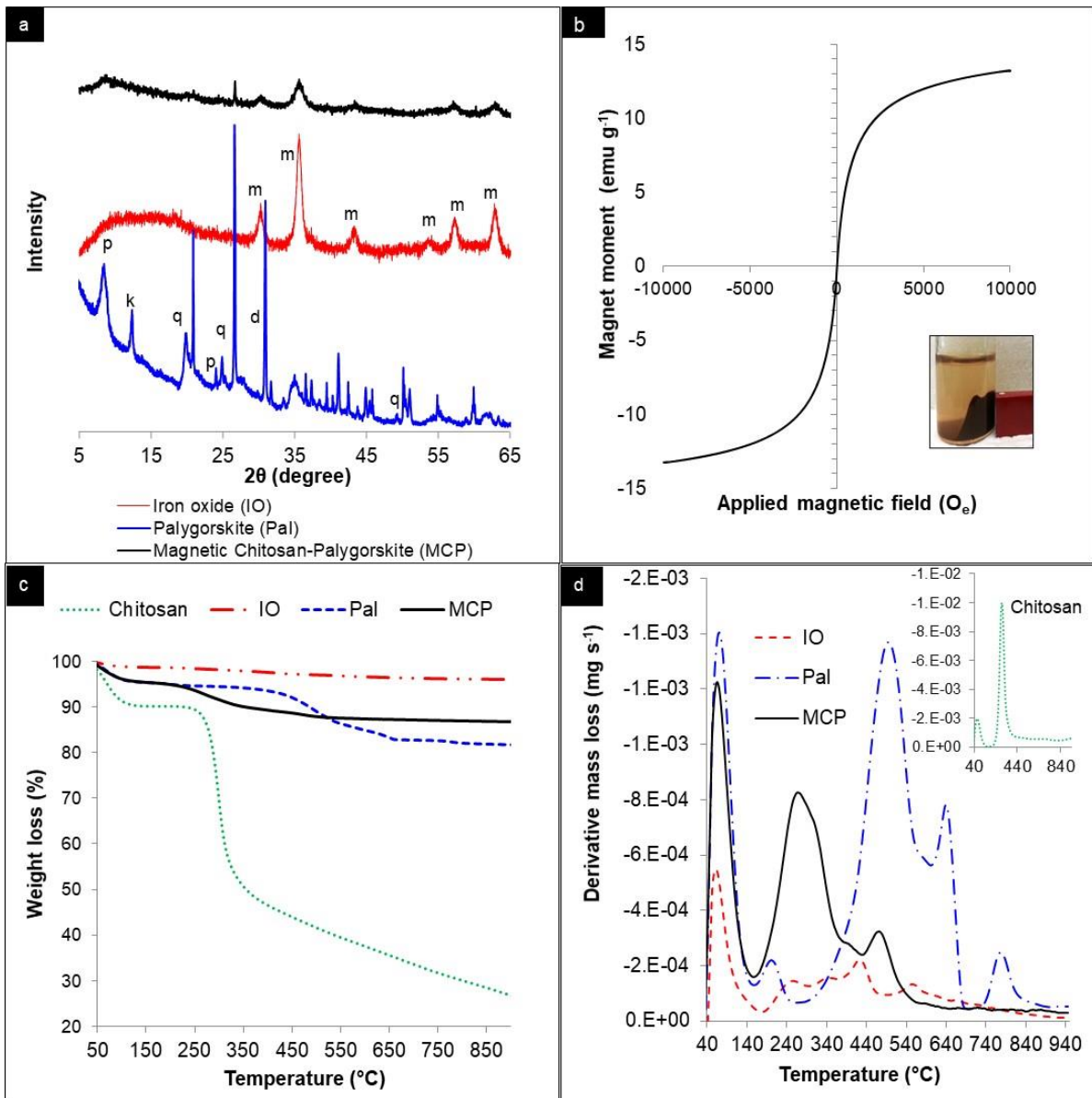
857 Table 1. Specific surface area, pore volume and pore diameter of palygorskite (Pal), iron  
858 oxide (IO) and magnetic chitosan-palygorskite nanocomposite (MCP).

859 Table 2. Langmuir, Freundlich, Dubinin–Radushkevich and Temkin model parameters for  
860  $\text{Pb}^{2+}$  adsorption by magnetic chitosan-palygorskite nanocomposite (MCP) ( $p < 0.05$ ,  $n = 2$ ).

861 Table 3. Adsorption kinetic model parameters of  $\text{Pb}^{2+}$  adsorption by MCP (initial  $\text{Pb}^{2+}$   
862 concentration =  $200 \text{ mg L}^{-1}$ , at  $25^\circ\text{C}$ , under 150 agitation per min with  $5 \text{ g L}^{-1}$  adsorbent  
863 loading) at  $p < 0.05$ ,  $n = 2$ .

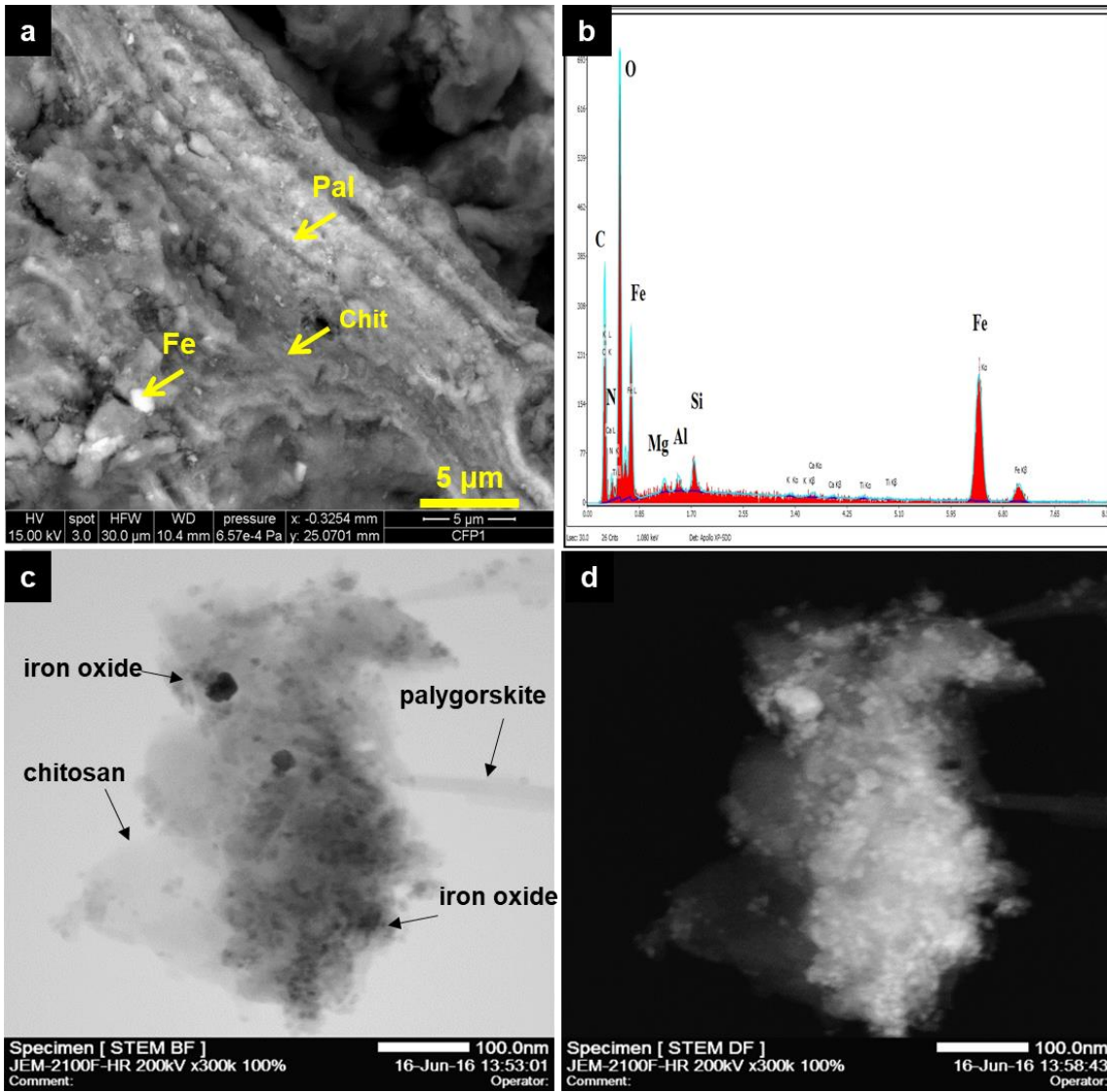
864 Table 4. Comparison of the efficiency of  $\text{Pb}^{2+}$  adsorption by magnetic composites based on  
865 important experimental parameters.

866



**Fig. 1.**

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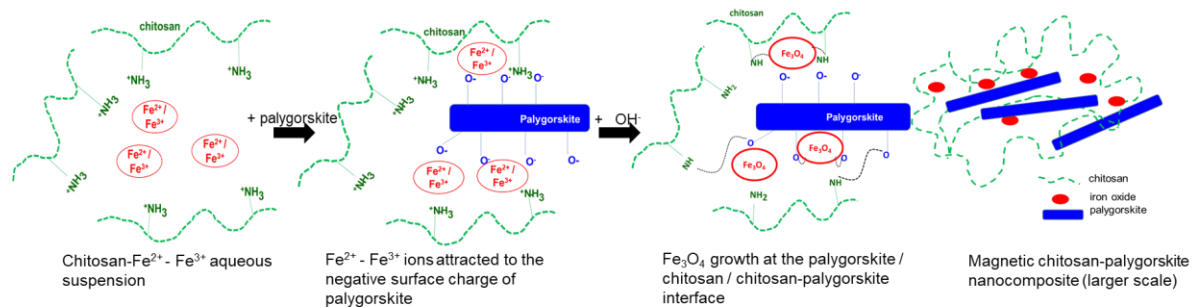


871

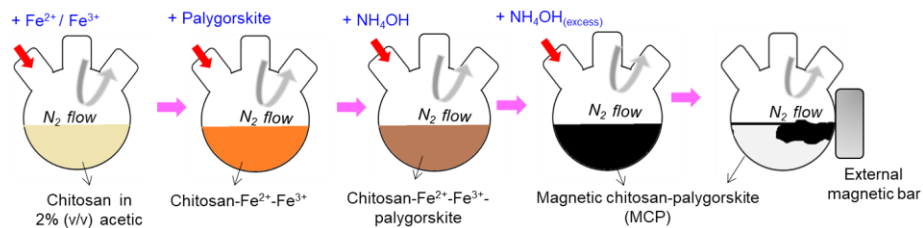
872 Fig. 2.

873

**a. Proposed synthesis reaction mechanism**



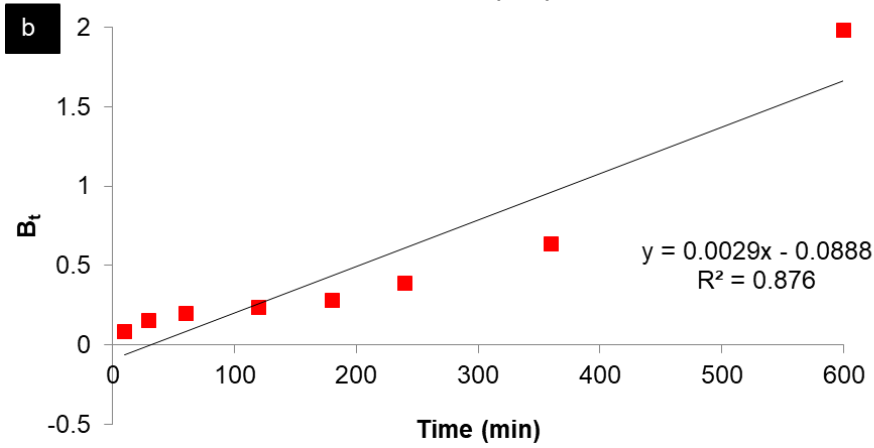
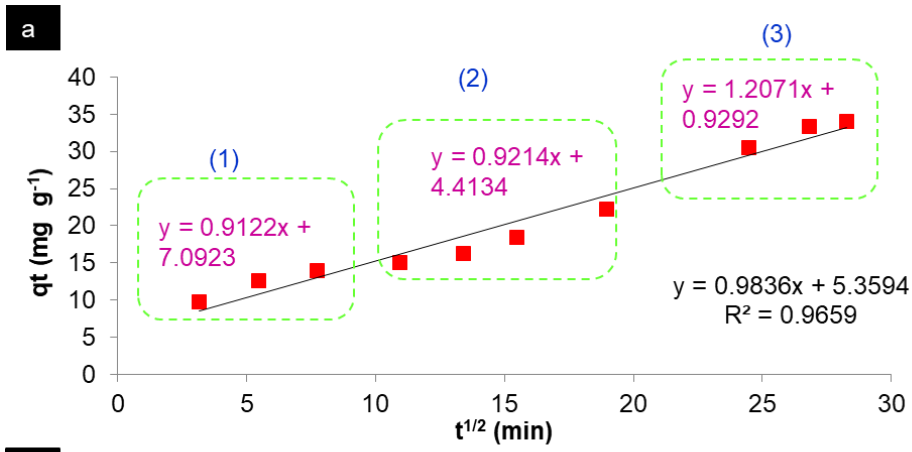
**b. Flow diagram for the synthesis of MCP**



874

875 Fig. 3.

876

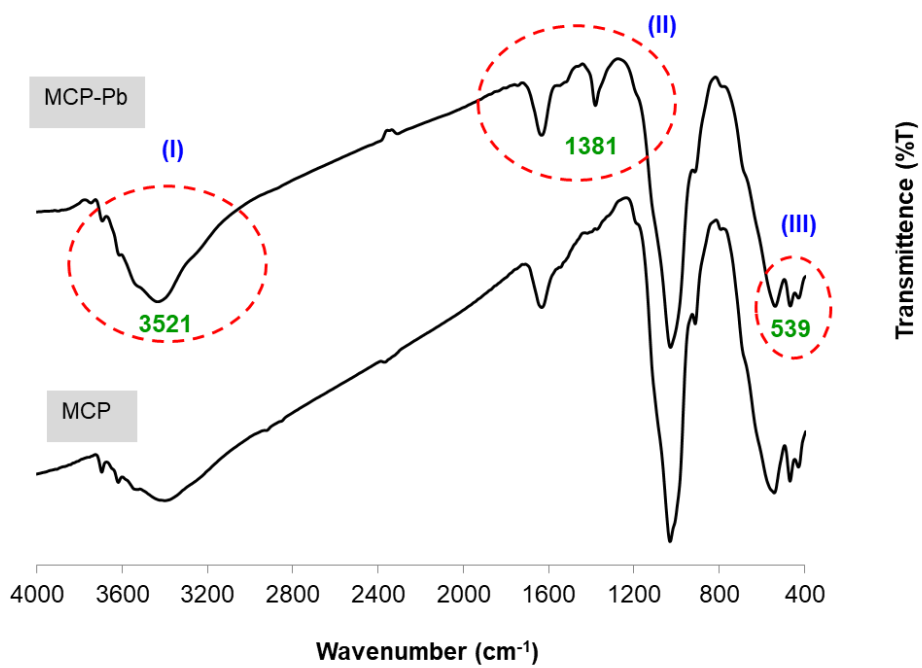


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879 Fig. 4.

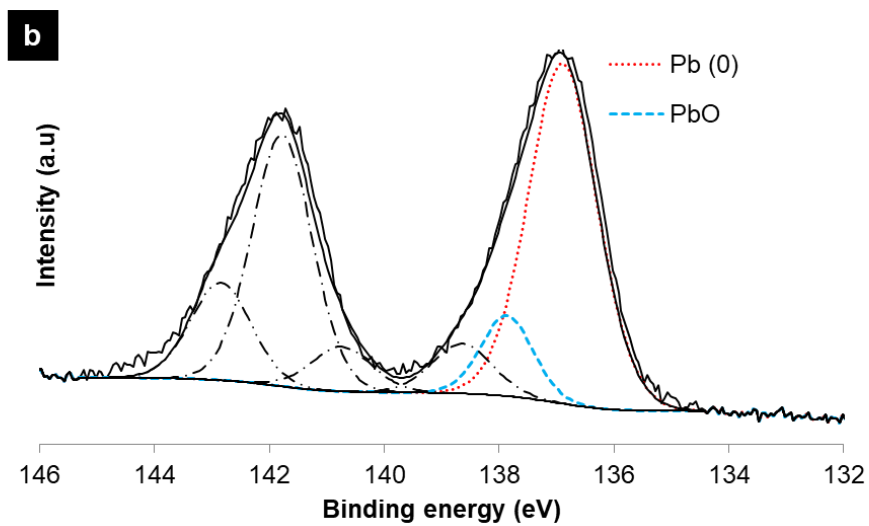
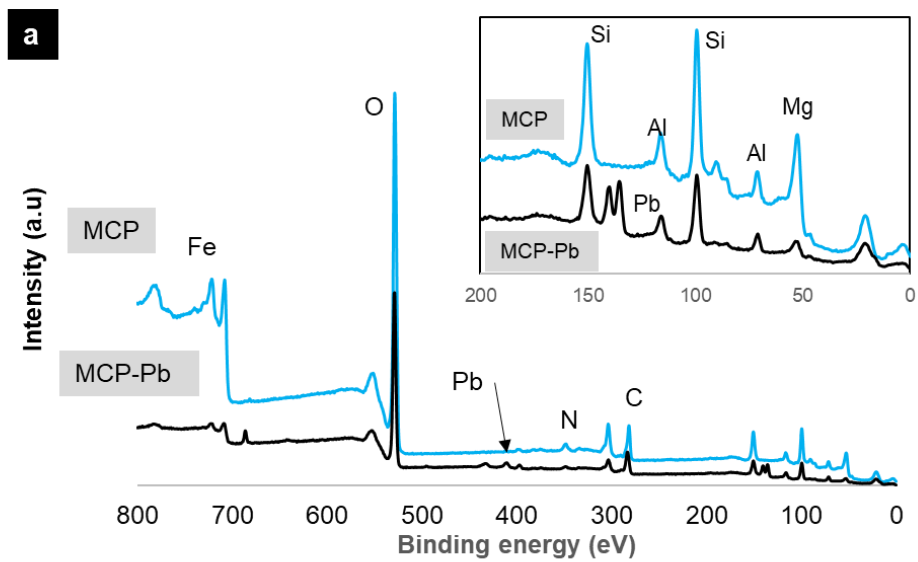
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882 Fig. 5.

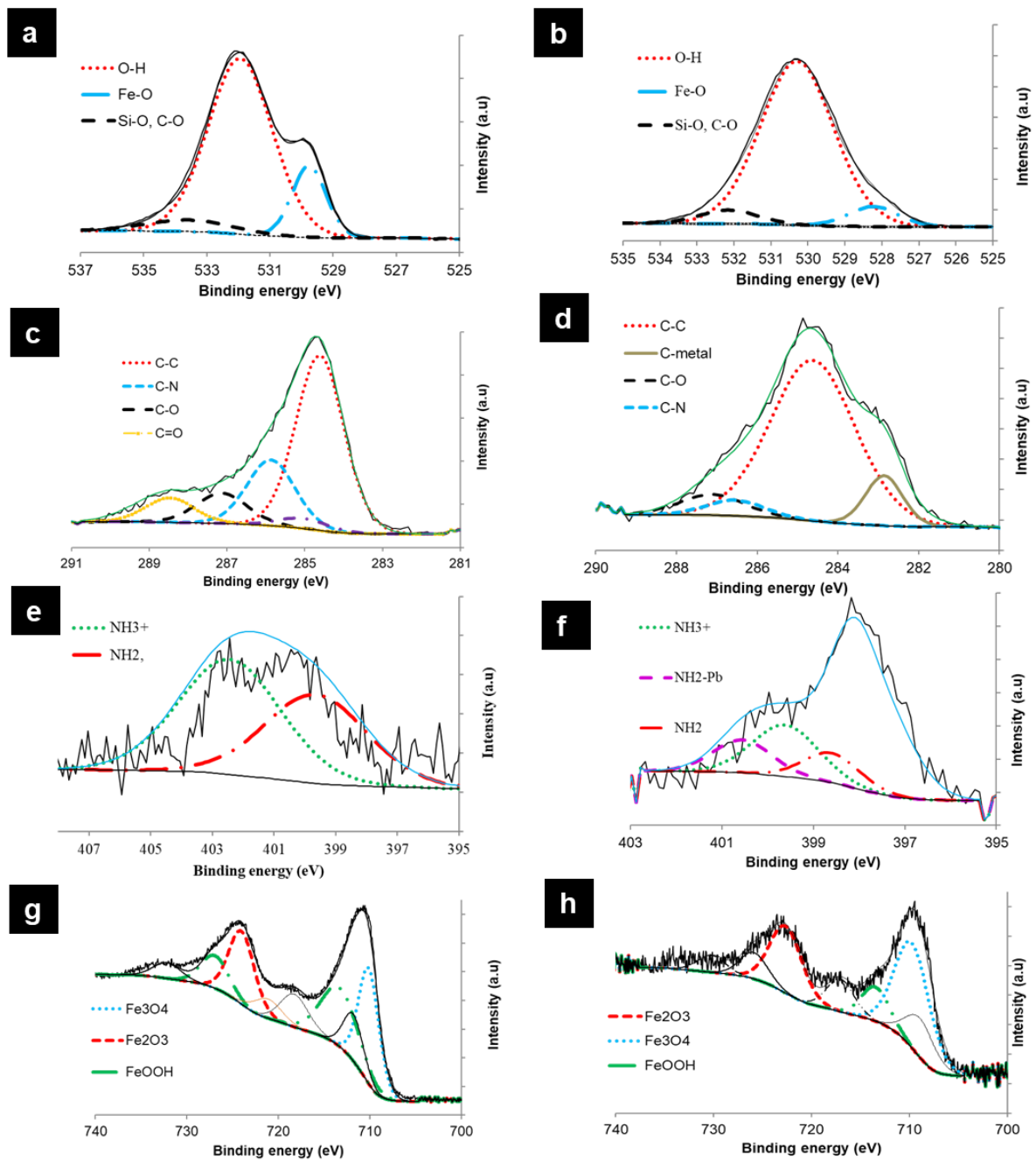
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885 Fig. 6.

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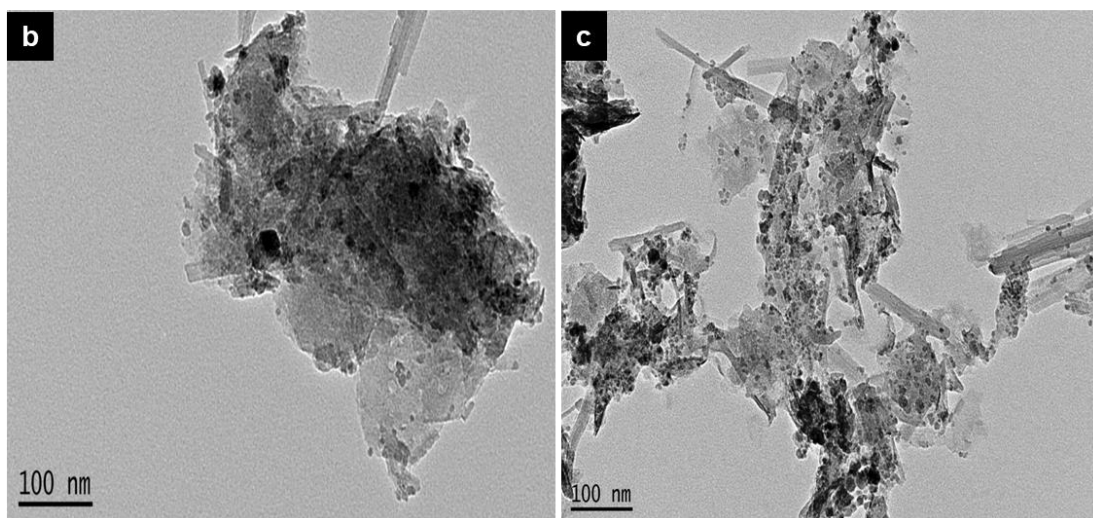
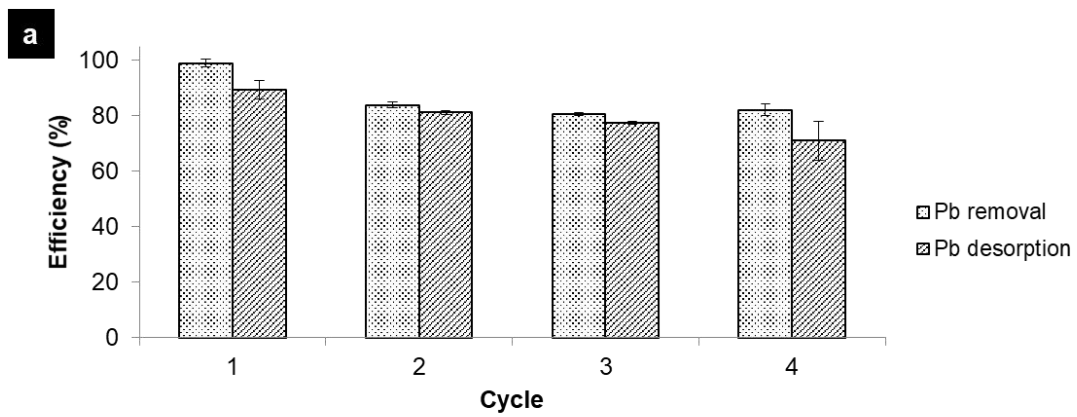


887

888 Fig. 7.

889





890

891 Fig. 8.

892

893 **Tables**

894 Table 4. Specific surface area, pore volume and pore diameter of palygorskite (Pal), iron  
895 oxide (IO) and magnetic chitosan-palygorskite nanocomposite (MCP).

Parameter	Pal	IO	MCP
Specific surface area ( $\text{m}^2 \text{g}^{-1}$ )	49.4	72.6	18.3
Average pore volume ( $\text{cm}^3 \text{g}^{-1}$ )	0.127	0.215	0.038
Average pore size ( $\text{\AA}$ )	93.0	100	82.1

896

897 Table 5. Langmuir, Freundlich, Dubinin–Radushkevich and Temkin model parameters for  
 898  $\text{Pb}^{2+}$  adsorption by magnetic chitosan-palygorskite nanocomposite (MCP) ( $p < 0.05$ ,  $n = 2$ ).

Models/parameters	Value
<i>Langmuir</i>	
$q_{\max}$ calculated ( $\text{mg g}^{-1}$ )	63.3
$K_L$ ( $\text{L mg}^{-1}$ )	0.0524
$R^2$	0.9855
$q_{\max}$ (experimental) ( $\text{mg g}^{-1}$ )	58.5
<i>Freundlich</i>	
$K_F$ ( $\text{L g}^{-1}$ )	9.415
$N$	2.846
$R^2$	0.9820
<i>Dubinin-Radushkevich (D-R)</i>	
$q_{\max}$ ( $\text{mg g}^{-1}$ )	91.4
$\beta$ ( $\times 10^{-9} \text{ mol}^2\text{J}^{-2}$ )	3.00
$E$ ( $\text{kJ mol}^{-1}$ )	12.90
$R^2$	0.8059
<i>Temkin</i>	
$b_T$ ( $\text{J mol}^{-1}$ )	22.61
$A_T$ ( $\text{L g}^{-1}$ )	0.9087
$R^2$	0.8708

899

900 Table 6. Adsorption kinetic model parameters of  $\text{Pb}^{2+}$  adsorption by MCP (initial  $\text{Pb}^{2+}$   
 901 concentration =  $200 \text{ mg L}^{-1}$ , at  $25^\circ\text{C}$ , under 150 agitation per min with  $5 \text{ g L}^{-1}$  adsorbent  
 902 loading) at  $p < 0.05$ ,  $n = 2$ .

Kinetics models / Parameters	value
<i>Pseudo-first order</i>	
$k_1 (\text{min}^{-1})$	$7.60 \times 10^{-3}$
$q_{\text{max}} (\text{mg g}^{-1})$	26.8
$R^2$	0.9139
<i>Pseudo-second order</i>	
$k_2 (\text{g mg min}^{-1})$	$23.6 \times 10^{-3}$
$q_{\text{max}} (\text{mg g}^{-1})$	35.8
$R^2$	0.9227
<i>Intra-particle diffusion</i>	
$k_i (\text{mg g}^{-1} \text{min}^{0.5})$	0.9836
C	5.359
$R^2$	0.9659
<i>Elovich</i>	
$\alpha (\text{mg g}^{-1} \text{min}^{-1})$	1.404
$\beta (\text{g mg}^{-1})$	0.1795
$R^2$	0.8044

903

904 Table 4. Comparison of the efficiency of Pb<sup>2+</sup> adsorption by magnetic composites based on important experimental parameters.

Material	Working pH	Adsorbent loading (g L <sup>-1</sup> )	Initial Pb <sup>2+</sup> concentration (mg L <sup>-1</sup> )	Maximum adsorption capacity (mg g <sup>-1</sup> )	Magnetic susceptibility (emu g <sup>-1</sup> )	Total regeneration cycles and percent removal (%) at the cycle end	Reference
Chitosan-graft- polyacrylamide magnetic composite microspheres	5	10	200	63.7	7.60	N/G*	[78]
Chitosan-magnetite	6	0.1	50 – 80	63.3	55.0	N/G	[79]
Magnetic chitosan nanocomposite	4	3.0	10	3.16	74.0	6 cycles, 93%	[80]
Magnetic Chitosan /graphene oxide composites	5	8.0	N/G	76.9	39.6	5 cycles, 75%	[81]
Palygorskite-iron oxide nanocomposite	5	5.0	20 – 500	26.6	18.3	3 cycles, 64%	[23]

Polyamide-amine dendritic magnetic halloysite nanotubes	5.6	0.5	50 – 200	194	~3.0	8 cycles, 90.6%	[82]
Magnetic nanoparticles coated montmorillonite	6.5	0.002	N/G	38.2	15.0	5 cycles, N/G	[83]
hydroxyapatite- magnetite-bentonite composite	8	2.0	20 – 2100	404	13.2	5 cycles, 86%	[84]
Magnetic sepiolite Clay	6	2.5	N/G	96.2	28.1	5 cycles, ~80%	[85]
Magnetic kaolinite clay	6	1.0	10 – 70	30.9	N/G	N/G	[86]
Magnetic chitosan - palygorskite	4	5.0	50 – 500	58.5	14.3	4 cycles, 82%	This study

905

906 \*N/G: Not given.

907



932 **SD 1: Adsorption isotherm models**

933 *Langmuir isotherm*

934 Langmuir adsorption isotherm is characterized by monolayer adsorption of adsorbate on a  
935 homogeneous adsorbent surface [1]. The Langmuir isotherm is expressed by the equations 1  
936 and 2:

937  $q_e = (K_L C_e q_m)/(1 + K_L C_e)$  (Eq. 1)

938  $C_e/q_e = 1/(K_L q_m) + C_e/q_m$  (Eq. 2)

939 where,  $q_e$  is the amount of adsorbate adsorbed per unit mass of adsorbent ( $\text{mg g}^{-1}$ );  $C_e$  is the  
940 equilibrium adsorbate concentration ( $\text{mg L}^{-1}$ ).  $K_L$  and  $q_m$  are Langmuir constants which stand  
941 for bonding energy constant ( $\text{L mg}^{-1}$ ) and maximum monolayer adsorption ( $\text{mg g}^{-1}$ ),  
942 respectively. By plotting  $C_e/q_e$  versus  $C_e$ , the obtained slope of this plot gives  $1/q_m$  and  
943 intercept gives  $1/q_m K_L$ . Hence, we calculated the Langmuir constant values from the slope  
944 and intercept of the plot.

945

946 *Freundlich isotherm*

947 The Freundlich isotherm is an exponential expression which suggest that amount of  
948 adsorption increases with increase in adsorbate concentration [2]. The Freundlich isotherm is  
949 more suitable for heterogeneous adsorbent surface which is expressed by equations 3 and 4:

950  $q_e = K_F C_e^{1/n}$  (Eq. 3)

951  $\ln q_e = \ln K_F + \frac{1}{n} (\ln C_e)$  (Eq. 4)

952 where,  $q_e$  is the amount of adsorbate adsorbed per unit mass of adsorbent ( $\text{mg g}^{-1}$ );  $C_e$  is the  
953 equilibrium adsorbate concentration ( $\text{mg L}^{-1}$ ).  $K_F [(\text{mg g}^{-1}) (\text{L mg}^{-1})^{1/n}]$  and  $1/n$  are Freundlich  
954 constant at equilibrium and exponential factor, respectively. By plotting  $\ln q_e$  versus  $\ln C_e$ ,  
955 Freundlich constants values were calculated from slope  $1/n$  and intercept  $\ln K_F$ .

956



957 *Dubinin- Radushkevich (D-R) isotherm*

958 The D-R model is able to distinguish the nature of metal adsorption either physical or  
959 chemical [3] by measuring the mean free energy,  $E$  (the free energy of transfer of 1 mole of  
960 solute from infinity in solution to the surface of adsorbent).

961 The D-R model constant,  $\beta$  ( $\text{mol}^2 \text{J}^{-2}$ ), is determined by equations 5 and 6 [4]:

962 
$$\ln q_e = \ln q_{\max} - \beta \varepsilon^2 \quad (\text{Eq. 5})$$

963 
$$\varepsilon = RT \ln \left[ 1 + \left( \frac{1}{C_e} \right) \right] \quad (\text{Eq. 6})$$

964 where,  $q_e$  is the amount of metal adsorbed at equilibrium ( $\text{mg g}^{-1}$ ) and  $q_{\max}$  is the maximum  
965 adsorption capacity ( $\text{mg g}^{-1}$ ). Meanwhile  $R$ ,  $T$ , and  $\varepsilon$  is the gas constant ( $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ ),  
966 temperature (K) and the Polanyi potential ( $\text{J}^2 \text{ mol}^{-2}$ ), respectively. The  $\beta$  and  $q_{\max}$  can be  
967 calculated from the slope and intercept of the D-R model plot.

968 The relationship between the  $\beta$  value and mean free energy of adsorption ( $E$ ) ( $\text{kJ mol}^{-1}$ ) is  
969 derived from equation 7:

970 
$$E = -\frac{1}{\sqrt{2\beta}} \quad (\text{Eq. 7})$$

971

972 *Temkin isotherm*

973 Temkin isotherm model considers the interaction effect between adsorbate and adsorbent on  
974 adsorption phenomenon. The model suggests that heat of adsorption would decrease linearly  
975 with surface coverage due to the adsorbate-adsorbent interaction [5]. The Temkin isotherm  
976 can be expressed by equations 8 and 9:

977 
$$q_e = (RT/b_T) \ln (A_T C_e) \quad (\text{Eq. 8})$$

978 
$$q_e = B \ln A_T + B \ln C_e \quad (\text{Eq. 9})$$

979 where,  $q_e$  is the amount of adsorbate adsorbed per unit mass of adsorbent ( $\text{mg g}^{-1}$ ),  $B = RT/b_T$ ,  
980  $b_T$  is the Temkin constant related to heat of sorption ( $\text{J mol}^{-1}$ ),  $A_T$  is the Temkin isotherm  
981 constant ( $\text{L g}^{-1}$ ),  $R$  is the gas constant ( $8.314 \text{ J. mol}^{-1} \text{ K}^{-1}$ ), and  $T$  is the absolute temperature  
982 (K).

983

## 984 **SD2: Adsorption kinetic models**

### 985 *Pseudo-first order kinetic model*

986 The assumption of this model is the sorption rate abates linearly with the adsorption capacity  
987 [6]. It is expressed by the equations below:

$$988 \quad q_t = q_e (1 - e^{-k_1 t}) \quad (\text{Eq. 10})$$

$$989 \quad \ln (q_e - q_t) = \ln q_e - k_1 t \quad (\text{Eq. 11})$$

990 where,  $q_e$  and  $q_t$  are the amount of adsorption at equilibrium and time  $t$ , respectively ( $\text{mg g}^{-1}$ ),  
991  $k_1$  is the rate constant of pseudo first-order adsorption ( $\text{min}^{-1}$ ). By plotting  $\ln (q_e - q_t)$  versus  $t$ ,  
992 we obtained the slope  $k_1$  and intercept  $\ln q_e$ .

993

### 994 *Pseudo-second order kinetic model*

995 The pseudo-second-order kinetic model is usually utilized to elucidate a chemical sorption and  
996 it considers the rate-limiting step is the interaction between two reagent particles [7]. It is  
997 expressed by the equations below:

$$998 \quad q_t = \frac{q_e^2 k_2 t}{1 + q_e k_2 t} \quad (\text{Eq. 12})$$

$$999 \quad t/q_t = 1/k_2 q_e^2 + t/q_e \quad (\text{Eq. 13})$$

1000 where,  $q_e$  and  $q_t$  are the amount of adsorption at equilibrium and time  $t$ , respectively ( $\text{mg g}^{-1}$ ),  
1001  $k_2$  is the rate constant of pseudo first-order adsorption ( $\text{g mg}^{-1} \text{ min}^{-1}$ ). By plotting  $t/q_t$  versus  $t$ ,  
1002 we obtain the slope  $1/q_e$  and intercept  $1/k_2 q_e^2$ .

1003

1004 *Intra-particle diffusion model*

1005 Intra-particle diffusion model is characterized by diffusion where the adsorption process is  
1006 dependent upon speed of adsorbate diffusion through adsorbent [8]. By plotting  $q_t$  versus  $t^{0.5}$ ,  
1007 we obtain the constant  $k_i$  ( $\text{mg g}^{-1}\text{min}^{-1/2}$ ) from slope and  $C$  ( $\text{mg g}^{-1}$ ) from the intercept.

1008  $q_t = k_i t^{1/2} + C$  (Eq. 14)

1009

1010 *Elovich model*

1011 Elovich model is characterized by chemisorption nature of adsorption kinetic process related  
1012 to surface coverage [9] and expressed by the equations 15 and 16. By plotting  $q_t$  versus  $\ln(t)$ ,  
1013 we obtain the slope  $1/\beta$  and intercept  $1/\beta \ln(\alpha\beta)$ .

1014  $dq_t/dt = \alpha e^{-(\beta \cdot q_t)}$  (Eq. 15)

1015  $q_t = 1/\beta \ln(\alpha\beta) + 1/\beta \ln(t)$  (Eq. 16)

1016 where,  $q_t$  is the sorption capacity at time  $t$  ( $\text{mg g}^{-1}$ ),  $\alpha$  is the initial sorption rate ( $\text{mg g}^{-1} \text{min}^{-1}$ ),  
1017 and the parameter  $\beta$  is related to the extent of surface coverage and activation energy for  
1018 chemisorption ( $\text{g mg}^{-1}$ ).

1019

1020 *Boyd model*

1021 The model was expressed as a function of  $F$ , described as the fraction of solute adsorbed at a  
1022 specific time ( $q_t$ ,  $\text{mg g}^{-1}$ ) and at equilibrium ( $q_e$ ,  $\text{mg g}^{-1}$ ), calculated through the expression  $F$   
1023  $= q_t/q_e$ .

1024 The Boyd parameter ( $B_t$ ) could be determined through equations 17 or 18, depending on the  
1025 value of  $F$  [10].

1026 For  $F < 0.85$ :  $B_t = 2\pi - \frac{\pi^2 F}{3} - 2\pi \left( \frac{1 - \pi F}{3} \right)^{1/2}$  (Eq. 17)

1027 For  $F > 0.85$ :  $B_t = -\ln(1 - F) - 0.4977$  (Eq. 18)

1028 **SD3: Thermodynamic analysis**

1029 The standard Gibbs free energy change of adsorption ( $\Delta G^\circ$ ) (sup info) was determined by the  
1030 classic Van't Hoff equation (equation 19):

1031 
$$\Delta G^\circ = -RT \ln K \quad (\text{Eq. 19})$$

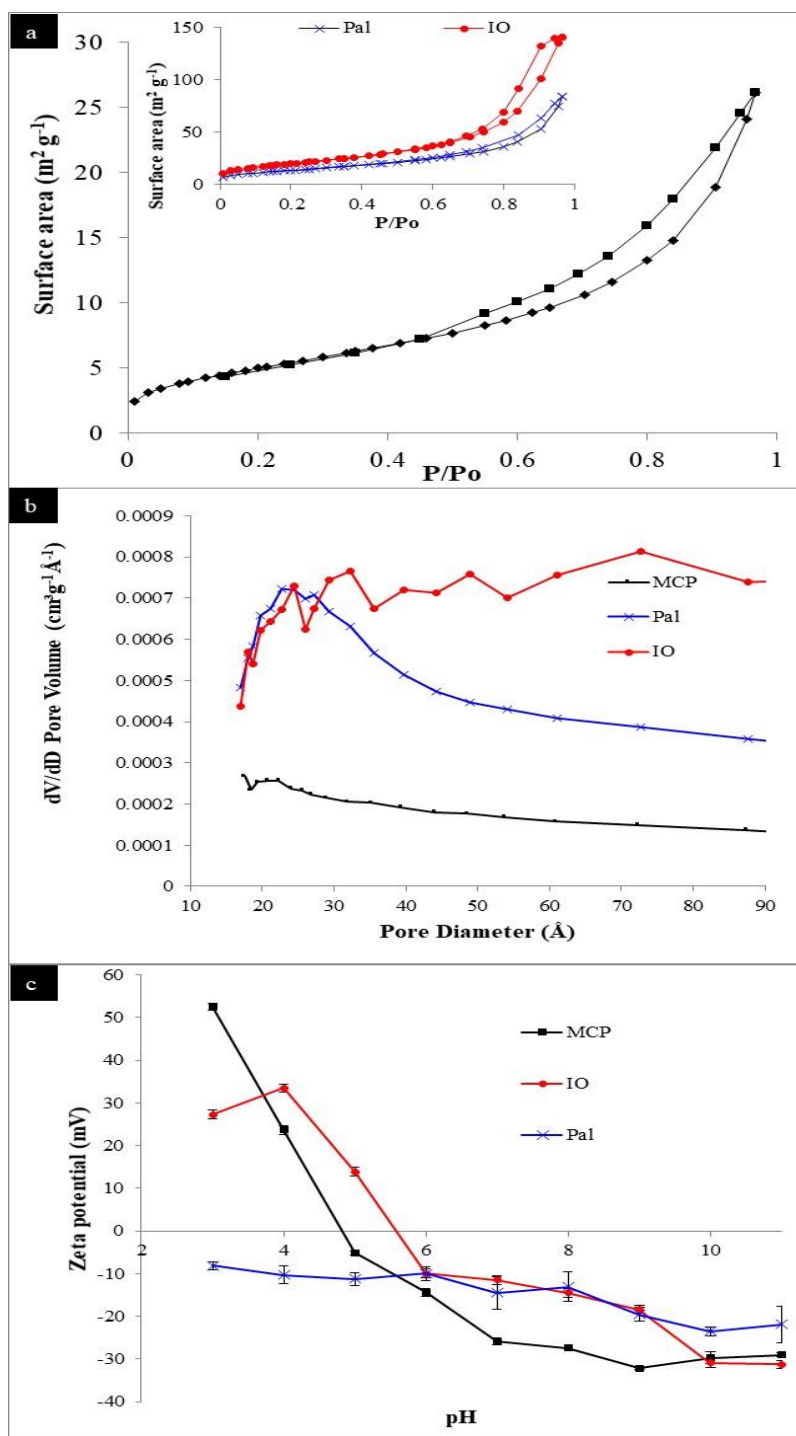
1032 where, R is the universal gas constant ( $8.314 \text{ J mol}^{-1}\text{K}^{-1}$ ) and K is the equilibrium constant at  
1033 the temperature T (K).  $K_D$ , a distribution coefficient constant (dimensionless) was used to  
1034 represent the K [11] and was calculated through equation 20:

1035 
$$K_D = \frac{q_e}{C_e} \quad (\text{Eq. 20})$$

1036 where  $q_e$  and  $C_e$  is respectively the equilibrium adsorption capacity ( $\text{mg g}^{-1}$ ) and  
1037 concentration at equilibrium ( $\text{mg L}^{-1}$ ). By using a derivative Van't Hoff equation (equation  
1038 21), the standard enthalpy of adsorption ( $\Delta H^\circ$ ) and entropy of adsorption ( $\Delta S^\circ$ ) were  
1039 determined through plotting  $\ln K_D$  versus  $1/T$  [11]. From this graph, the magnitude of  $\Delta H^\circ$   
1040 was calculated from the slope, while  $\Delta S^\circ$  was derived from the intercept.

1041 
$$\ln K_D = \frac{\Delta S^\circ}{R} - \frac{\Delta H^\circ}{RT} \quad (\text{Eq. 21})$$

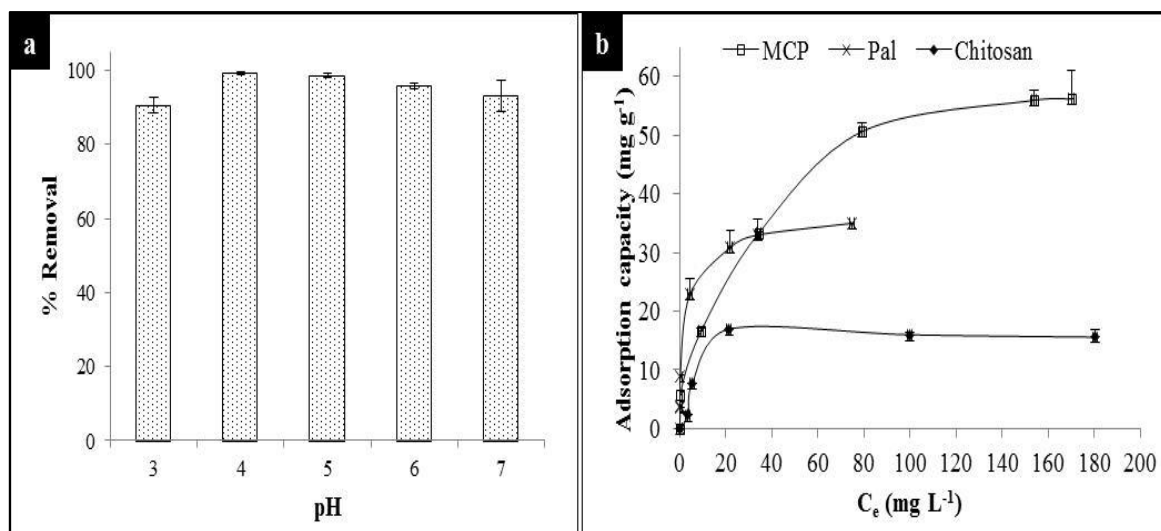
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1044

1045 **Fig. S1.** N<sub>2</sub> adsorption-desorption isotherm (a), pore size distribution (b), and zeta  
1046 potential values (c) of magnetic chitosan-palygorskite composite (MCP), iron oxide (IO) and  
1047 palygorskite (Pal). Error bars represent standard error at 95% confidence level, n = 2.

1048



1049

1050 **Fig. S2.** Adsorption of  $Pb^{2+}$  on MCP: (a) influence of pH on  $Pb^{2+}$  removal (at initial  $Pb^{2+}$   
 1051 concentration of  $50\text{ mg L}^{-1}$ ), (b) adsorption isotherms of MCP, palygorskite (Pal) and chitosan  
 1052 (at  $25^{\circ}\text{C}$  with 150 agitations per min and  $5\text{ g L}^{-1}$  adsorbent loading) (Error bars represent  
 1053 standard error at 95% confidence level,  $n = 2$ ).

1054

1055 **Supplementary tables**

1056 **Table S1.** Thermodynamic parameters of Pb<sup>2+</sup> adsorption by MCP at different temperatures  
 1057 and initial concentrations

Initial [Pb <sup>2+</sup> ] (mg L <sup>-1</sup> )	Adsorption capacity (mg g <sup>-1</sup> )			$\Delta G^\circ$ (kJ mol <sup>-1</sup> )			$\Delta H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
	25°C	40°C	55°C	25°C	40°C	55°C		
	50	5.74	7.01	12.3	-103	-108	-113	118
100	16.6	21.2	22.1	-29.4	-30.9	-32.4	40.9	98.8
200	33.3	38.2	35.6	-11.3	-11.9	-12.4	25.8	38.0

1058

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