NADH Regeneration: A Case Study of Pt-catalyzed NAD⁺

Reduction with H₂

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Abstract:

This study shows the importance of resolving catalytic performance in the regeneration of the

reduced form of nicotinamide adenine dinucleotide (NADH) through activity measurements based

on NAD⁺ conversion and the closure of mass balance via by-product quantification. This approach is

applied to assess the performance of supported platinum catalysts with varying points of zero

charge, utilizing H₂ as a reductant. It was found that Pt/SiO₂, which exhibits a net negative charge

under the reaction conditions, outperforms the neutral Pt/C and positively charged Pt/MgO due to

the favorable electrostatic attraction between the catalyst surface and positively charged (+1)

nicotinamide ring. NMR spectroscopy identifies side-products formed during NAD⁺ hydrogenation.

Keywords: cofactor; supported Pt; conversion; selectivity; mass balance; by-product

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Oxidoreductases account for one-fourth of all known enzymes and with their exclusive and highly desirable properties (high activity, enantioselectivity and mild operating conditions), they have been used in a wide range of biotransformations, including the synthesis of chemicals and pharmaceuticals, biodegradation and detoxification. 1.2 The majority of oxidoreductases depend on a nicotinamide adenine dinucleotide cofactor in its reduced form, NAD(P)H, or its oxidized form, NAD(P)+, to transfer the required reducing or oxidizing equivalent to the substrate. Despite being prolific cofactors, the high cost and the stoichiometric amounts required make the consumption of these cofactors impractical. This has motivated significant research in recycling NAD(P)H from NAD(P)+ to make the reductive process economically feasible (Scheme 1). Over the last 50 years, NAD(P)H regeneration using biocatalytic, chemical, electrochemical, photochemical, homogeneous catalytic and heterogeneous catalytic methods have been investigated. 4.5

It is noteworthy that the reported regeneration studies have almost exclusively used the yield of NAD(P)H (either validated or unvalidated by enzymatic assays) as a performance indicator.⁶⁻²¹ It would not be an issue for enzymatic regeneration as enzymes are intrinsically selective meaning the yield is equivalent to conversion. This is, however, not applicable for non-enzymatic regeneration as it has been frequently reported that unselective products (e.g., the enzymatically inactive 1,6-NADH, 1,2-NADH, NAD₂ dimers and cofactor decay products,¹⁷⁻²¹ Scheme 1) can be formed. In fact, for any other catalytic reaction system, conversion and selectivity are indeed more fundamental and typically discussed. A thorough search of the literature did not unearth any studies reporting experimentally measured NAD(P)+ conversion, except when a validated yield approaches ~100% as convincingly demonstrated by the works of Antonietti (photocatalysis²²), Fukuzumi (homogeneous catalysis²³) and Minteer (electrocatalysis²⁴). When the yield is lower, as is the case in most studies, relying on the yield of NAD(P)H alone as a performance indicator provides little information and, importantly, discloses no information on mass/carbon balance.

In this work, we have examined, for the first time, the conversion, selectivity and mass balance during the course of NAD⁺ reduction reactions for NADH regeneration, employing supported Pt catalysts (Pt/SiO₂, Pt/C and Pt/MgO) and using H₂ as a reducing agent. Different by-products have been characterized with their relative contribution towards the overall NAD⁺ conversion also investigated. The results have demonstrated a clear contrast to the analysis obtained from a "yield-only" approach and show fundamentals of the support effect as well as by-product formation that otherwise would have been missed.

The catalysts employed have been fully characterized (see Figures S1-3 for details), with key results summarized in Table 1. Pt/SiO₂ and Pt/MgO exhibit type IV isotherms with a H1 hysteresis loop characteristic of mesoporous materials. Both catalysts possess spherical Pt nanoparticles that are well dispersed with narrow size distributions and mean particle sizes of 2.2 and 2.4 nm, respectively. A commercial Pt/C hydrogenation catalyst was used for comparison purposes. The Pt/C exhibits typical activated carbon characteristics in terms of surface area and porosity, where the Pt particles are also well dispersed on the carrier with a narrow size distribution (1-3 nm) and an average size of 1.6 nm. The point of zero charge (pZC) values of the catalysts were determined by the pH drift method (Table 1 and Figure S4). For Pt/SiO₂, at a pH of 3.0 the surface net charge is zero, meaning neutral hydroxylation of Si (Si-OH). Deprotonation of the surface can occur if the catalyst pZC is lower than the working pH, resulting in a negatively charged surface (Si-O⁻). Protonation occurs when the pZC is higher than the working pH, resulting in a positively charged surface (Si-OH₂+).²⁵ Referring to Figure S4, it can be seen that for Pt/SiO₂ most of the curve lies in the negative region $(\Delta pH < 0)$ showing its ability to be negatively charged under biologically relevant conditions that require a pH higher than 3.0. In the case of Pt/C, the pZC was determined to be 7.5 which gives Pt/C a nearly neutral surface at pH 7. Pt/MgO exhibits a high pZC (10.3) which shows that it will be positively charged (due to a protonation process, Mg-OH₂⁺) under a reaction pH that is lower than

10.3. The pZC results are in agreement with the literature where the pZCs of SiO_2 , activated carbon and MgO were reported between 2.5 and 3.1, $^{26-28}$ 7.4 and 7.8, 29,30 and 10 and 12.5, 26 respectively.

The catalytic results are first shown (Figure S5) by determining the yield based on all products that exhibit an UV-Vis absorbance at 340 nm (Y_{340 nm}) and applying the absorption coefficient of 1,4-NADH, which is the most frequent yield determination method used in the literature.⁶⁻¹⁶ We must note that even though these publications refer to it as a yield of NADH (referring to 1,4-NADH), this cannot hold unless the 340 nm absorbance is solely due to 1,4-NADH, considering that 1,6-NADH and the NAD₂ dimer also exhibit λ_{max} at 345 and ~340 nm, respectively. Importantly it is also well established that non-specific reduction of NAD⁺ can produce 1,2-, 1,6-NADH and the dimers. Given this, the results shown in Figure S5 could not lead to any reliable conclusions on activity/selectivity. We should flag here that the majority of the literature validated only the last experimental sample in terms of its 1,4-NADH concentration, meaning there has been no time-on-stream measurement on how such concentrations were reached. With a recently established method for the quantification of reaction products,³¹ we have been able to show, for each time-on-stream experimental point, that the 340 nm absorbance was due to a mixture of 1,4- and 1,6-NADH (individual yields provided in Figure S5). There are some variations in terms of $Y_{1,4-NADH}$ and $Y_{1,6-NADH}$ over the three catalysts (Figure S5), but knowing already they are unselective from the beginning of the regeneration, again no meaningful link can be established between the catalyst characteristics and their performance. Unless a full picture of the reaction profiles (e.g., conversion, selectivity and mass balance) are presented, the conclusions/interpretations argued could potentially be misleading.

With the product selectivity and NAD⁺ conversion experimentally determined, the catalytic results are now presented in **Figure 1**. Surprisingly, the mass balance was not closed over the entire course of the reactions, a result that has never been emphasized (or even reported) in the literature. It

appears to be an underlying issue in the development of non-enzymatic regeneration techniques. Figure 1 shows that for all the catalysts, as the conversion increased with time the selectivity of the unknown (calculated through mass balance closure) decreased then levelled whereas the selectivity of 1,4- and 1,6-NADH increased and stabilized. Pt/SiO₂, Pt/C and Pt/MgO exhibited a conversion of 80.0%, 84.1% and 56.6% in 2 h, respectively, with corresponding initial TOFs of 1600 h⁻¹ for Pt/SiO₂, 1123 h⁻¹ for Pt/C and 990 h⁻¹ for Pt/MgO. The specific activity order matches well with the increasing pZC values $(3.0 \rightarrow 7.5 \rightarrow 10.3,$ Figure 1(d)). This can be attributed to the overall catalyst surface charge, which affects the interactions with the positively charged (+1) nicotinamide ring (where the reaction occurs³²) via electrostatic forces. At a reaction pH of 7, Pt/SiO₂ has a strong negatively charged surface due to the pZC deprotonation mechanism. This increases the local concentration of nicotinamide ring (+1, Figure S6) around the Pt nanoparticles where Pt-H_{ads} species^{33,34} are available for hydrogenation, thus enhancing the probability of reactions. On the other hand, at pH 7, both ionizable hydroxyl groups (pKa = 2.4 and 6.6) on the diphosphate linkage of NAD+ are deprotonated exhibiting each a charge of -1.35 This side of the molecule (-2) should exhibit an electrostatic repulsion with the negatively changed surface. Moreover, it is reported that the diphosphate linkage is highly hydrophilic and typically stays in the bulk aqueous buffer solution away from the catalyst surface (Figure S6). 32,36 These all support that a negatively charged catalyst surface is favorable for NAD⁺ hydrogenation. In the case of the least active Pt/MgO, it has a high pZC of 10.3, corresponding to a positively charged surface that resulted in unfavorable interaction with the nicotinamide ring (+1). Pt/C exhibits a pZC between those of Pt/SiO₂ and Pt/MgO, hence an intermediate activity. The same activity-pZC relationship was also obtained at pH 10 (Figure S7), consistent with the above discussions and confirming the surface charge contribution. To this end, Roy and co-workers have recently reported that interactions via electrostatic forces can also influence NADH yield in photocatalytic regeneration.³⁷ Although the support pZC affected the activity, it had no obvious influence on the selectivity. For instance, at $X_{NAD}^+ = ^{\sim}47\%$, the selectivity of 1,4-NADH were as

follows: 20.2 % for Pt/SiO₂, 25.1 % for Pt/C and 17.8 % for Pt/MgO. It is only through the conversion and mass balance examinations that these observations were obtained. The present results highlight the importance of carefully validating the mass balance and the respective contributions to the 340 nm absorbance prior to claiming any selectivity/yield values, and, hence, arriving at mechanistic assumptions.

In order to shed some light on the unknown product, further experiments on the stability of 1,4-NADH and NAD⁺ under various conditions have been conducted. When no catalyst was used, almost 20% of the initial 1,4-NADH was consumed by self-decay in 180 min regardless of the nature of the gas (Figure 2(a)), consistent with first order decay kinetics as reported previously. 20,38 1,4-NADH undergoes an acid-catalyzed hydration reaction to form the primary decay product, 6hydroxytetrahydropyridine adenine dinucleotide (UV-vis at 290-300 nm).³⁹ On the other hand, Figure 2(b) shows the stability of NAD+ after 180 min in the presence of N2 and Pt/C as a representative catalyst. The results of the enzymatic kit (measuring the total concentration of 1,4-NADH and NAD+)31 as well as the UV-scans (inset of Figure 2(b)) also prove that NAD+ stays intact throughout time. However, it was interesting to see that in the case of 1,4-NADH when H₂ and Pt/C were used, the rate of concentration decrease was higher with a loss of 65.4% after 180 min, suggesting enhanced decay due to the Pt catalyst which provides protons. 33,34 The results of the enzymatic kit match the actual concentration of 1,4-NADH indicating that 1,4-NADH is the only enzymatically active species present in the reaction medium (i.e., no tautomerization or NAD+ formation). The results of the UV-scans (see inset of Figure 2(a)) conducted at 180 min of each reaction prove the formation of an enzymatically inactive product with absorbance around 290-300 nm. These results demonstrate that once formed, 1,4-NADH may be subject to enhanced decay by the catalyst in the reaction medium and conditions, in line with the following ¹H NMR analysis.

The ¹H NMR results obtained from the reduction of NAD⁺ (using Pt/C as a representative catalyst) are shown in Figure 3. Singlets are single peaks assigned to hydrogen atoms that do not have any surrounding or neighbor hydrogen. For NAD⁺ (Figure 3(a)), the singlet located at around 9.20 ppm is characteristic of the hydrogen H-2' of the nicotinamide moiety. 40 The other two singlets located between 8 and 8.5 ppm are attributed to the hydrogen atoms of the adenine ring. 40,41 In the case of a freshly prepared 1,4-NADH solution (Figure 3(b)), the singlet at 6.85 ppm is attributed to the H-2 of the nicotinamide ring, 42 whereas the other two singlets between 8 and 8.5 ppm are characteristic of the adenine ring (in the R group, Figure S6).⁴¹ The ¹H NMR results of the products at 2 h (Figure 3(c)) shows a combination of both NAD⁺ and 1,4-NADH. However, two new singlets appear at 7.01 and 7.13 ppm, characteristics of the by-products formed during regeneration (as evident over all three Pt catalysts, see also Figure S8). Knowing that 1,4-NADH can self-decay with time (Figure 2(a)), 38,43 a 1,4-NADH sample was left for decay and subsequently ¹H NMR spectra of the products were collected (Figure 3(d)). The 1,4-NADH decay product appears through a singlet at 7.13 ppm which matches one of the peaks in the NADH regeneration products. The other signal should be due to 1,6-NADH as one of our confirmed products, exhibiting a peak at 7.01 ppm. In order to establish this, we have synthesized a mixture of 1,6- and 1,4-NADH based on borohydride NAD+ reduction.³¹ The two isomers exhibit NMR peaks at 7.02 and 6.86, respectively (Figure 3(e)), in good agreement with our reaction profile confirming the generation of 1,6-NADH. Figure 2(c) summarizes the possible NADH regeneration pathways over these Pt catalysts under our reaction conditions. The (catalyzed) decay of 1,4-NADH has often been neglected with prolonged reaction time (e.g., 13h and 21 h) in the literature and if the produced NADH isomers are not enzymatically validated, 1,6-NADH would have been missed. Although not detected in our system, we want to flag the potential formation of 1,2-NADH and/or its decay product. In a nonspecific NAD+ reduction system (like borohydride reduction³¹ but possibly in other electron transfer processes), 1,2-NADH can be formed but quickly decay in the medium (e.g., a pH 7 phosphate buffer), 31 as evident by the 6.63 ppm peak

in Figure 3(e). Given the "yield-only" approach prevailing in the literature, the NMR profiles should also be examined in detail.

In summary, the examination of conversion, selectivity and mass balance in NADH regeneration is proven critical and can provide reliable performance indicators (e.g., TOF based on NAD⁺ consumption). Accordingly, it is shown that an overall negatively charged catalyst surface (i.e., reaction pH higher than pZC) favored the catalytic activity in NADH regeneration while a positively charged surface inhibited the performance. The electrostatic attraction between the catalyst surface (at pH 7, Pt/SiO₂ (negative) > Pt/C (~neutral) > Pt/MgO (positive)) and the positively charged nicotinamide ring (+1) of the NAD+ molecules increases the local concentration of the nicotinamide ring around Pt and hence the potency of the hydrogenation reaction. In addition to the formation of 1,6-NADH, a Pt enhanced 1,4-NADH decay reaction was also evident. We hope that these results may urge future scrutiny on conversion, selectivity and mass balance closure in non-enzymatic NADH regeneration systems prior to publishing the data.

Supporting Information

The Supporting Information is available free of charge at ...

Experimental, results and discussion, figures and references.

ACKNOWLEDGMENTS

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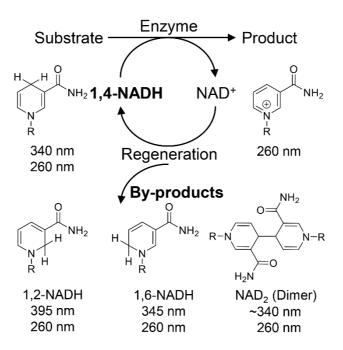
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Table 1

Table 1: Summary of the physicochemical properties of the Pt/SiO₂, Pt/C and Pt/MgO catalysts.

	Pt/SiO ₂	Pt/C	Pt/MgO
Pt Loading (%)	0.83	0.93	1.52
BET Surface Area (m ² g ⁻¹)	165	938	86
Pore Volume (cm ³ g ⁻¹)	0.9	0.4	0.7
Pore Size (nm)	25.4	5.0	28.3
Particle Size (nm)	2.2	1.6	2.4
pZC (-)	3.0	7.5	10.3

Scheme 1



Scheme 1. Schematic representation of biotransformations with *in situ* NADH regeneration that can generate unselective 1,2-NADH, 1,6-NADH and NAD₂ dimer products with their corresponding absorption maxima.

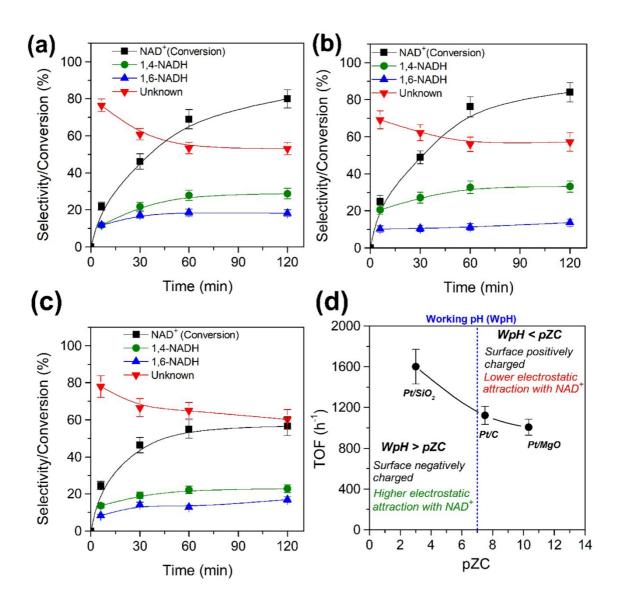


Figure 1. Selectivity and conversion as a function of time in the regeneration of NADH over supported Pt catalysts: Pt/SiO₂ (a), Pt/C (b) and Pt/MgO (c); Effect of catalyst point of zero charge (pZC) on the initial TOF (d). Reaction conditions: $[NAD^+]_0 = 1.5$ mM, 5 mg catalyst, 10 atm H₂, 0.1 M phosphate buffer pH 7, 37 °C, 1200 rpm.

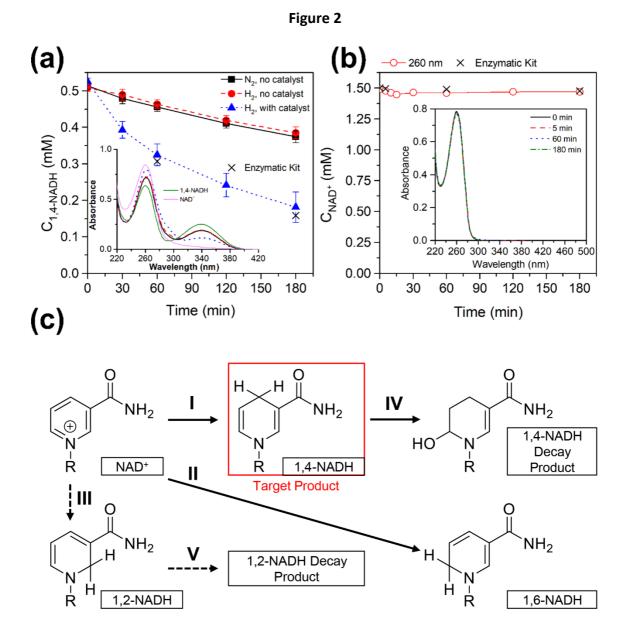


Figure 2. (a) 1,4-NADH stability test ($C_{1,4-NADH}$ as a function of time) under N_2 and no catalyst, H_2 and no catalyst and H_2 with catalyst (Conditions: $[1,4-NADH]_0 = 0.5$ mM, 0.1 M phosphate buffer pH 7, 5 mg of Pt/C (if applicable), 37 °C, 10 atm, 1200 rpm); inset: UV-vis absorbance at 180 min with 0.5 mM of NAD+ and 1,4-NADH as references; (b) NAD+ stability test (C_{NAD} + as a function of time) with N_2 and Pt/C catalyst (Conditions: $[NAD^+]_0 = 1.5$ mM, 0.1 M phosphate buffer pH 7, 5 mg of Pt/C, 37 °C, 10 atm, 1200 rpm); inset: UV-vis absorbance in the course of the reaction; (c) Schematic representation of the Pt promoted NADH regeneration pathways.



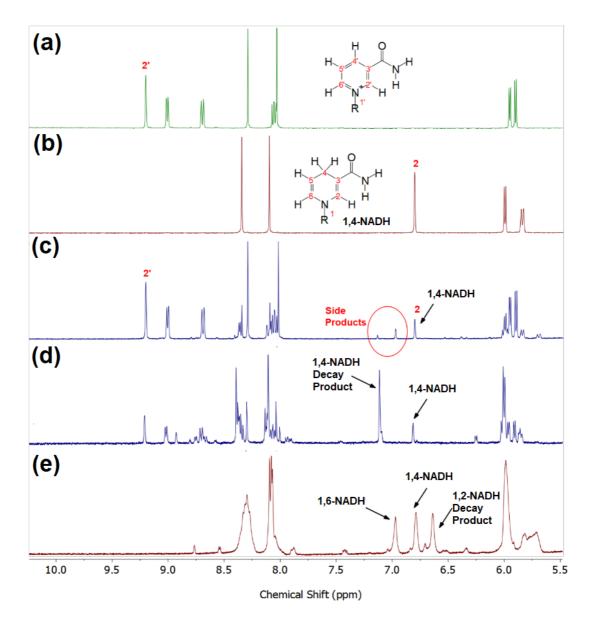


Figure 3. ¹H NMR spectra for (a) NAD⁺ ($C_0 = 6$ mM in 0.1 M D₂O phosphate buffer pH 7), (b) 1,4-NADH ($C_0 = 6$ mM in 0.1 M D₂O phosphate buffer pH 7), (c) Pt/C catalyzed NADH regeneration products ([NAD⁺]₀ = 6 mM in 0.1 M D₂O phosphate buffer pH 7, 20 mg Pt/C, 37 °C, 10 atm H₂, 1200 rpm, 2 h), (d) 1,4-NADH self-decay ([1,4-NADH]₀ = 6mM in 0.1 M D₂O phosphate buffer pH 7 at 20 °C) and (e) NAD⁺ Borohydride Reduction Products ([NAD⁺]₀ = 15 mM in 0.1 M D₂O phosphate buffer pH 7 at 20 °C with [NaBH₄]₀ = 75 mM).